

THE FRAMEWORK PROGRAMME FOR RESEARCH AND INNOVATION  
HORIZON 2020



INSTITUT DE CHIMIE  
SEPARATIVE DE MARCOULE



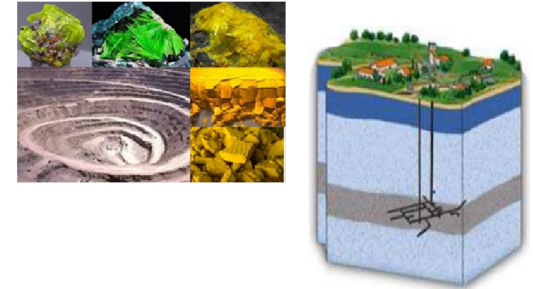
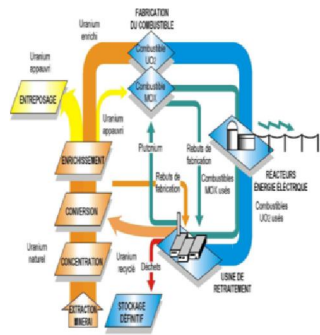
# New insights in the description of the dissolution of actinide dioxides : better understanding for their reprocessing



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## Transverse approach of the material elaboration



**Sintering :  
densification  
microstructure**

**Dissolution**

**Leaching**

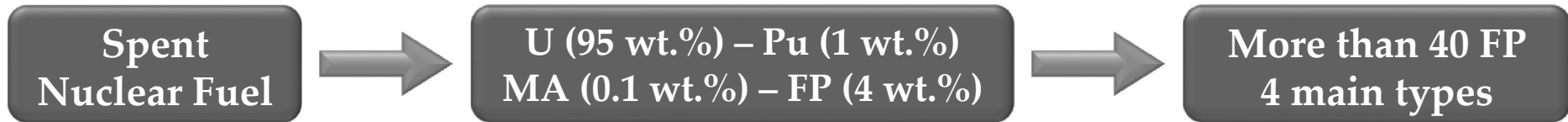
**Model compounds :  
New ways of synthesis  
New precursors**

*Optimized Syntheses*

**Properties in use :  
Chemical durability  
Long-term behavior**

- ✦ **Dissolution of  $AnO_2$ ,  $(An,Ln)O_{2-x}$  / Fluorite-type prepared by wet chemistry routes**
  - ❖ **Conventional parameters** ( **chemical composition**, temperature, acidity, ... )
  - ❖ **Structural parameters** ( **oxygen vacancies**, superstructure, secondary phases, ... )
  - ❖ **Microstructural parameters** ( **crystal defects**, crystallite size, densification rate, ... )

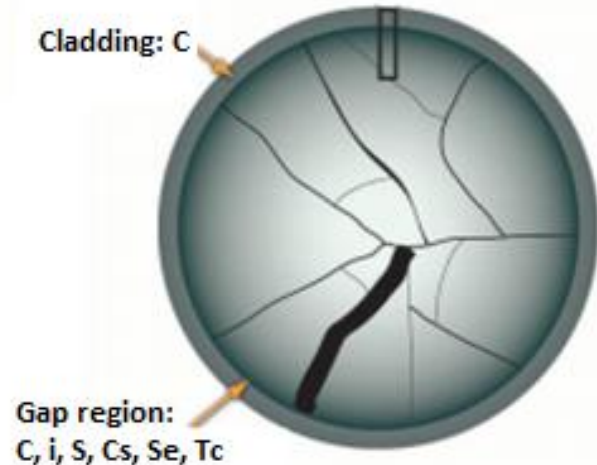
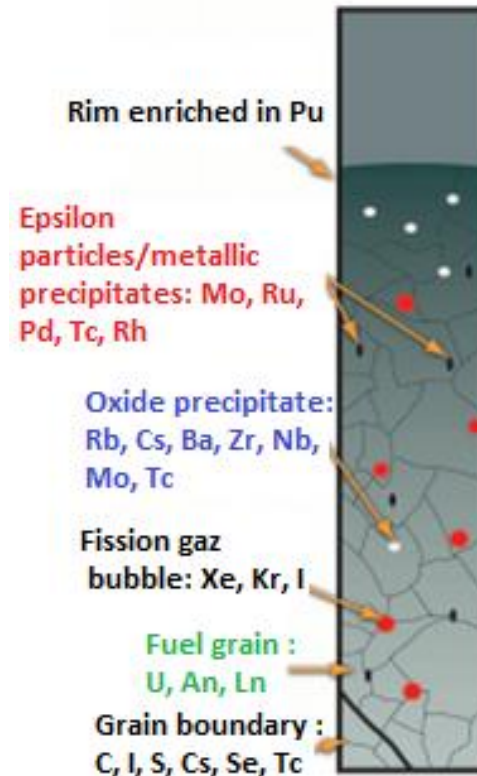
# Distribution of FP and An in SNF



**PGM**  
(Ru, Rh, Pd)  
≈ 0.6 mol.%

**Lanthanides**  
(La, Ce, Pr, Nd)  
≈ 1 mol.%

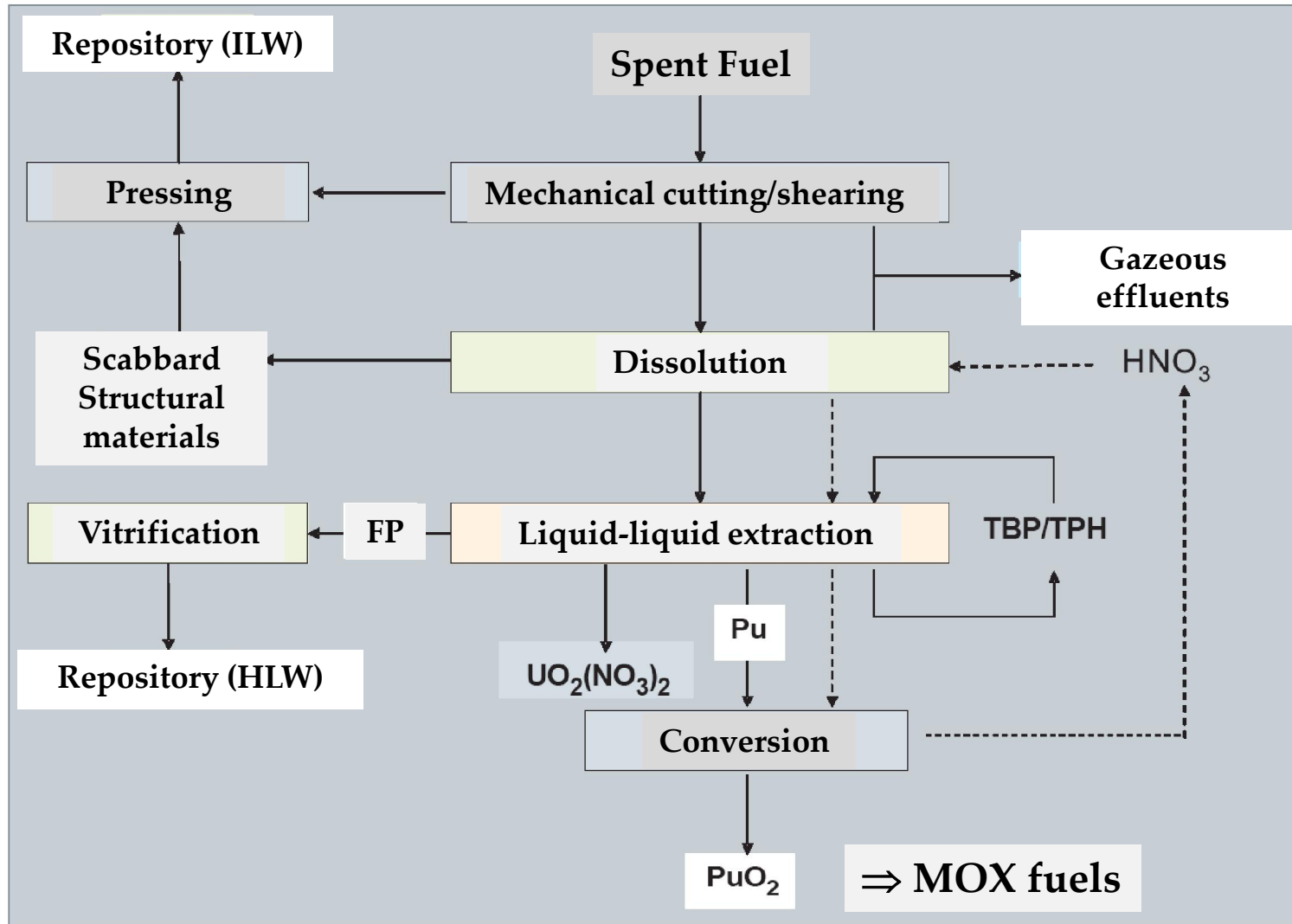
**Actinides**  
(Np, Pu, Am, Cm)  
≈ 1.1 mol.%



**Which impact on UO<sub>2</sub> dissolution ?**

P. Burns, R.C. Ewing, A. Navrotsky, *Science* 2012, 335, 1184-1187  
PRECCI Report, CEA, 2001, CEA-R-5958E

# Dissolution : a key step in the front-end of reprocessing



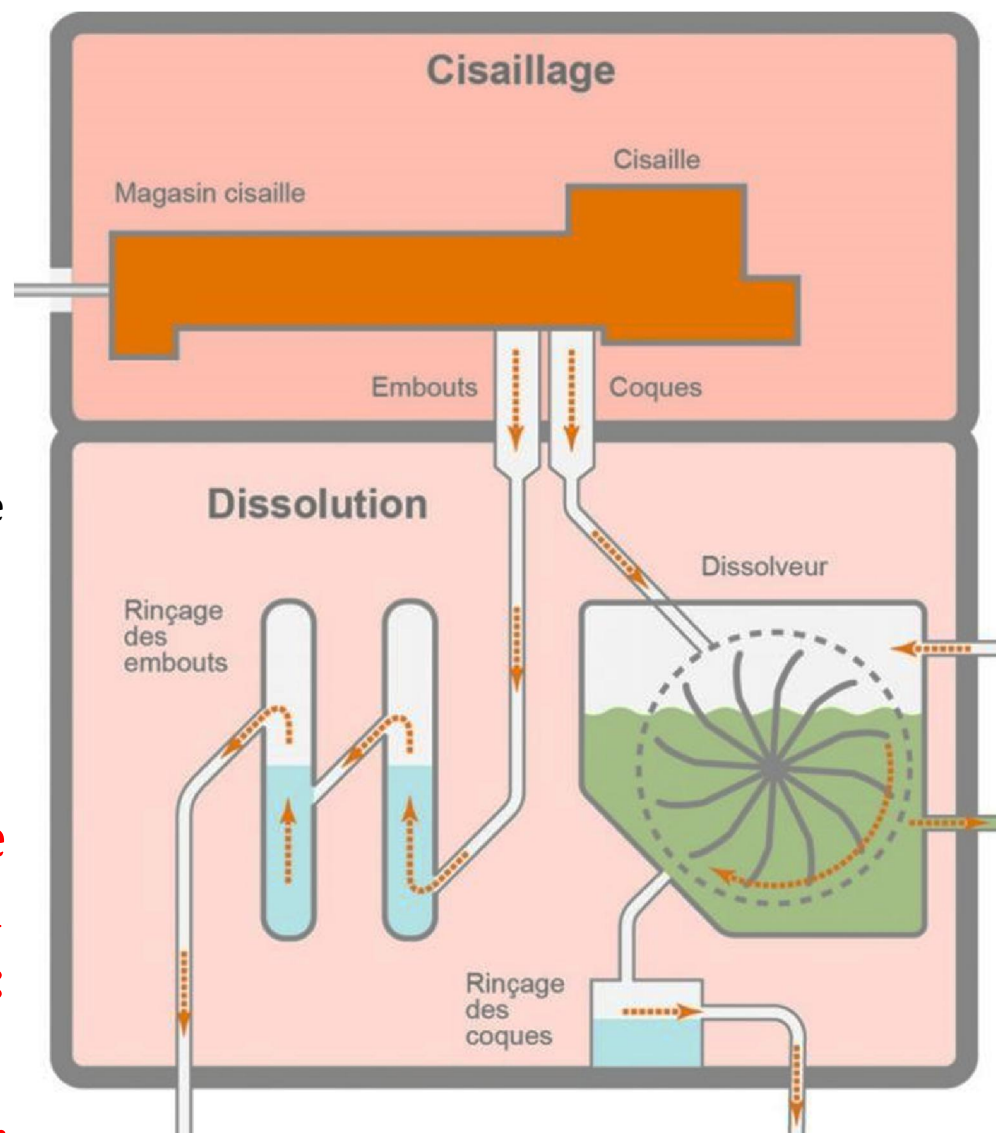
Monographie CEA, Ed. Le Moniteur, 2008

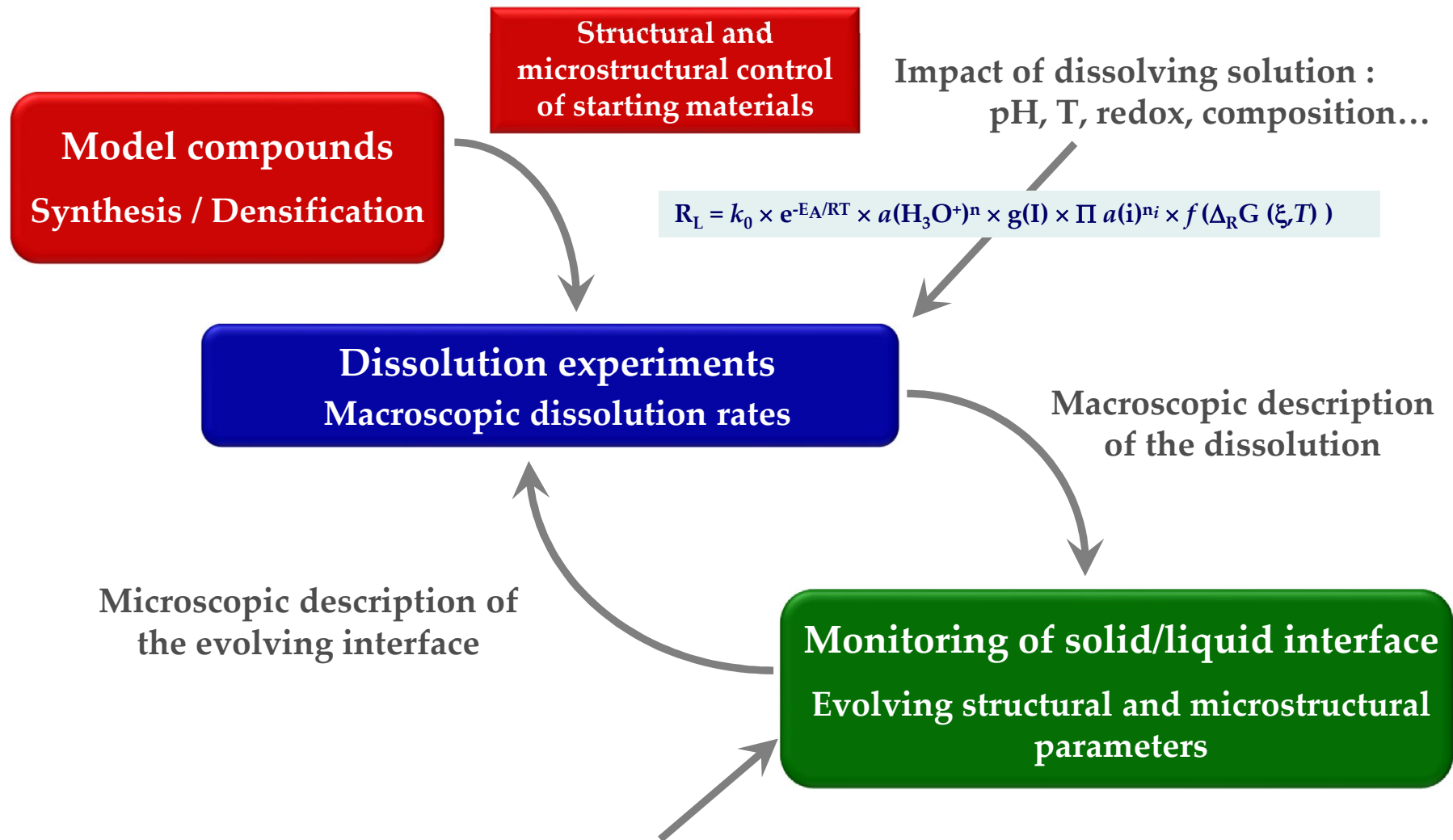
# Dissolution : a key step in the front-end of reprocessing



- *Shearing of the fuel pens*  
Zircaloy scabbard / irradiated  $\text{UO}_2$
- *Dissolution*
  - Hot and Concentrated  $\text{HNO}_3$
  - Oxidation of U(IV) into U(VI)
  - Uptake of scabbards pieces with the help of bucket-wheel  
⇒ Specific conditioning

**Necessity to better discriminate and prioritize the reactions and parameters driving dissolution: chemistry, radiolysis, structure, homogeneity, microstructure, ...**

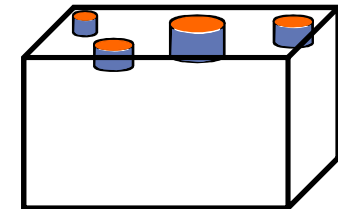
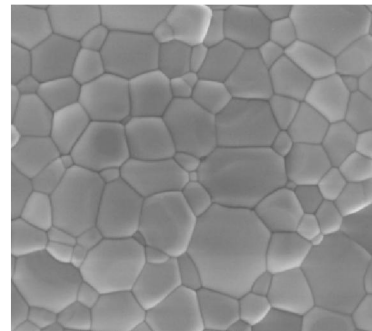
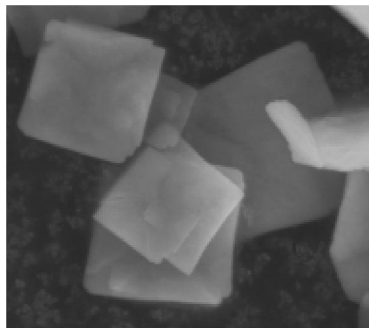
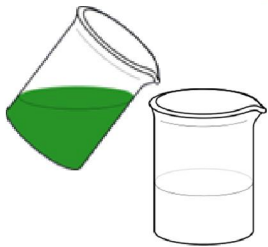




*Operando* analysis (ESEM, X-EDS, G-XRD, XRR, AFM)

↳ Topography, porosity, chemical composition of interface

# Preparation of model samples : Powdered – Sintered Actinide bearing oxides



## Oxalate precipitation

## Conversion



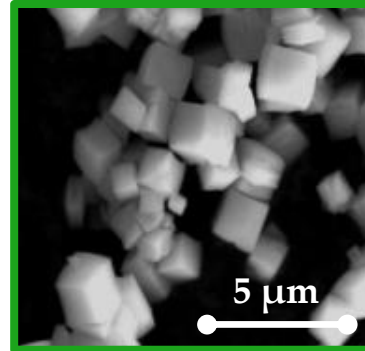
↳ 7% Y – 13% La – 26% Ce – 12% Pr – 42% Nd

R. T.  
 $H_2C_2O_4$  : + 50%

Washing  
( $H_2O$  – EtOH)



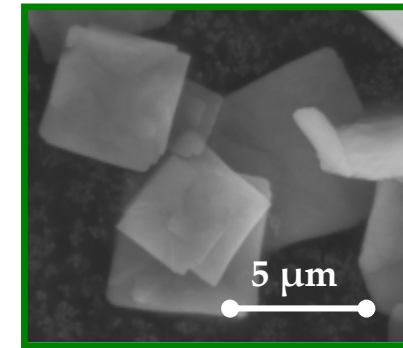
Drying  
(90°C)



500°C / 4 h



Air  
then  
Ar /  $H_2$



Platelet grains  
 $\approx 5 \mu m$  in size

## Quantitative precipitation for U and Th precipitation

	Expected mole ratio	Obtained (Dissolution)	Recovery yield (%)
U	0.9	$0.89 \pm 0.04$	99.3 ✓
Ln(III)	0.1	$0.11 \pm 0.02$	

Full dissolution  
ICP-AES



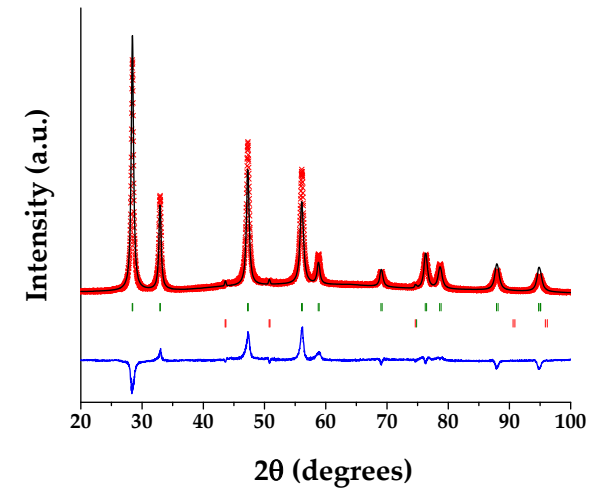
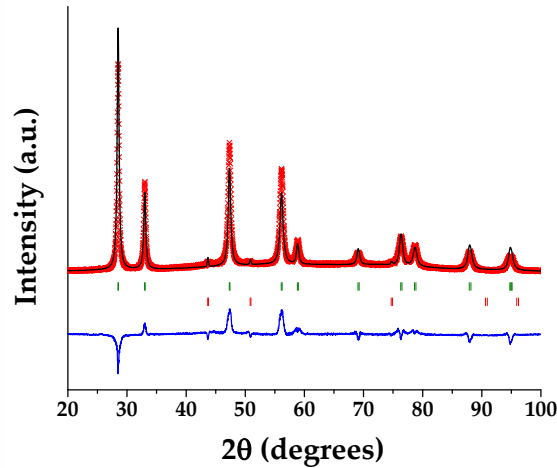
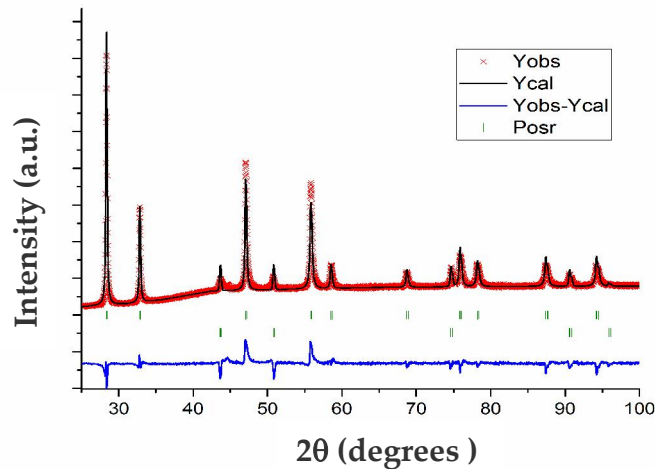
Y	0.07	$0.06 \pm 0.02$	99.9 ✓
La	0.13	$0.14 \pm 0.03$	93.8 ✓
Ce	0.26	$0.31 \pm 0.05$	92.9 ✓
Pr	0.12	$0.13 \pm 0.08$	98.7 ✓
Nd	0.42	$0.42 \pm 0.04$	95.6 ✓



# Characterization by XRD



➤ Complete solid solution for  $\text{Th}_{1-x}\text{U}_x\text{O}_2$ , following the Vegard's law



$a = 5.466 \text{ \AA}$

Literature :  
 $a = 5.47127(8) \text{ \AA}$

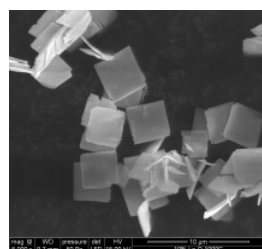
$a = 5.442 \text{ \AA}$

$a = 5.438 \text{ \AA}$

Incorporation of Ln(III) in the  $\text{UO}_2$   
Fluorite-type structure

G. Leinders, *J. Nucl. Mater.*, 2015, 459, 135-142

# Sintering of $U_{1-x}Ln_xO_{2-x/2}$ samples



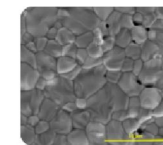
Grinding step  
30 Hz / 30 min



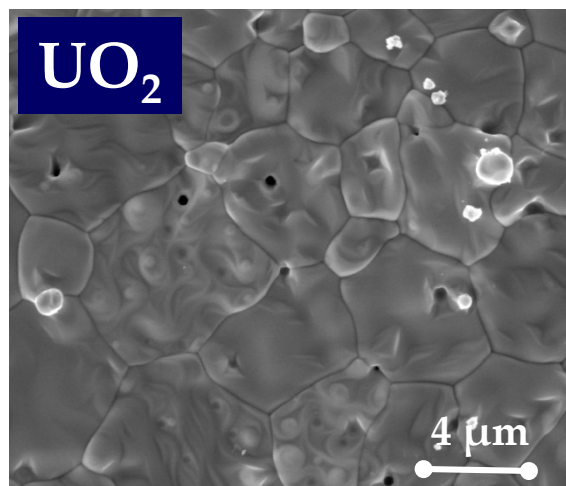
Uniaxial pressing  
RT – 500 MPa



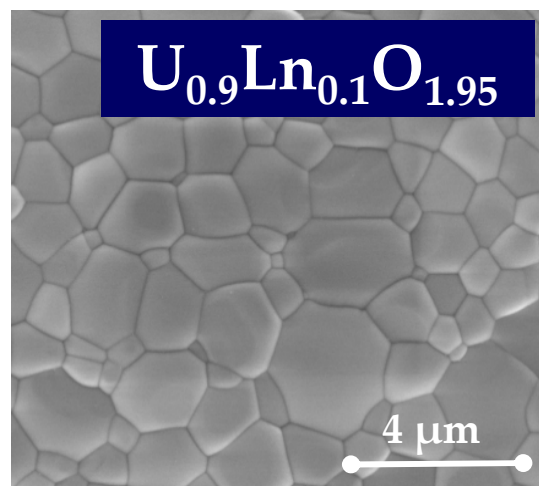
Heating treatment  
1550°C / 8h  
Ar – 5% H<sub>2</sub>



Characterization  
PXRD, BET, ESEM, Pycnometry



Densification rate: 93%  
Average grain size: 11.8 μm



Densification rate: 90%  
Average grain size: 3.4 μm



Densification rate: 87%  
Average grain size: 0.9 μm

T. Cordara, PhD, University of Montpellier, 2017

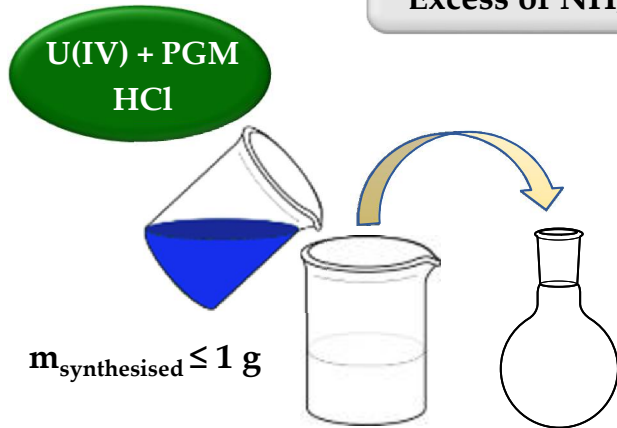
# Preparation of PGM doped $\text{UO}_2$



## Hydroxide precipitation

$\text{UO}_2$  doped with 3% PGM  
Rh (10%) – Ru (55%) – Pd (35%)

Room temperature  
Excess of  $\text{NH}_4\text{OH}$



Washing  
(water + ethanol)

Precipitate  
+  
EtOH

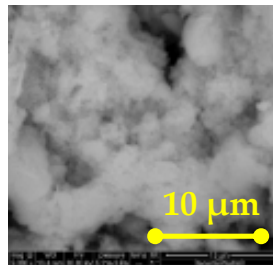


Drying under vacuum  
 $T = 40^\circ\text{C}$

## Conversion

### Recovery yield

- ☺ U : 99.9 %
- ☺ Ru : 90 %
- ☺ Pd : 100 %
- ☺ Rh : 85 %



Highly reactive

$120 - 150 \text{ m}^2 \cdot \text{g}^{-1}$

Crystallite size: 2-5 nm

$800^\circ\text{C} / 4 \text{ h}$



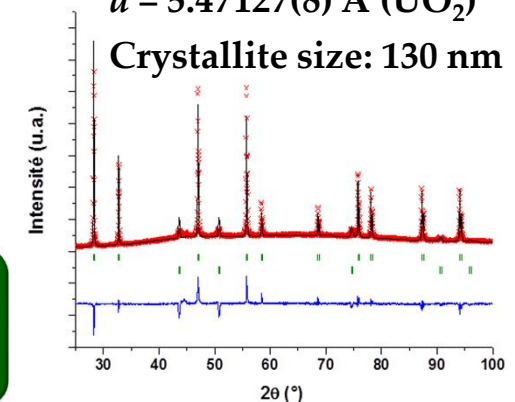
Ar /  $\text{H}_2$

No PGM in the  
 $\text{UO}_2$  structure

$a = 5.470 \text{ \AA}$

$a = 5.47127(8) \text{ \AA} (\text{UO}_2)^*$

Crystallite size: 130 nm



J. Martinez, Patent FR3016360 – WO2015/107086, 2015  
N. Clavier et al., Chem. Phys. Chem., 2017, 18, 2666-2674  
T. Cordara, J. Nucl. Mater., 2019, Submitted  
\* G. Leinders, J. Nucl. Mater., 2015, 459, 135-142

# Sintering of $\text{UO}_2$ : PGM



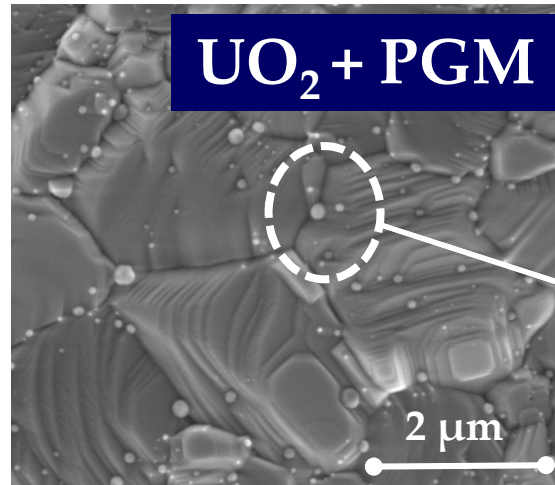
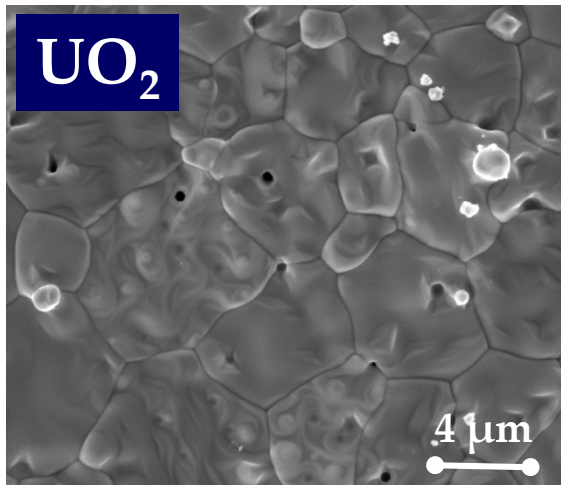
Uniaxial pressing  
RT – 500 MPa



Heating treatment  
1550°C / 8h  
Ar – 5%  $\text{H}_2$



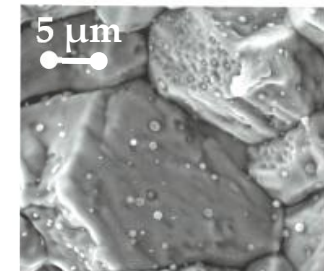
Characterization  
PXRD, BET, ESEM,  
Pycnometry



Ru, Rh, Pd bearing  
aggregates located at GB  
(surface + inner)

Densification rate: 93%  
Average grain size: 11.8  $\mu\text{m}$

Densification rate : 89%  
PGM-aggregates < 0.5  $\mu\text{m}$   
 $\text{UO}_2$  grains size  $\approx$  1-5  $\mu\text{m}$



T. Cordara, *J. Nucl. Mater.*, 2019, Submitted  
J. Noirot, *Monographie CEA*, 2009, 25-28



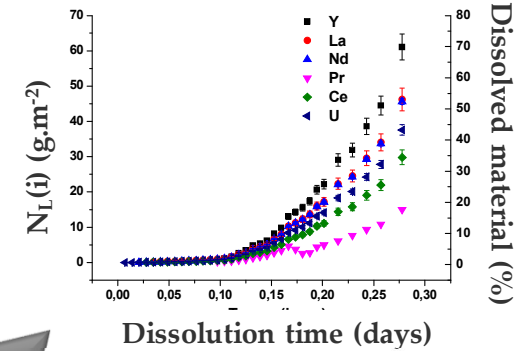
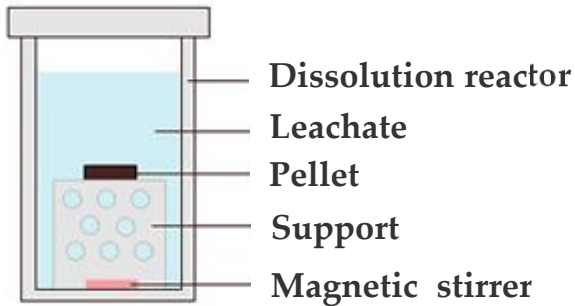
**Chemical durability of the ceramics  
during dissolution processes**

# Dissolution test: experimental device



Powder, Pellet

Static conditions  
Dynamic conditions



$$R_L(i) = \frac{d N_L(i)}{d t} = \frac{1}{f_i \times S} \times \frac{d m_i}{d t}$$

$$N_L(i) = \frac{m_i}{f_i \times S}$$

Amount of (i) in solution (g)  
Reactive surface area (m<sup>2</sup>)  
Mass ratio of (i) in the solid

	$R_{L,0}(i)$ (g.m <sup>-2</sup> .d <sup>-1</sup> )	$R_{L,0}(U)/R_{L,0}(Ln)$
U	5,4 ± 0,2	--
Y	< L.Q.	--
La	7,8 ± 0,1	1,4
Pr	< L.Q.	--
Nd	6,8 ± 0,2	1,3
Ce	4,9 ± 0,2	0,9

ICP-AES  
ICP-MS  
α liquid scintillation



$R_L(i) \approx R_L(j)$ : congruent dissolution  
 $R_L(i) \neq R_L(j)$ : incongruent dissolution

## 2 Study of the surface (sub-surface) of the material Identification of the dissolution mechanisms

### Techniques for observations :

- ✓ Optical microscopy, SEM, ESEM, TEM, ...

### Techniques for surface analysis :

- ✓ Grazing XRD, XRR, ...
- ✓ Spectroscopy (UV, IR, Raman, TRLIFS, ...)
- ✓ EPMA, EELS, X-EDS, ...
- ✓ XPS, EXAFS, XANES, ...

### ❖ To determine :

- ✓ Thickness of the altered layer
- ✓ Nature of the altered layer
- ✓ Characterization of neoformed phases

## 1 Analysis and quantification of elements released in solution

### Elementary concentration determination :

- ✓ Dissolved species, colloidal species
- ✓ Analytical techniques :  
ICP-MS, ICP-AES,  
 $\alpha$  or  $\beta$  scintillation,  $\alpha$  or  $\beta$  spectroscopy

### Species distribution (speciation) :

- ✓ Redox, complexation, acid-base reactions

### ❖ Access to :

- ✓ Direct determination of  $C_{Mi}$
- ✓ Evaluation of weight loss :  $\Delta m_{mat}$
- ✓ Saturation indexes

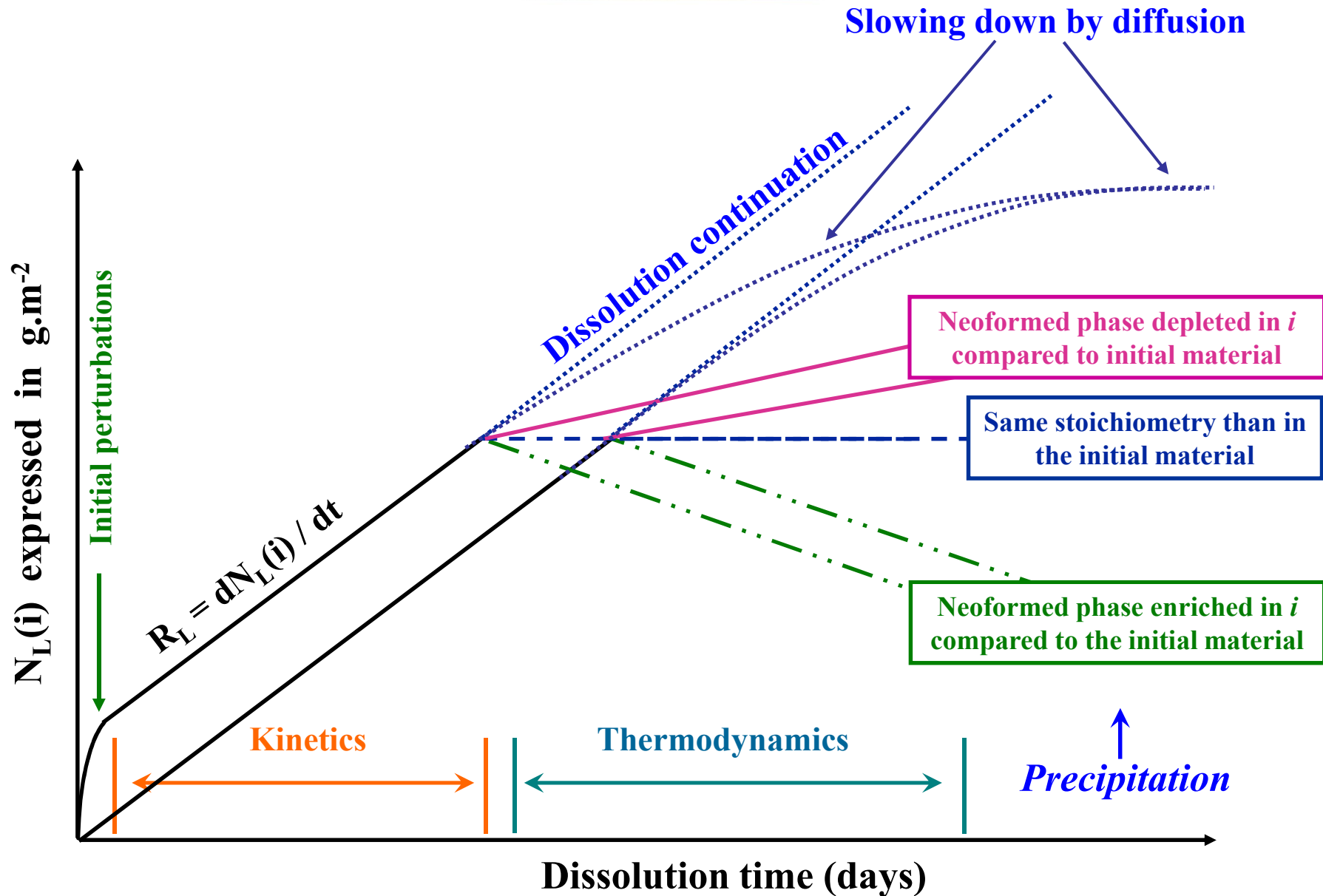
### Normalization tools :

$$N_L(i) = \frac{\Delta m_i}{x_i \times S}$$

$$R_L(i) = \frac{d N_L(i)}{dt} = \frac{1}{x_i \times S} \times \frac{d}{dt} (\Delta m_i)$$

## Description of dissolution & saturation mechanisms

# Schematic representation of ceramic dissolution

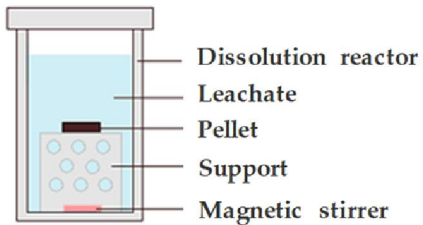




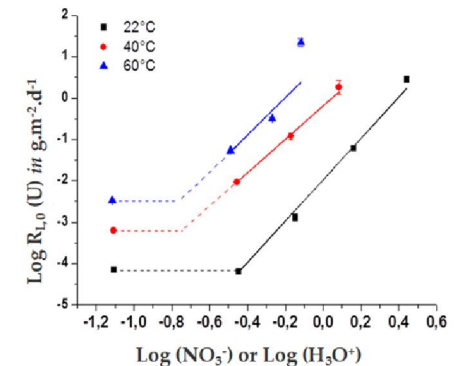
# Macroscopic study

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# Multiparametric expression of the dissolution kinetics



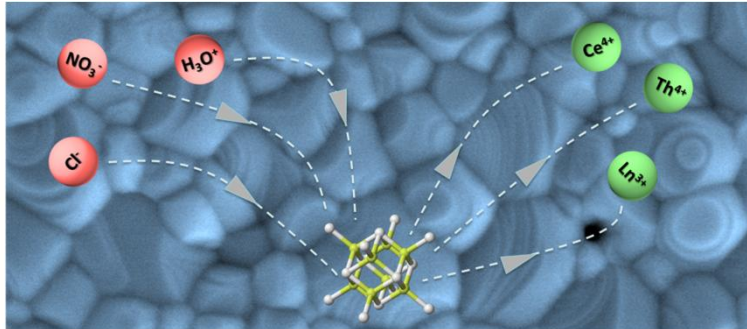
$$R_L = k_0 \times e^{-\frac{E_A}{RT}} \times (\text{H}_3\text{O}^+)^n \times g(I) \times (E_i)^{ni} \times f(\Delta_r G)$$



★ A.C. Lasaga : Geochemical approach

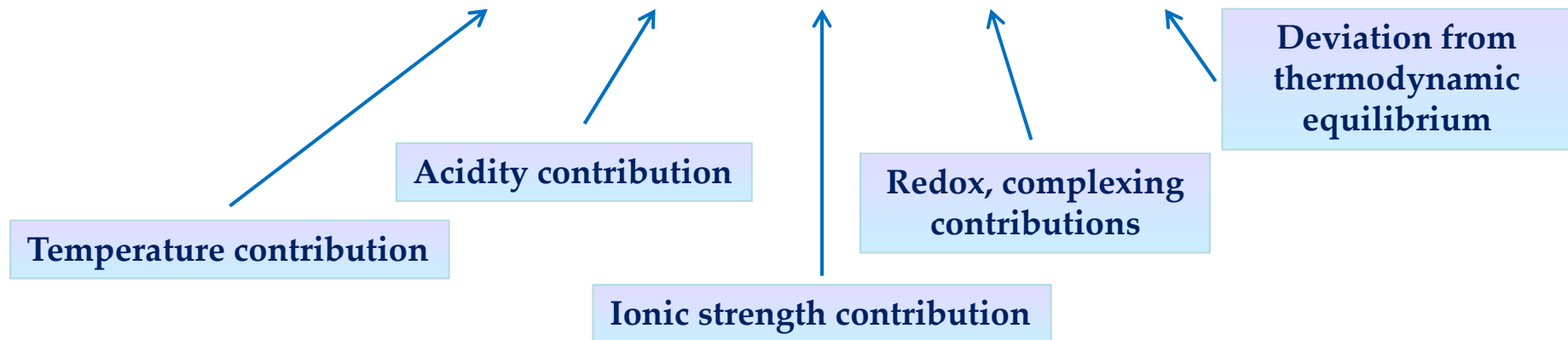
⇒ **Activated Complex Theory**

- ↪ Only chemical effects (solution)
- ↪ Control more often by surface reactions
- ↪ No microstructural effect (solid)



*D. Horlait et al., J. Mater. Chem. A, 2 (2014) 5193*

$$R_L = k_0 \times e^{-E_A/RT} \times a_{H^+}^n \times g(I) \times \prod a_i^{m_i} \times f(\Delta_R G)$$

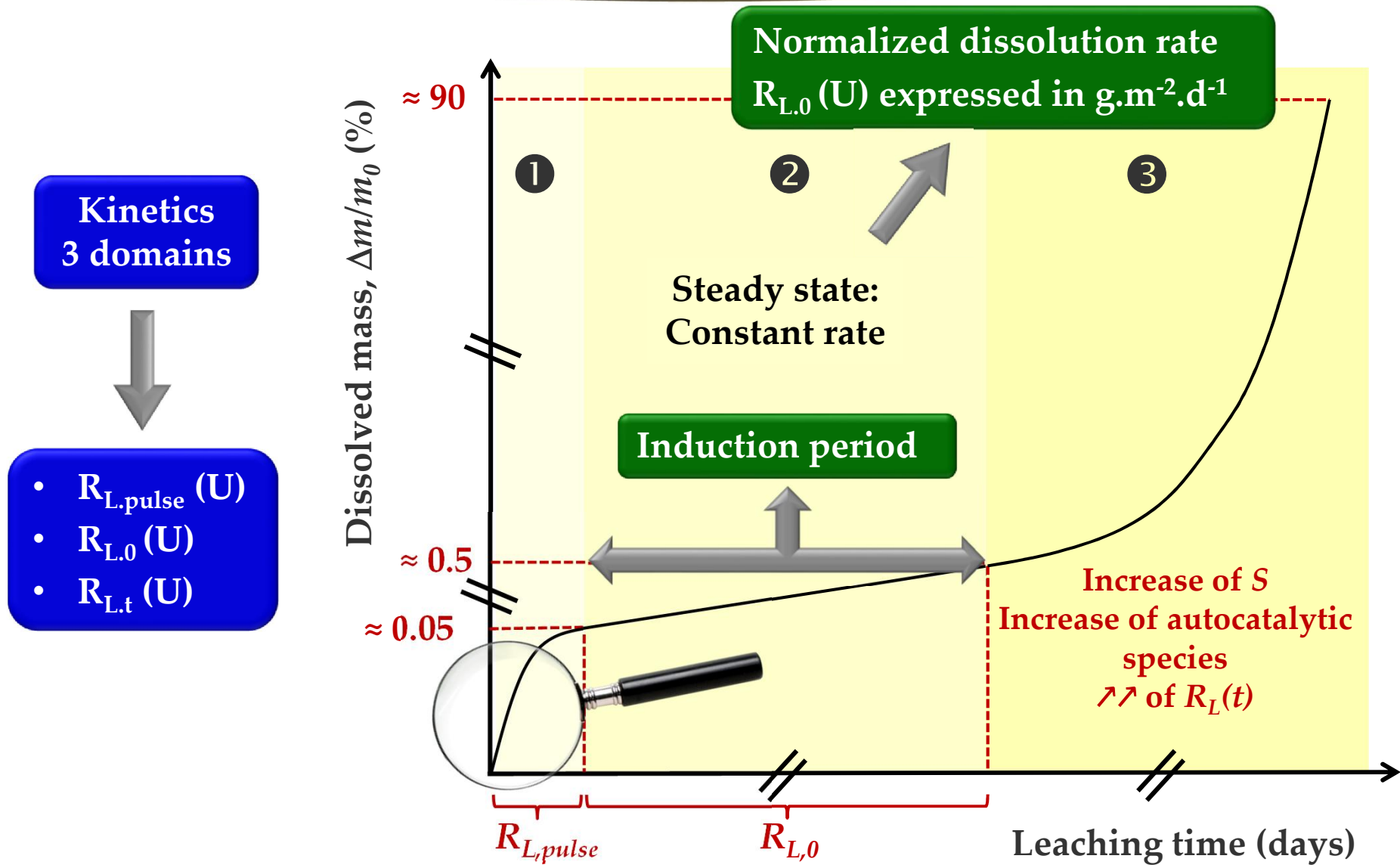


*A.C. Lasaga et al., Rev. Mineral., 31 (1995) 23*  
*A.C. Lasaga et al., J. Geophys. Res., 89 (1984) 4009*

**Impact of conventional parameters  
(acidity, temperature, ...) on the  
dissolution kinetics**



# General trend of $\text{UO}_2$ dissolution in nitric acid



T. Cordara *et al.*, *J. Nucl. Mater.* 2017, 496, 251-264

T. Dalger *et al.*, *J. Nucl. Mater.* 2018, 510, 109-122

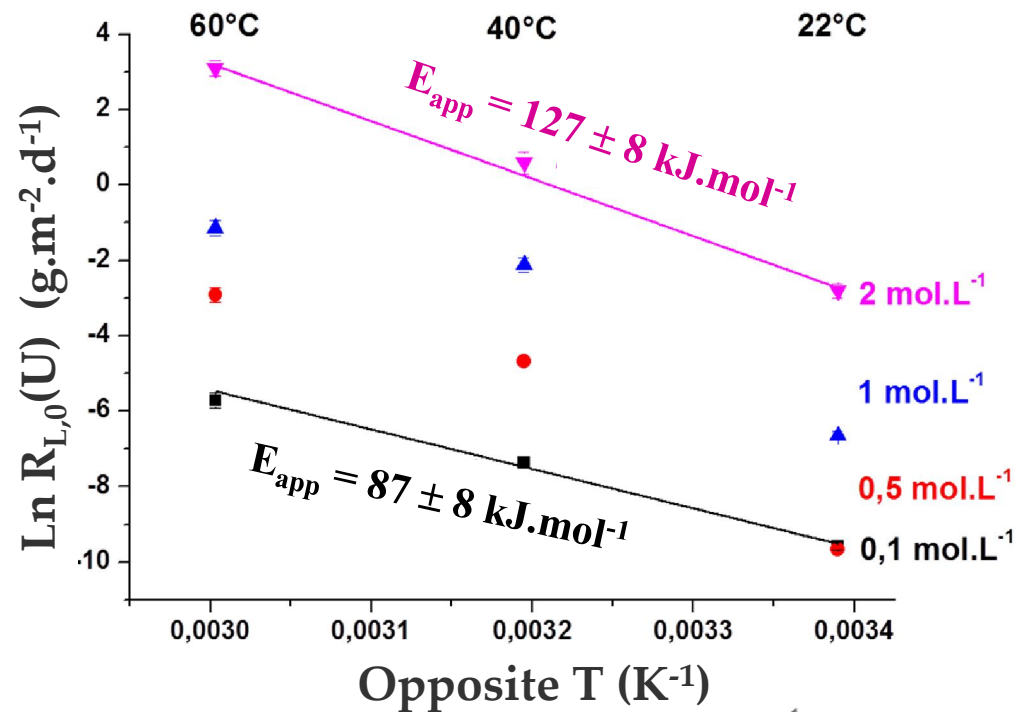
# Impact of temperature on UO<sub>2</sub> dissolution



Reference  
Sintered UO<sub>2</sub>

0.1 – 0.5 – 1 – 2M HNO<sub>3</sub>  
T : 22°C – 40°C – 60°C  
Static conditions

$$R_L = k \times e^{-\frac{E_A}{RT}}$$



Impact of the acid concentration on the activation energy due to change in predominant mechanism:  
Surface controlling ⇒ Redox controlling reactions



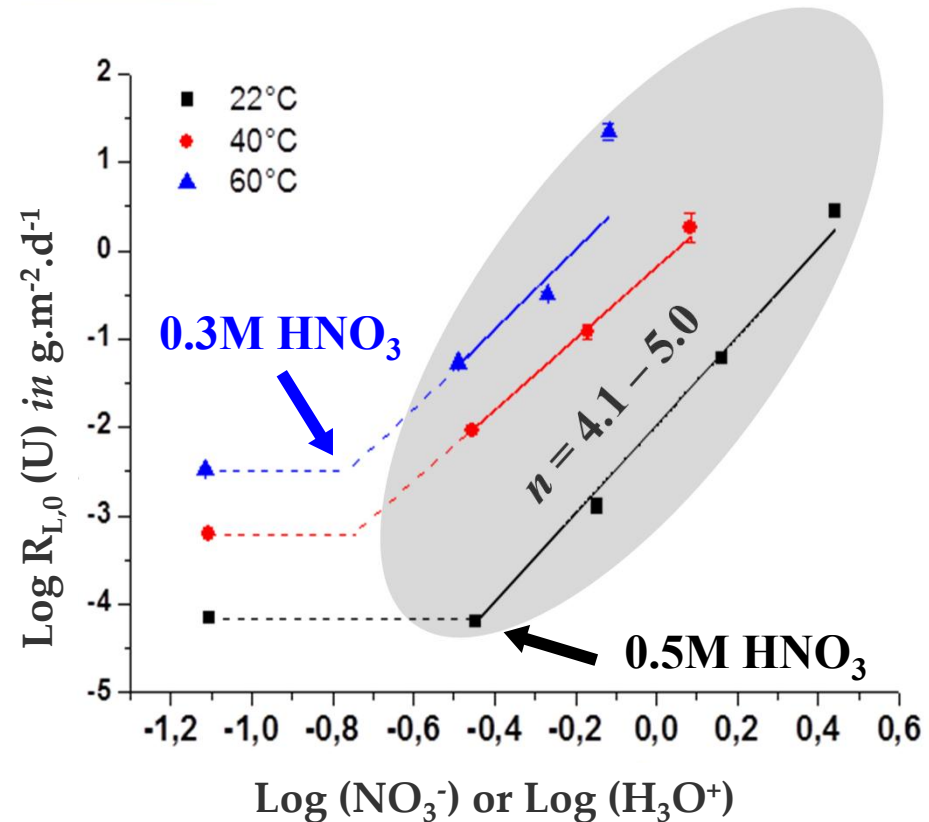
# Impact of acid concentration on UO<sub>2</sub> dissolution



Reference  
Sintered UO<sub>2</sub>

0.1 – 0.5 – 1 – 2M – 4M HNO<sub>3</sub>  
T : 22°C – 40°C – 60°C  
Static conditions

$$R_L = k_T' \times (\text{H}_3\text{O}^+)^n$$



Modification of the preponderant dissolution mechanism with acid concentration

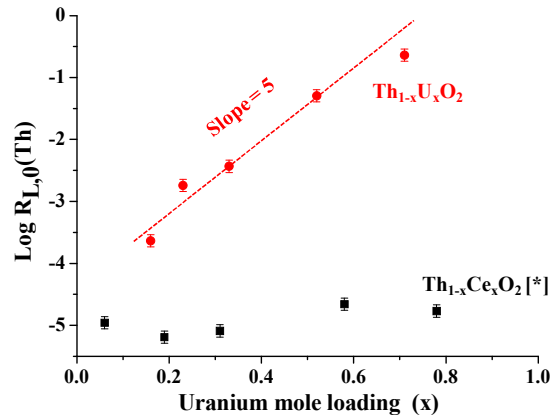
C<sub>HNO<sub>3</sub></sub> < 0.5 M ⇒ Surface controlling reactions  
 C<sub>HNO<sub>3</sub></sub> > 0.5 M ⇒ Redox controlling reactions

# Dissolution of $\text{Th}_{1-x}\text{U}_x\text{O}_2$ solid solutions



## Composition

2M  $\text{HNO}_3$ ,  $T = 60^\circ\text{C}$   
Static conditions

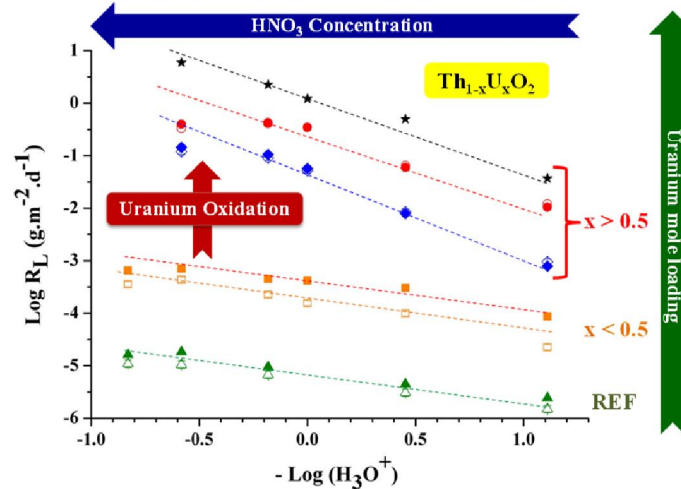


Strong increase of  $R_L(i)$   
with the amount of U

Oxidative process  
 $\text{U(IV)} \rightarrow \text{U(VI)}$

## Acidity

$$R_L = k_T' \times (\text{H}_3\text{O}^+)^n$$

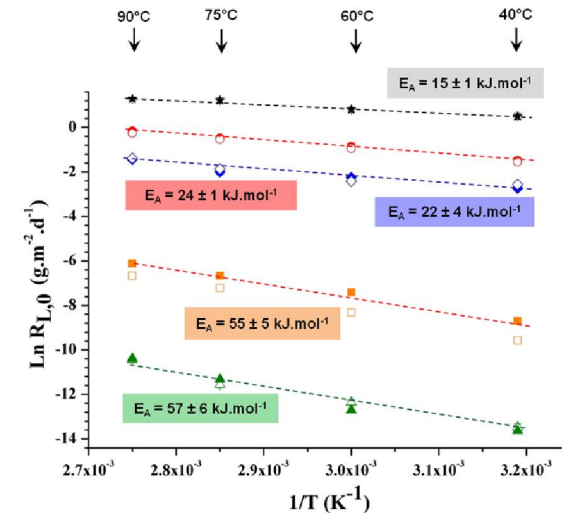


Modification of the controlling dissolution  
mechanism with U mole fraction ( $x_U > 0.5$ )

$x < 0.5 \Rightarrow$  Surface controlling reactions  
 $x > 0.5 \Rightarrow$  Redox controlling reactions

## Temperature

$$R_L = k \times e^{-\frac{E_A}{RT}}$$



L. Claparede *et al.*, *J. Nucl. Mater.*, 2015, 457, 304-316

J. De Pablo *et al.*, *Geochim Cosmochim Acta*, 1999, 63, 3097-3103

# Impact of HNO<sub>2</sub> on dissolution



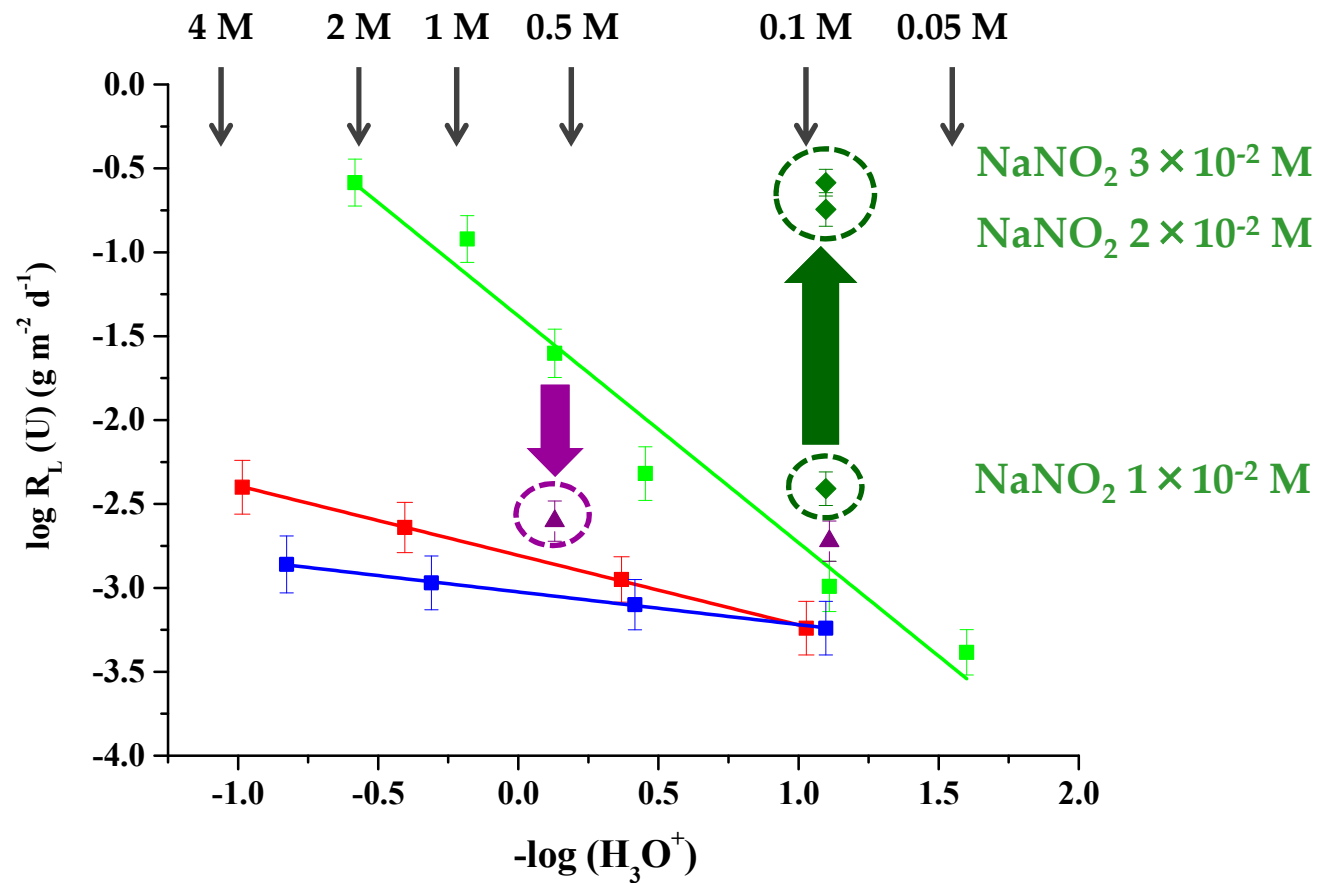
■ HNO<sub>3</sub>

■ H<sub>2</sub>SO<sub>4</sub>

■ HCl

▲ HNO<sub>3</sub> + hydrazinium

◆ HCl + NaNO<sub>2</sub>



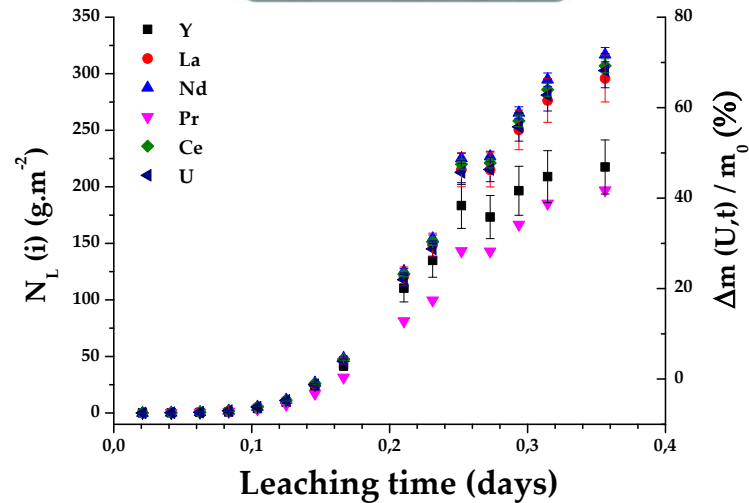
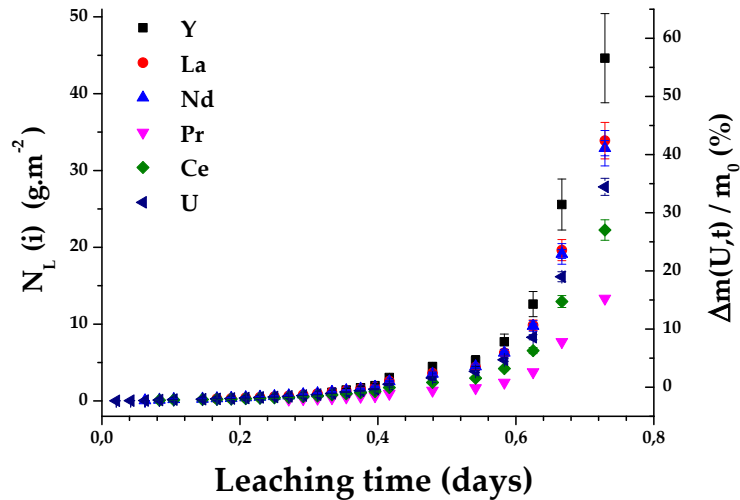
**Strong increase of the dissolution rate with HNO<sub>2</sub>  
Lower impact of H<sub>3</sub>O<sup>+</sup> et NO<sub>3</sub><sup>-</sup>**

F. Tocino, PhD, ICSM/CEA, Univ. Montpellier, Dec. 2015  
T. Dalger, PhD, ICSM/CEA, Univ. Montpellier, 2016–2019

T. Dalger et al., *J. Nucl. Mater.* 2018, 510, 109-122

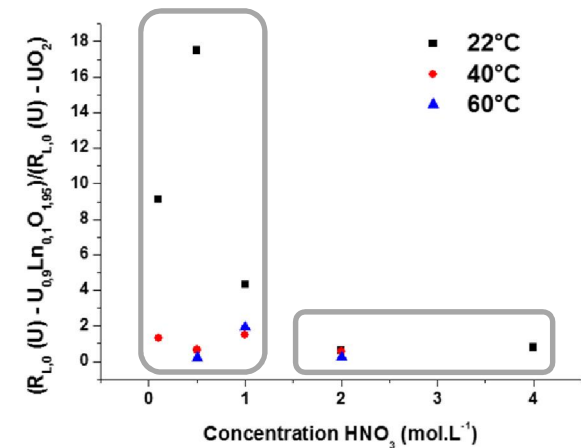


# Dissolution of $U_{1-x}Ln_xO_{2-x/2}$ solid solutions



Congruent dissolution Ln(III) / U  
In agreement with other systems (Th- & Ce-based)

Strong impact of Ln(III) on  $R_{L,0}$  for low acidity ( $C_{HNO_3} < 1M$ )  
e.g. increase by a factor up to  $\approx 20$  for  $U_{0.9}Ln_{0.1}O_{1.95}$  vs.  $UO_2$   
Small impact for higher acid concentrations ( $C_{HNO_3} > 2M$ )



D. Horlait et al., *J. Mater. Chem. A*, 2014, 2, 5193 – *J. Nucl. Mater.*, 2012, 429, 237; S. Szenknect et al., *J. Phys. Chem. C*, 2012, 116, 12027

# Dissolution of $U_{0.9}Ln_{0.1}O_{1.95}$ solid solution



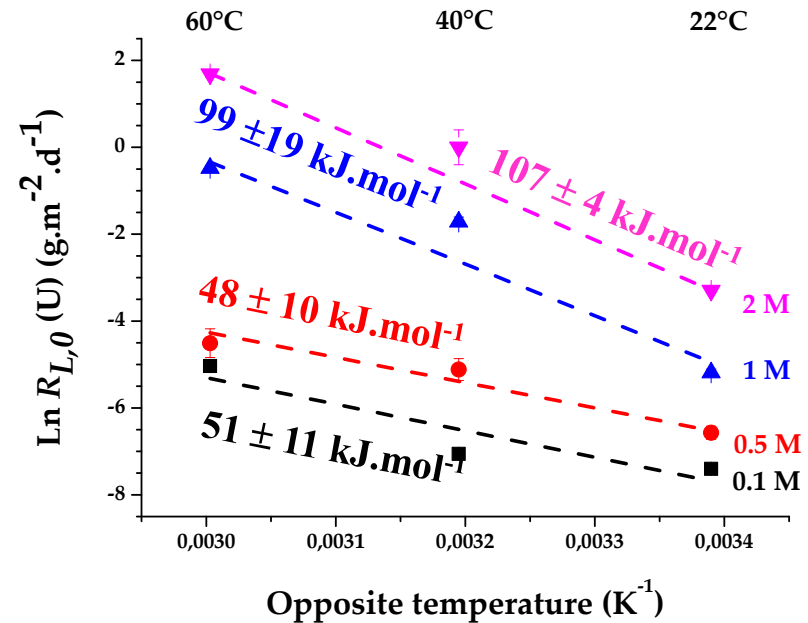
Sintered  $U_{0.9}Ln_{0.1}O_{1.95}$

0.1 – 0.5 – 1 – 2M – 4M  $HNO_3$   
 T : 22°C – 40°C – 60°C  
 Static conditions

$$R_L = k \times e^{-\frac{E_A}{RT}}$$

+

$$R_L = k_T' \times (C_N)^{n'}$$



**Modification of the preponderant dissolution mechanism with acid concentration**

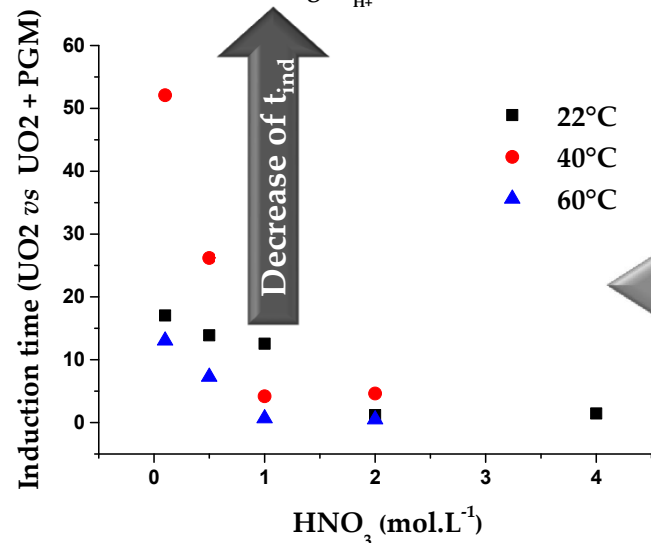
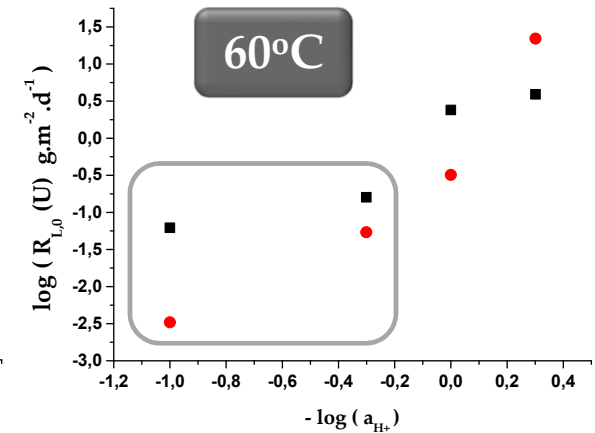
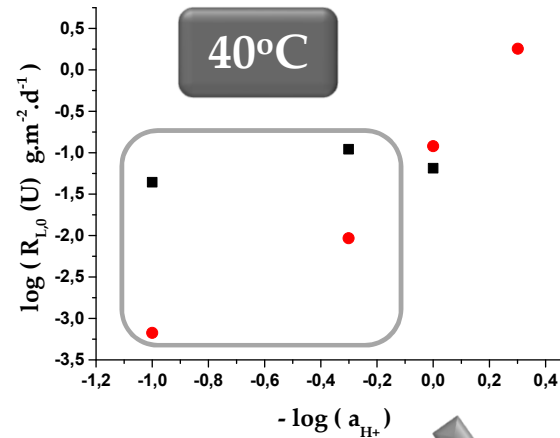
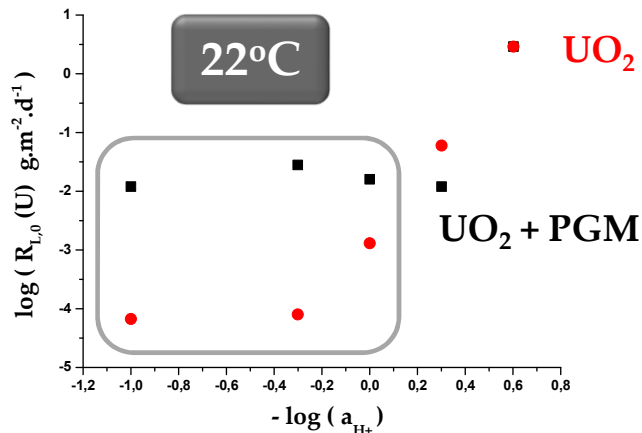
- ✦  $C_{HNO_3} \leq 0.5 \text{ M} \Rightarrow E_{app} \approx 50 \text{ kJ.mol}^{-1}$  and  $n'$  fractional
  - ↳ Surface controlling reactions
- ✦  $C_{HNO_3} > 0.5 \text{ M} \Rightarrow E_{app} \approx 100 \text{ kJ.mol}^{-1}$  and  $n' > 2$ 
  - ↳ Redox controlling reactions

# Dissolution of $\text{UO}_2$ doped with PGM



$\text{UO}_2$  doped with 3% PGM  
Rh (10%) – Ru (55%) – Pd (35%)

0.1 – 0.5 – 1 – 2M – 4M  $\text{HNO}_3$   
T : 22°C – 40°C – 60°C  
Static conditions



Very strong impact of PGM on  $R_{L,0}(\text{U})$   
More important in less acidic media  
Associated to reduction of induction period

T. Cordara, *J. Nucl. Mater.*, 2019, Submitted  
T. Kaczmarek, *PhD*, Univ. Montpellier (2018-2021)

# Dissolution of $\text{UO}_2$ doped with PGM



$\text{UO}_2$  doped with 3 mol% PGM  
Rh (10%) – Ru (55%) – Pd (35%)

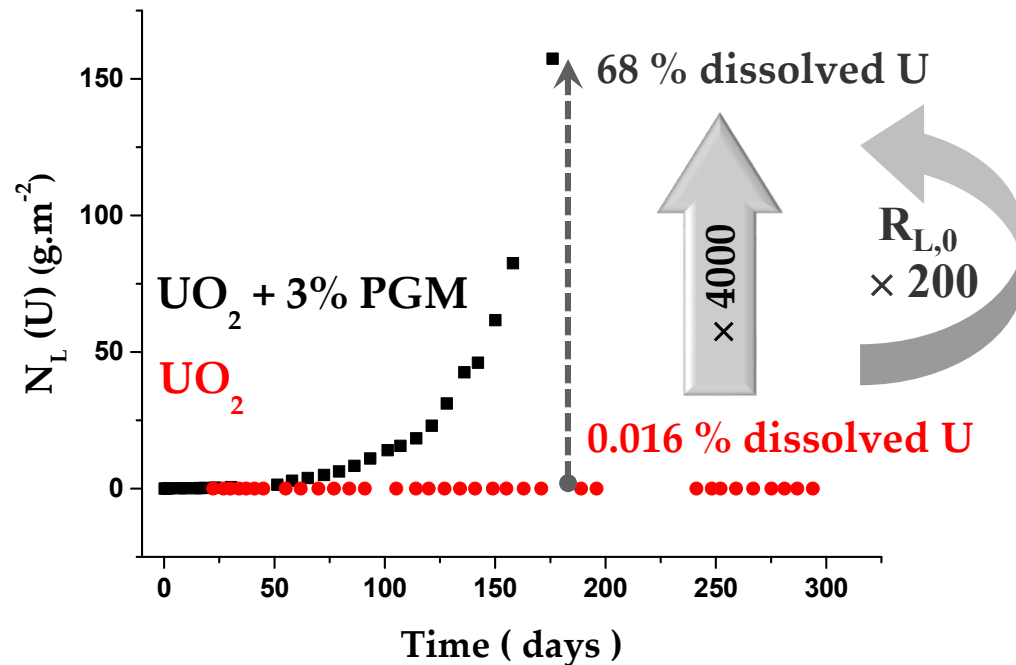
0.1 M  $\text{HNO}_3$  – 22°C  
Static conditions

$\text{UO}_2$  + PGM

$$R_{L,0}(\text{U}) = (1.2 \pm 0.2) \times 10^{-2} \text{ g.m}^{-2}.\text{d}^{-1}$$

$\text{UO}_2$

$$R_{L,0}(\text{U}) = (6.7 \pm 0.3) \times 10^{-4} \text{ g.m}^{-2}.\text{d}^{-1}$$



Strong impact associated to the presence of PGM on  $R_{L,0}(\text{U})$

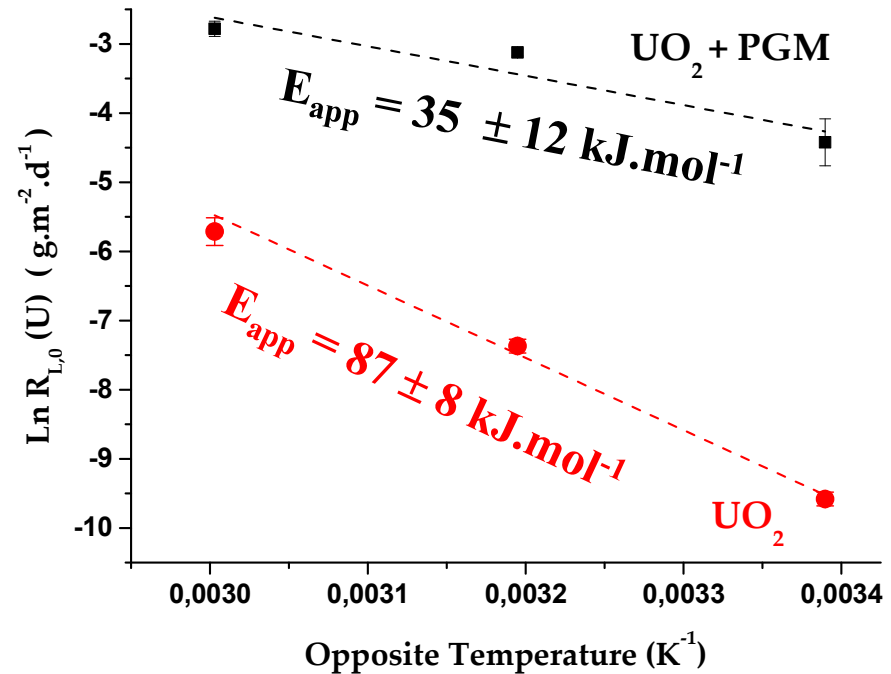
- ↪ Solid contribution @ the solid/liquid interface ?
- ↪ Solution contribution: reduction of  $\text{HNO}_3$  by PGM then production of autocatalytic species in solution (e.g.  $\text{HNO}_2$ ) ?

# Dissolution of $\text{UO}_2$ doped with PGM



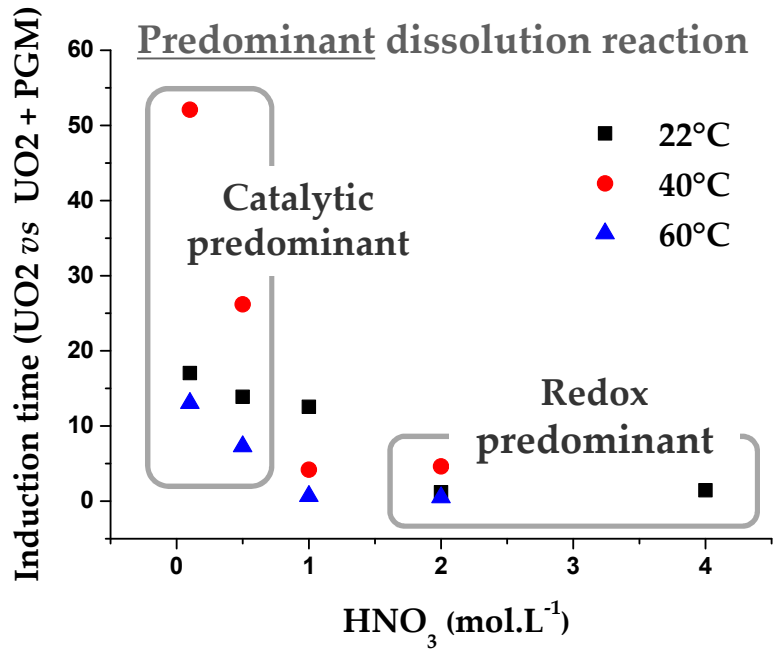
$\text{UO}_2$  doped with 3 mol% PGM  
Rh (10%) – Ru (55%) – Pd (35%)

0.1 M  $\text{HNO}_3$   
T : 22°C – 40°C – 60°C  
Static conditions



**Significant decrease of  $E_A$  with PGM**

**Catalytic process**  
Predominant in less acidic media  
Solution + at solid/liquid interface ?

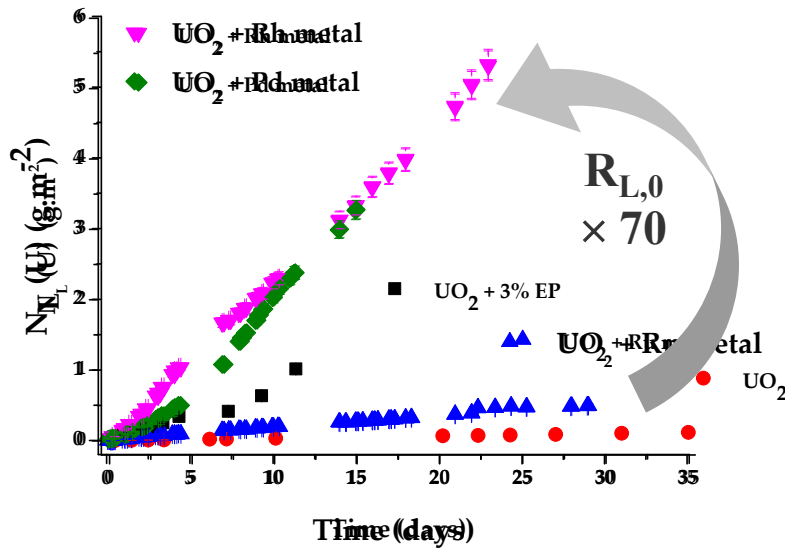
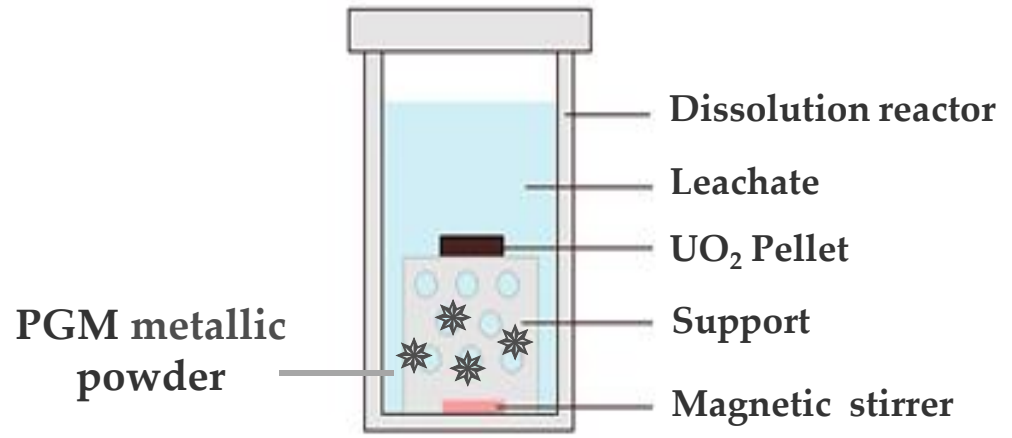


# Impact of PGM : contribution in solution



Sintered  $\text{UO}_2$   
+ PGM (in solution)

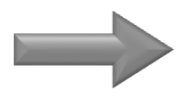
0.1  $\text{HNO}_3$  – 60°C  
Static conditions



Rh:  $R_{L,0} (\text{U}) = (2.3 \pm 0.1) \times 10^{-1} \text{ g.m}^{-2}.\text{d}^{-1}$   
 Pd:  $R_{L,0} (\text{U}) = (9.3 \pm 0.2) \times 10^{-2} \text{ g.m}^{-2}.\text{d}^{-1}$   
 Ru:  $R_{L,0} (\text{U}) = (1.8 \pm 0.1) \times 10^{-2} \text{ g.m}^{-2}.\text{d}^{-1}$

Pure  $\text{UO}_2$   
 $R_{L,0} (\text{U}) = (3.3 \pm 0.1) \times 10^{-3} \text{ g.m}^{-2}.\text{d}^{-1}$

Increase of  $R_{L,0} (\text{U})$  in the presence of PGM powders

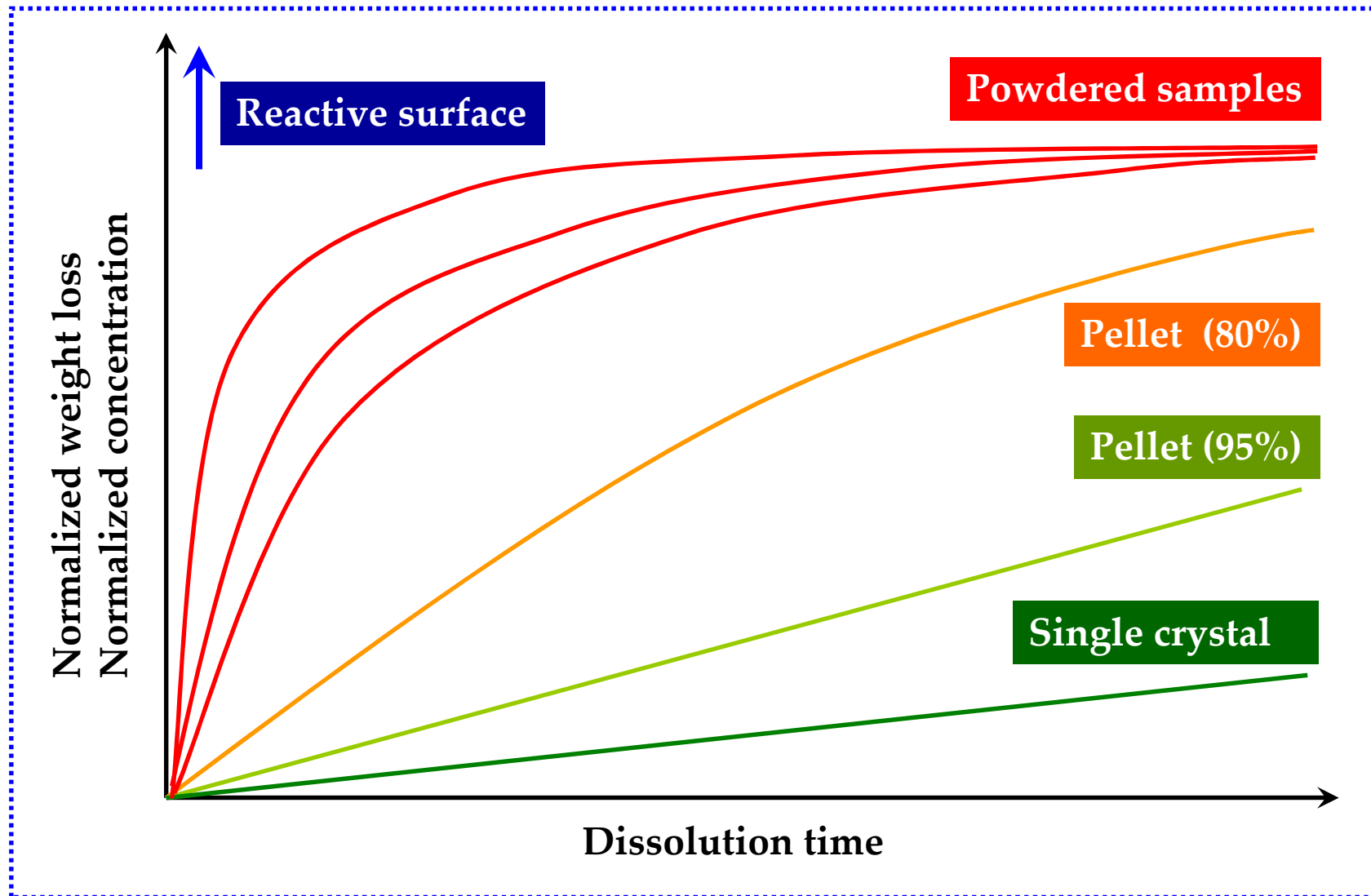


Catalytic effect associated to PGM in solution



# Impact of microstructural parameters on the dissolution kinetics







# Open question :



Is there any role of the microstructure on the material dissolution ?

$$R_L = k_0 \times e^{-E_A/RT} \times a_{H^+}^n \times g(I) \times \prod a_i^{mi} \times f(\Delta_R G) \times f(\text{microstructure}) ??$$

Acidity contribution

Temperature contribution

Ionic strength contribution

Redox, complexing contributions

Deviation from thermodynamic equilibrium

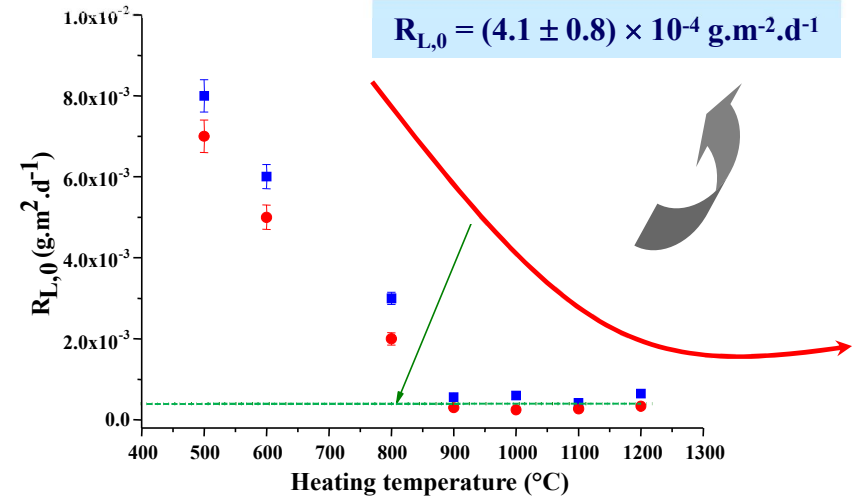
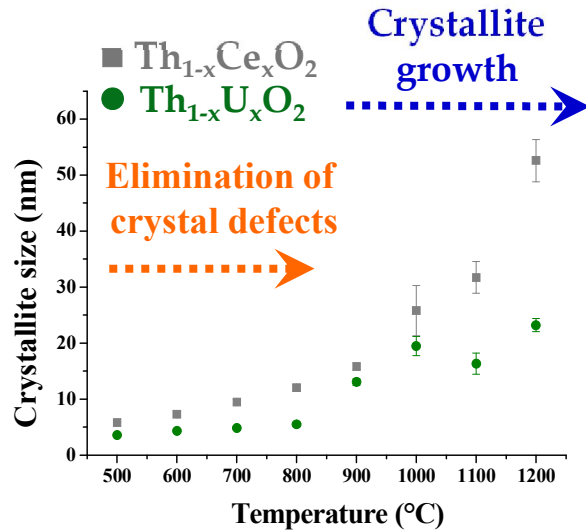
Potential roles of

- ❖ Crystallization state ?
- ❖ Crystallite size ?
- ❖ Grain size ?
- ❖ Densification rate ?
- ❖ Heterogeneity ?
- ❖ ... ?

# Role of microstructural parameters

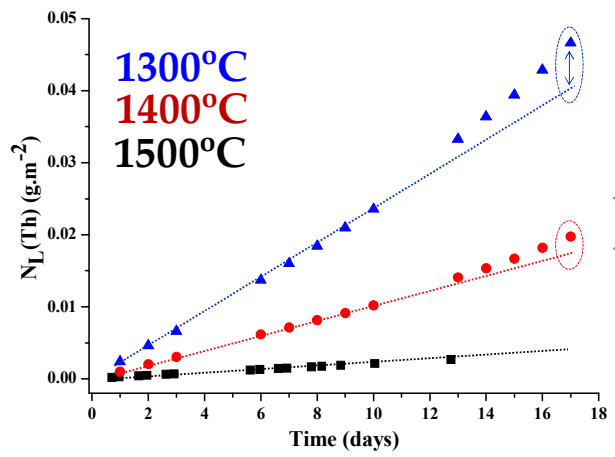
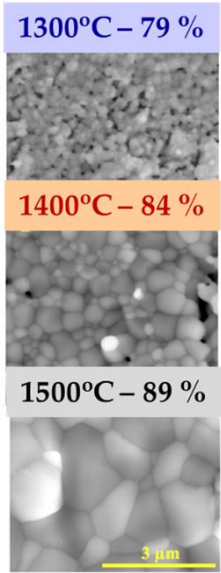


Crystallization state



✦ Crystal defects : moderate impact ✦ Crystallite size : weak impact

Desnification rate



Densification & Grain size ↗  
 $R_{L,0}$  ↘ i.e. durability ↗

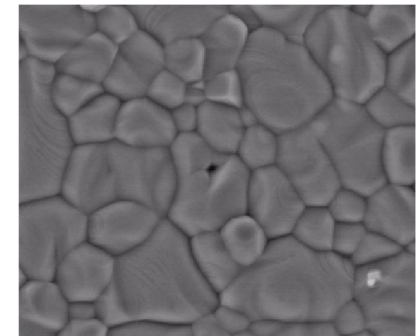
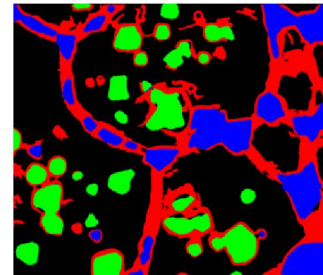
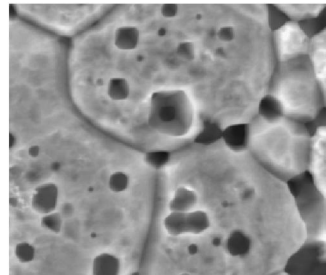
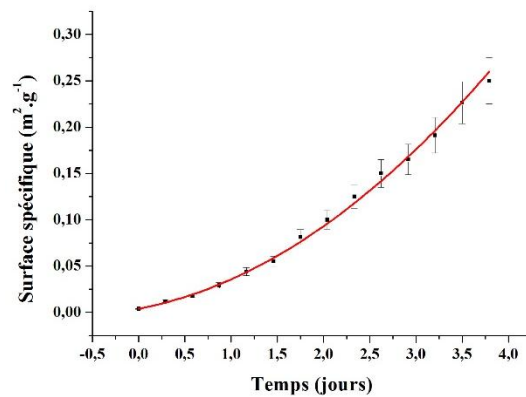
Cohesion & density of GB :  
✦ Moderate influence  
✦ Topological modifications

L. Claparede et al., *Inorg. Chem.*, 50 (2011) 9059 & 50 (2011) 11702, *J. Nucl. Mater.*, 457 (2015) 304

# Microscopic study

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## Microstructural evolution of solid/solution interface



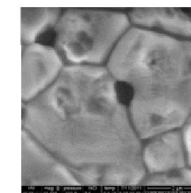
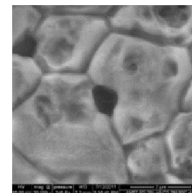
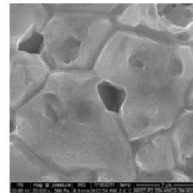
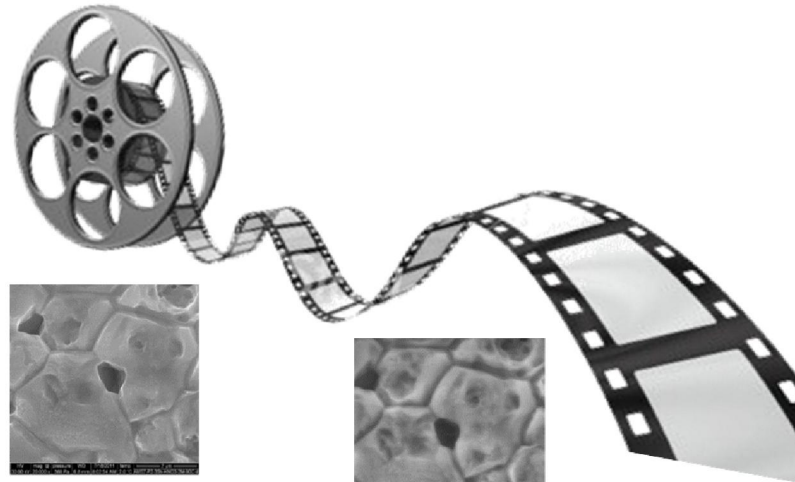
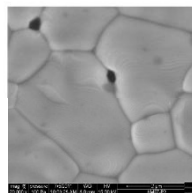
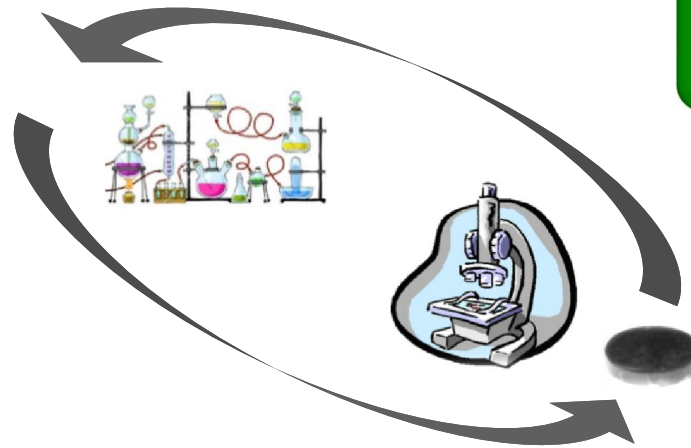
# Operando study of evolving interface during dissolution



## Dissolution tests



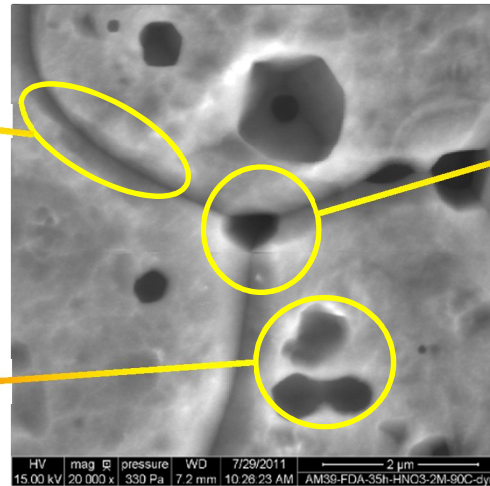
## Environmental SEM observations



$\text{Th}_{0.5}\text{U}_{0.5}\text{O}_2 - 2\text{M HNO}_3 - T = 90^\circ\text{C}$

Grain  
boundarie

Corrosion  
pits



Triple  
junction

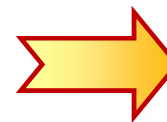
Strong microstructural  
evolution at  
solid/liquid interface

Main  
Open  
Questions

- Good evaluation of the initial reactive surface area ?
- What evolution of reactive surface area during dissolution ?
- What impact on the normalization ?
- What impact on the accuracy of the final obtained results ?

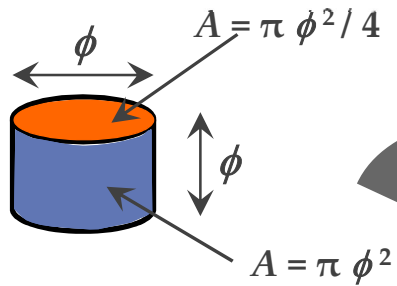
Some  
limitations

- Limited sample amounts
- Expected low  $S_{SA}$  values
- Impact of microstructure



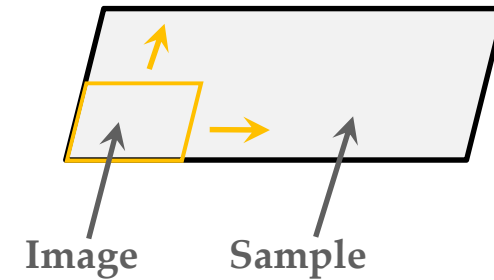
~~Geometric determination  
BET Analyses~~

# Evaluation of Specific Surface Area (SSA) : SESAM method



① Disc surface

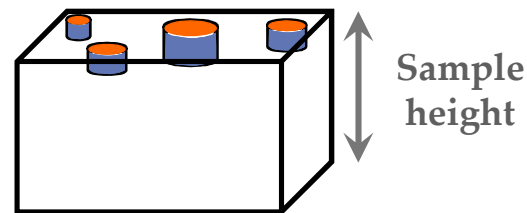
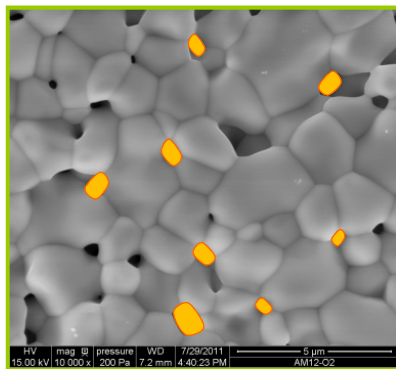
② Integration on image surface



③ Integration on sample surface

④ Integration on sample volume

⑤ Correction by the open porosity ratio



Grayscale threshold  
then binarization:

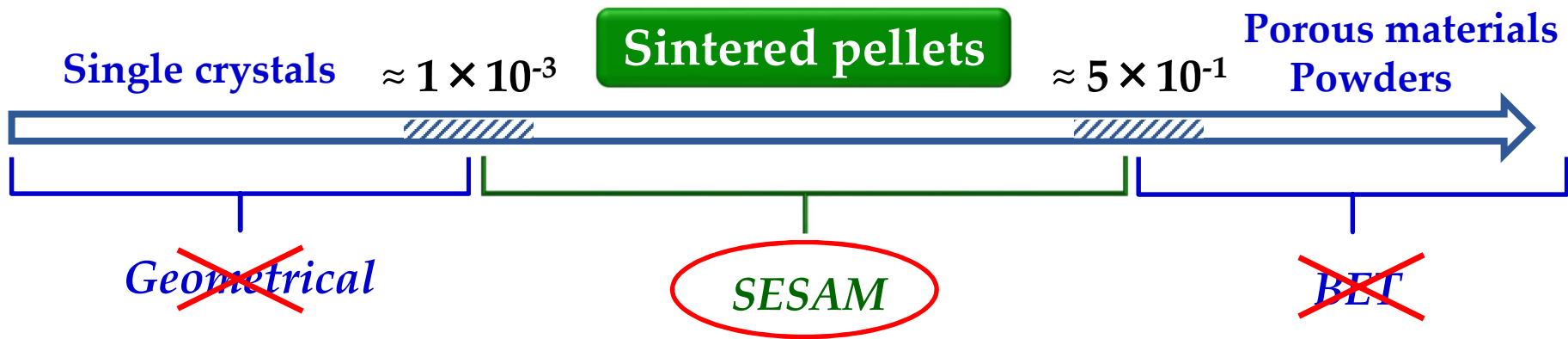
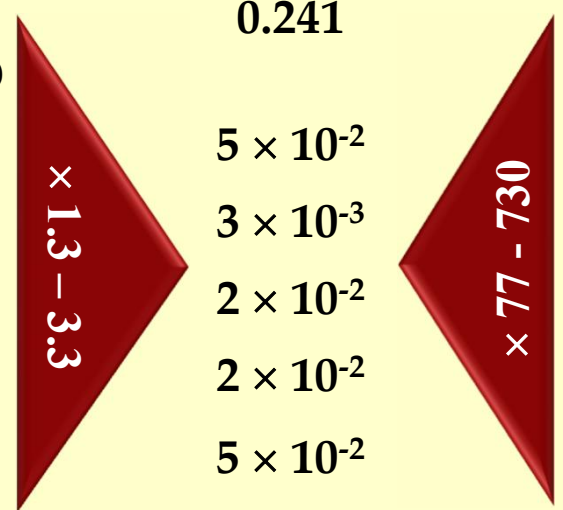
Surface area of the pores

**Estimated specific  
surface area**

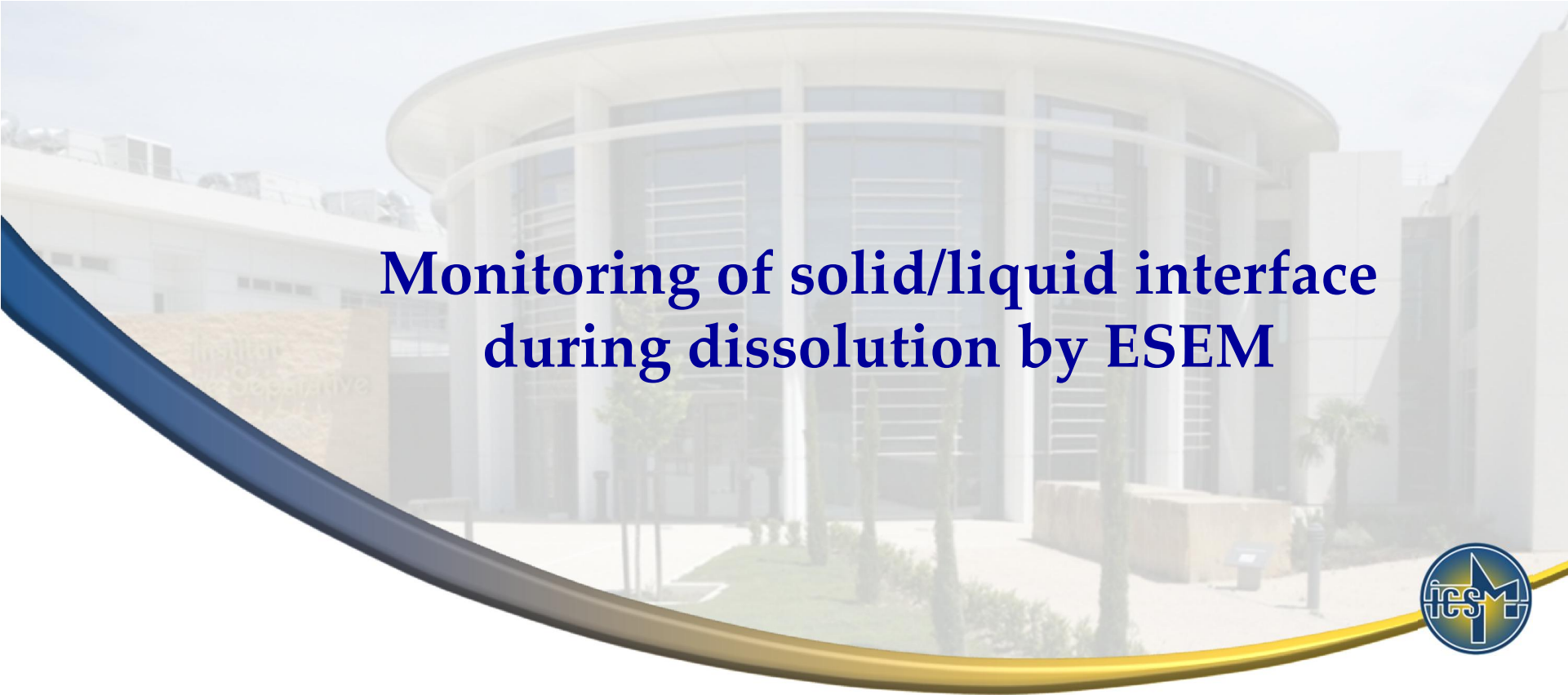
# Evaluation of SSA: SESAM method



Compound	Specific Surface Area ( $\text{m}^2 \cdot \text{g}^{-1}$ )		
	BET method (Kr)	SESAM method	Geometrical
CeO <sub>2</sub>	0.180 (20 pellets, $\approx$ 5 g)	0.241	$3.3 \times 10^{-4}$
UO <sub>2</sub> (reference)	< LoD	$5 \times 10^{-2}$	$2.6 \times 10^{-4}$
Th <sub>0.5</sub> U <sub>0.5</sub> O <sub>2</sub>	< LoD	$3 \times 10^{-3}$	$2.6 \times 10^{-4}$
Th <sub>0.25</sub> U <sub>0.75</sub> O <sub>2</sub>	< LoD	$2 \times 10^{-2}$	$2.6 \times 10^{-4}$
UO <sub>2</sub> + PGM	< LoD	$2 \times 10^{-2}$	$2.6 \times 10^{-4}$
U <sub>0.9</sub> Ln <sub>0.1</sub> O <sub>1.95</sub>	$1.5 \times 10^{-2}$ (5 pellets, $\approx$ 1 g)	$5 \times 10^{-2}$	$2.9 \times 10^{-4}$



\* T. Cordara, PhD, ICSM/CEA, Univ. Montpellier, Nov. 2017



**Monitoring of solid/liquid interface  
during dissolution by ESEM**



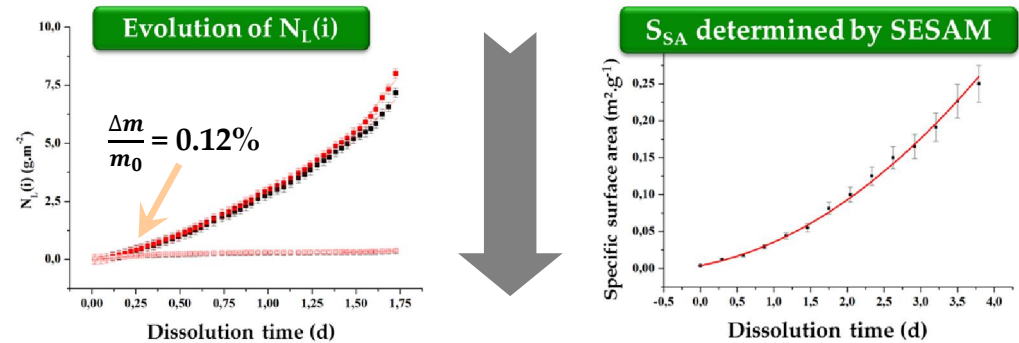
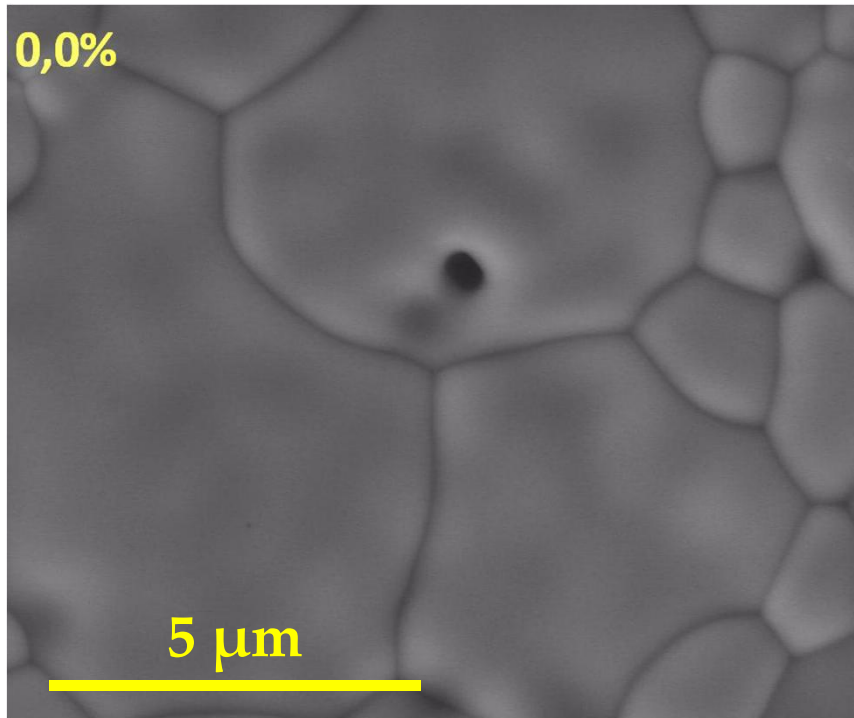


# Monitoring of solid/liquid interface during dissolution by ESEM



$\text{Th}_{0.5}\text{U}_{0.5}\text{O}_2$  pellet  
 2M  $\text{HNO}_3$  –  $T = 90^\circ\text{C}$   
 Time intervals : 7 hours

Heterogeneous dissolution  
 Preferential dissolution zones :  
 GB, triple junctions, pores  
 Formation of corrosion pits

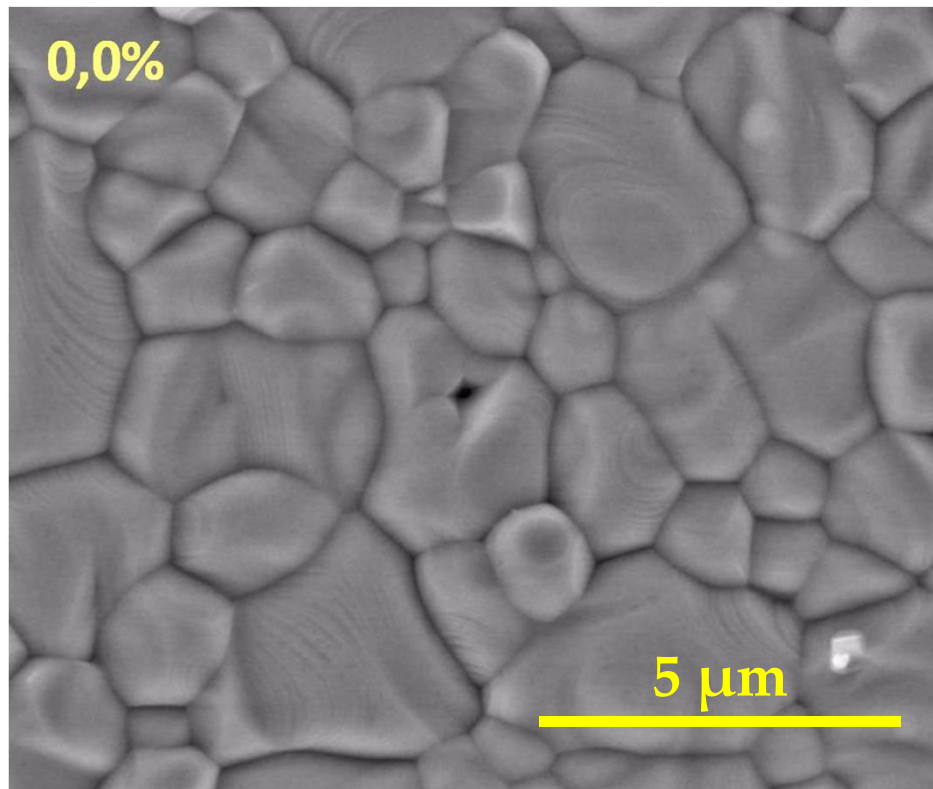


Surface reactions  
 controlling dissolution  
 Correction of S rapidly required  
 $\Delta m/m_0 = 3\% \Leftrightarrow S/S_0 \approx 20$

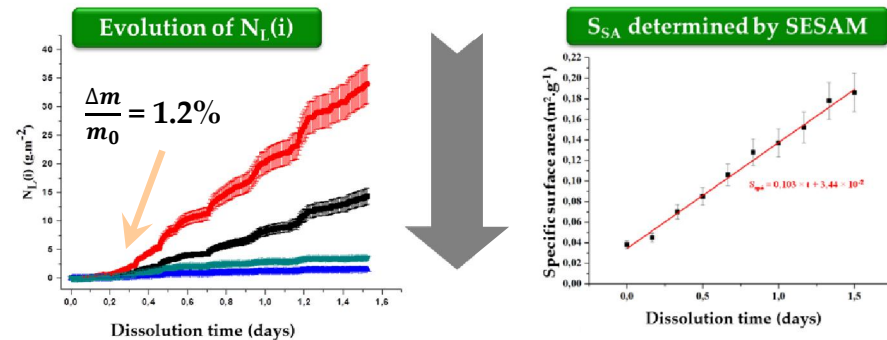
# Monitoring of solid/liquid interface during dissolution by ESEM



$\text{Th}_{0.25}\text{U}_{0.75}\text{O}_2$  pellet / 4M  $\text{HNO}_3$  – RT  
Time intervals : 1 hour



Homogenous dissolution  
Degradation of the  
entire interface

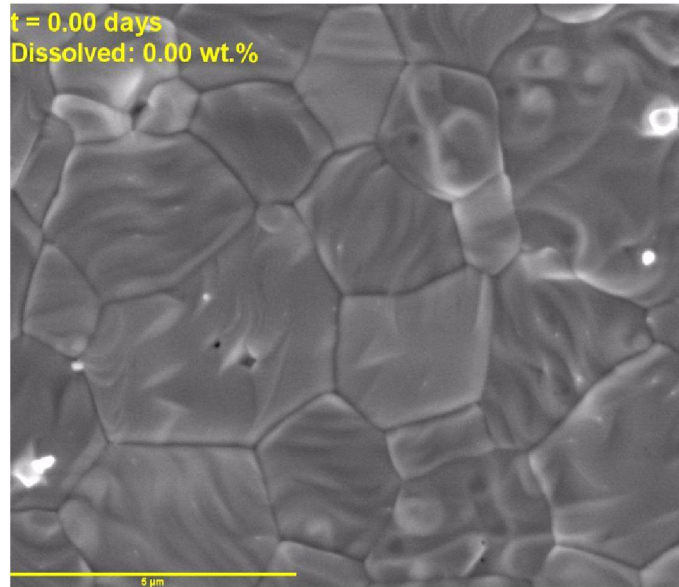


Redox reactions  
controlling dissolution  
 $\Delta m/m_0 = 22\% \Leftrightarrow S/S_0 \approx 5$

# Monitoring of solid/liquid interface during dissolution by ESEM

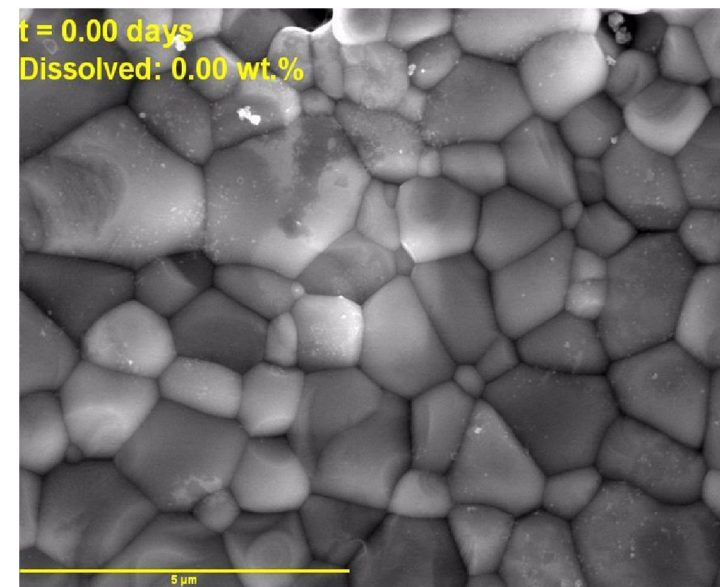


**UO<sub>2</sub> pellet**  
**1 M HNO<sub>3</sub> – T = 60°C**  
**Dissolution time : 3.2 days**



**Homogeneous dissolution**  
**Microstructural evolution**  
**Oxidation of U(IV)**

**U<sub>1.9</sub>Ln<sub>0.1</sub>O<sub>1.95</sub> pellet**  
**1 M HNO<sub>3</sub> – T = 60°C**  
**Dissolution time : 1.6 days**



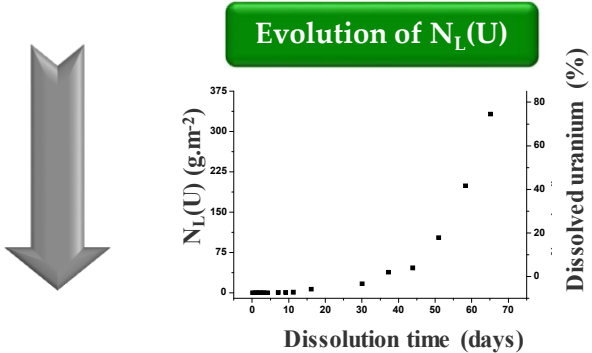
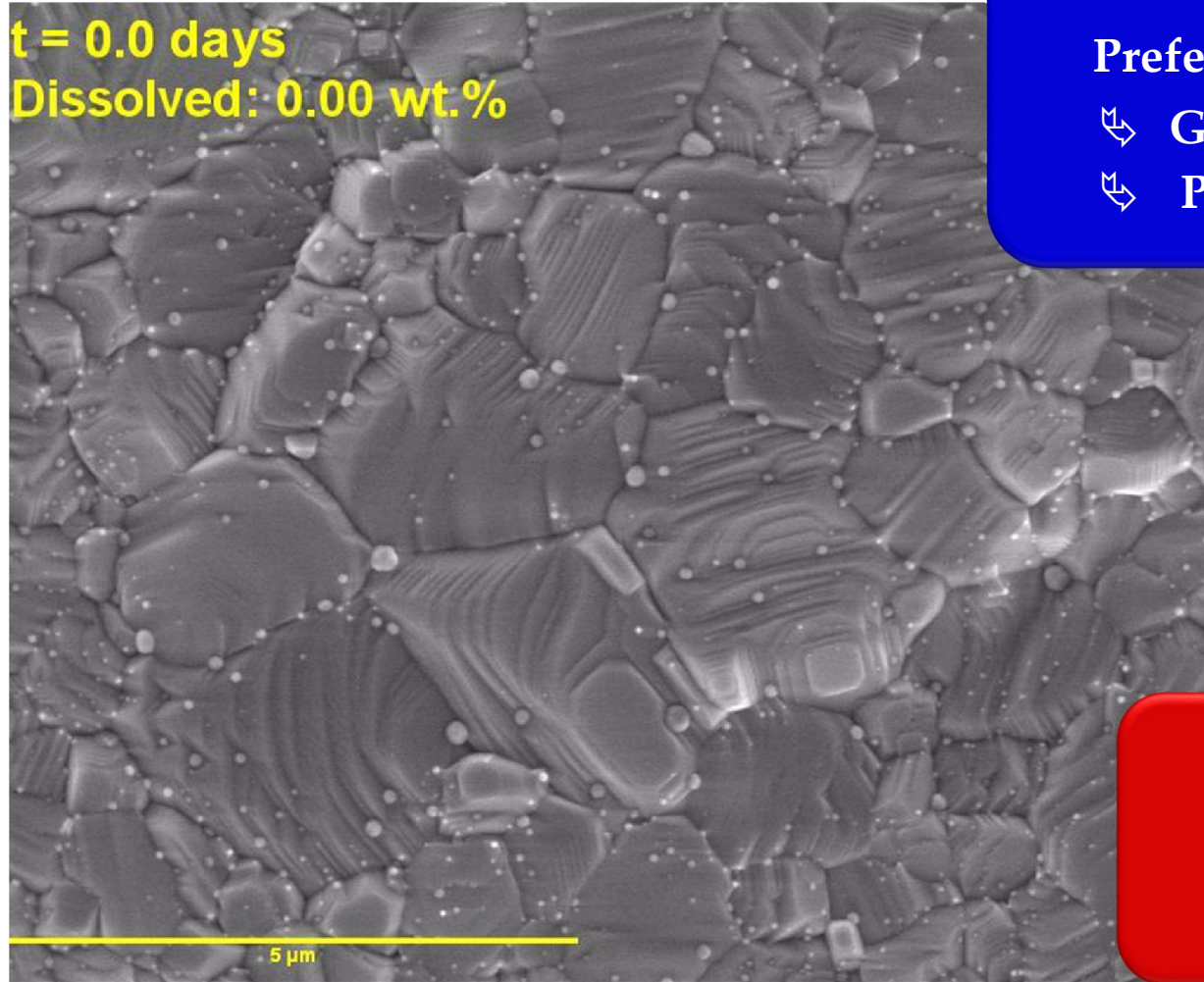
**Preferential dissolution zones (GB)**  
**Ln(III) – enrichment in GB**  
**↳ Decrease of energy of cohesion**

# Impact of PGM : contribution at the solid/solution interface



**UO<sub>2</sub> pellet with 3 mol.% PGM**  
**0.1 M HNO<sub>3</sub> – T = 60°C**  
**Dissolution time : 58 days**

**Heterogeneous dissolution**  
**Preferential dissolution zones :**  
↗ GB, triple junctions, pores  
↗ PGM / UO<sub>2</sub> / Solution interface



**Surface reactions**  
**controlling dissolution**  
**Impact of PGM**  
**@ Solid/Liquid interface**

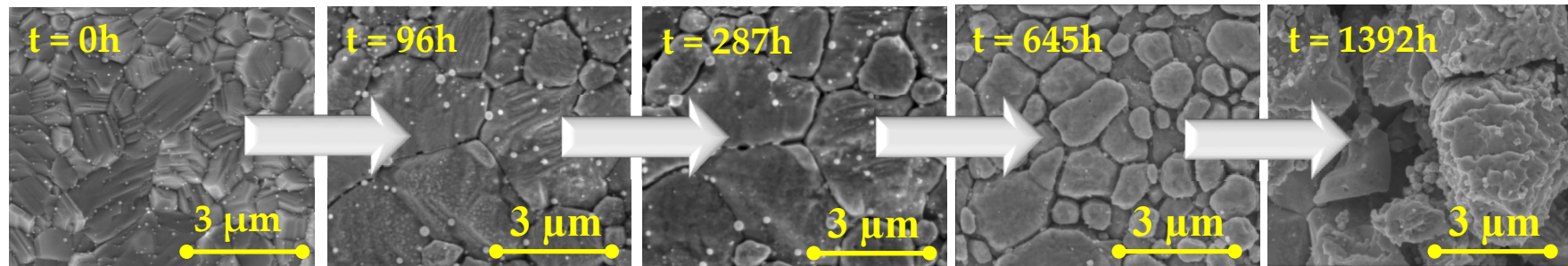
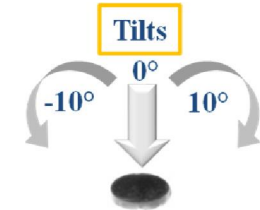
T. Cordara, PhD, ICSM/CEA, Univ. Montpellier, Nov 2017

# 3D analysis of the dissolution of $\text{UO}_2$ + PGM

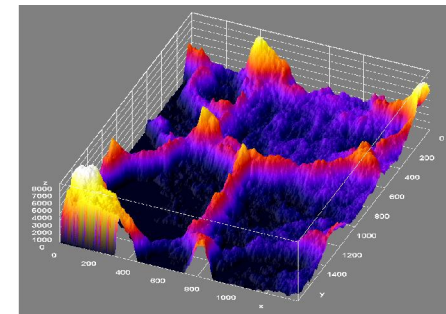
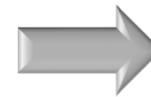
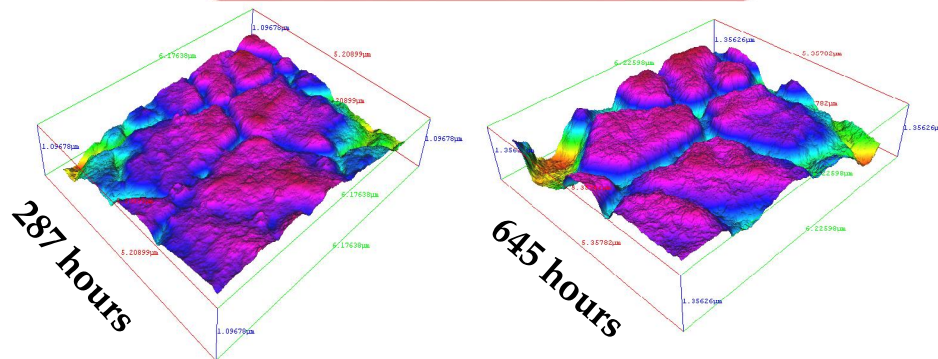


Sintered  $\text{UO}_2$  doped with  
3 mol% Rh-Ru-Pd  
0.1 M  $\text{HNO}_3$  – 60°C

*Operando* ESEM:  
Sequence of stereoscopic images



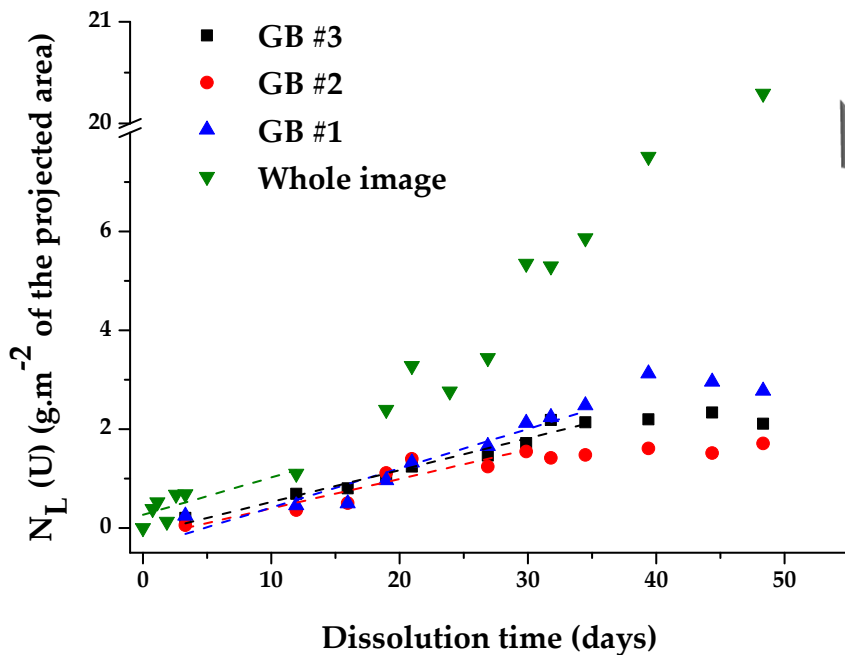
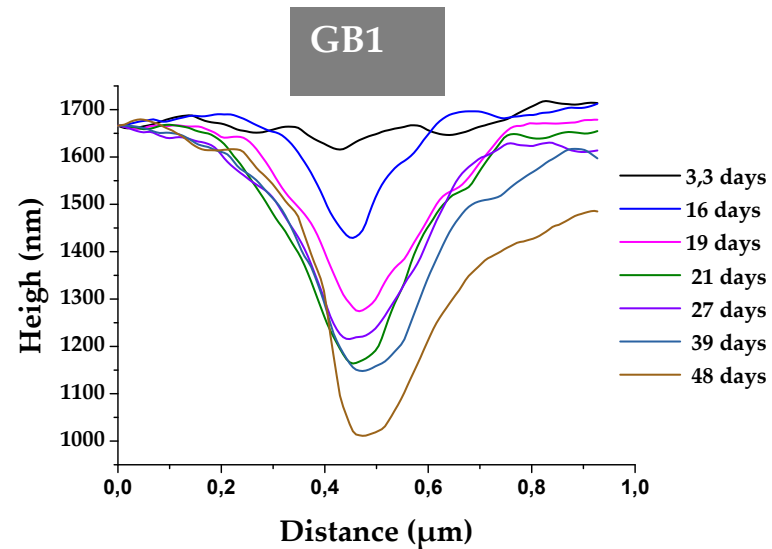
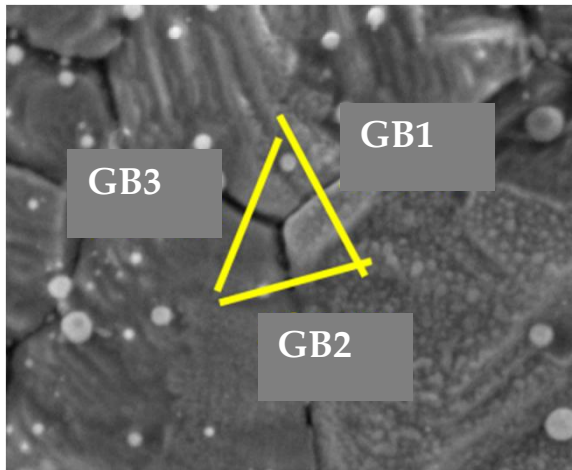
## 3D Reconstruction



Zones of interest: Access to  
dissolved volumes

\* T. Cordara, PhD, Univ. Montpellier, Nov. 2017

# 3D analysis of the dissolution of $\text{UO}_2 + \text{PGM}$



$$R_{L,0} (\text{global}) = 7.4 \times 10^{-2} \text{ g.m}^{-2}.\text{d}^{-1}$$

$$R_{L,0} (\text{GB}) = (6.5 \text{ to } 8.4) \times 10^{-2} \text{ g.m}^{-2}.\text{d}^{-1}$$



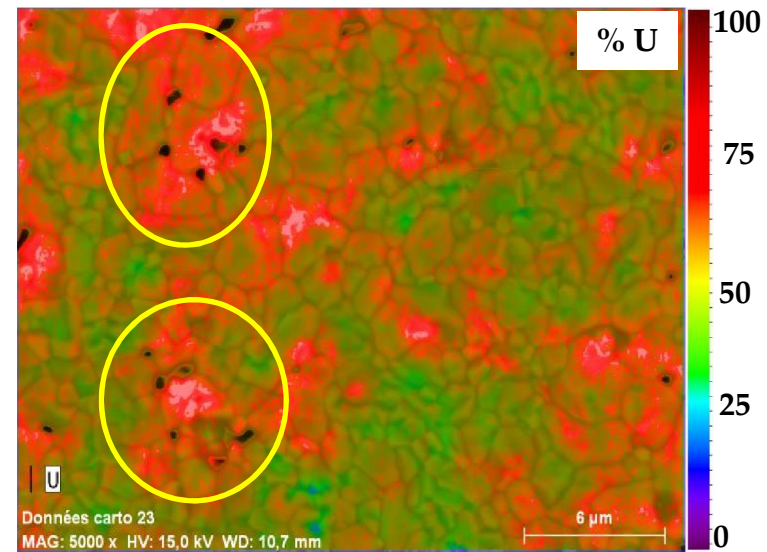
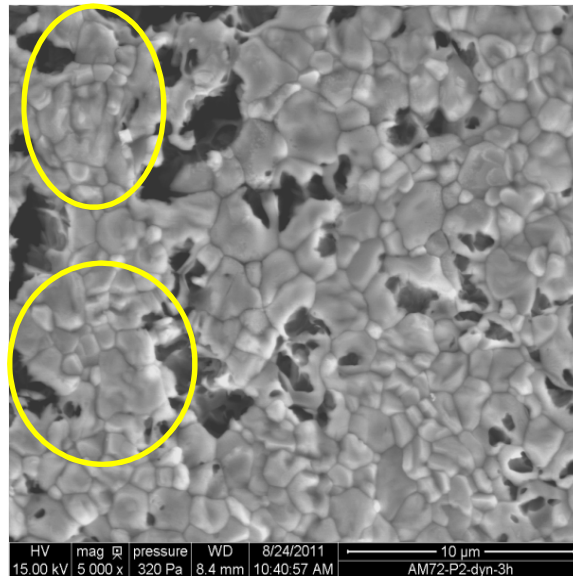
**Starting global dissolution directly linked to the dissolution of GB**



# Impact of the heterogeneity on the dissolution



$\text{Th}_{0.5}\text{U}_{0.5}\text{O}_2 - 2\text{M HNO}_3 - \text{T} = 90^\circ\text{C} - \text{Heterogeneous material}$



↓

**Preferential dissolution  
of U-enriched zones**

↘

**Strong modifications of  
the surface composition**

↘

**Strong impact on the  
reactive surface area**

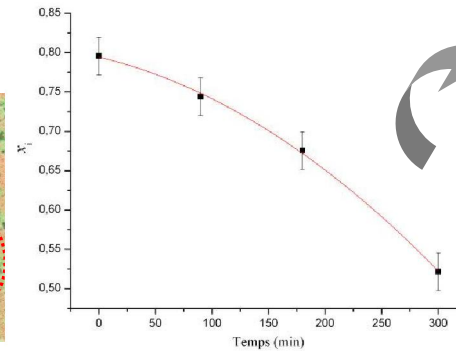
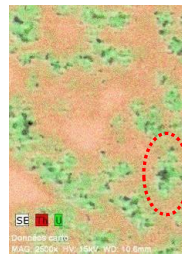
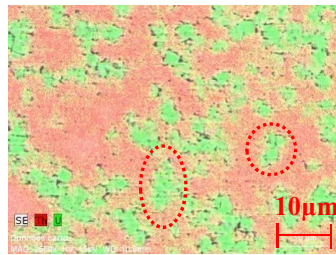


# Impact of heterogeneity

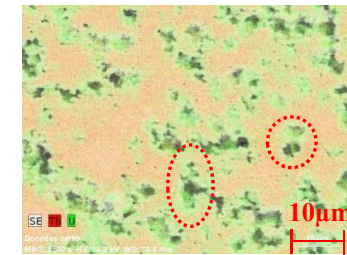
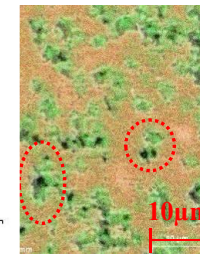


Th<sub>0.5</sub>U<sub>0.5</sub>O<sub>2</sub> – Heterogeneous material – 2M HNO<sub>3</sub>

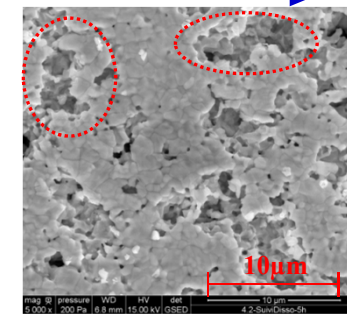
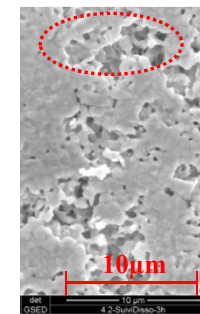
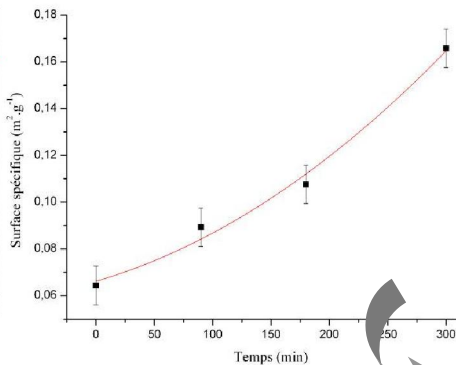
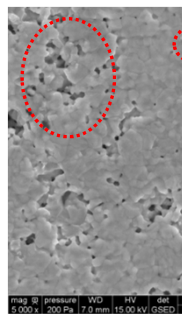
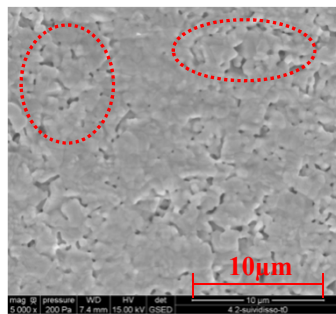
## Evolving composition : $f_i(t)$



$$f_i(t) = -1.9 \times 10^{-6} t^2 - 3.4 \times 10^{-4} t + 0.8$$



t = 0 min.
t = 90 min.
t = 180 min.
t = 300 min.



## Evolving surface : $S(t)$

$$S(t) = (6.1 \times 10^{-7} t^2 + 1.5 \times 10^{-4} t + 0.07) m(t)$$

Macroscopic level  
incongruent dissolution  
(preferential U release)



Image  
Analysis



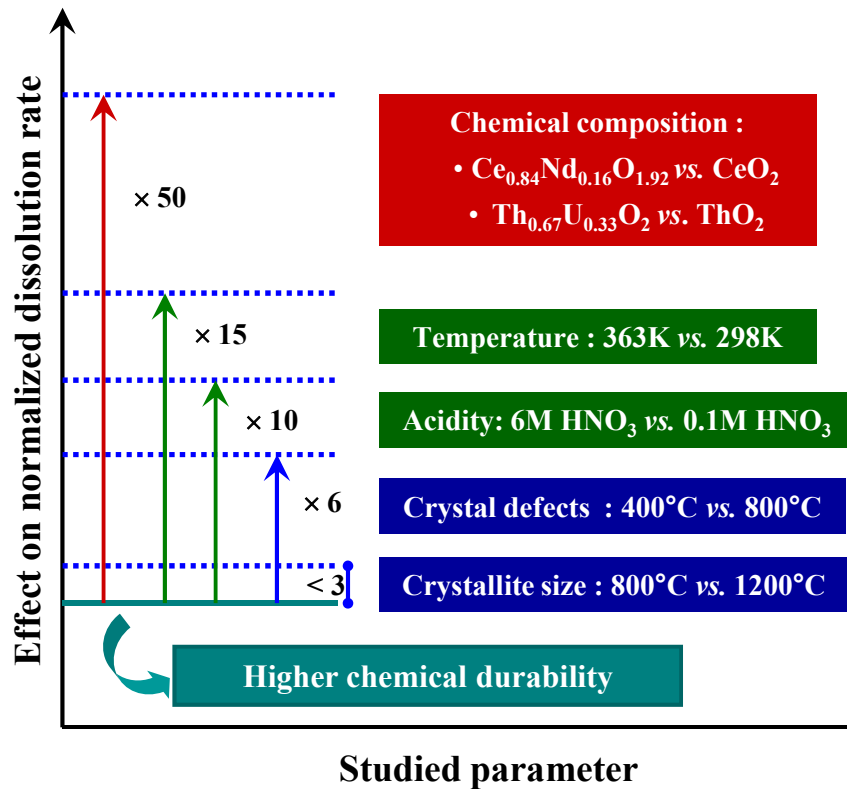
Microscopic level  
congruent dissolution  
(U enriched zones)



# Main Conclusions & Overviews



# Relative contribution of parameters during dissolution



Chemical composition :

- $Ce_{0.84}Nd_{0.16}O_{1.92}$  vs.  $CeO_2$
- $Th_{0.67}U_{0.33}O_2$  vs.  $ThO_2$

Temperature : 363K vs. 298K

Acidity: 6M  $HNO_3$  vs. 0.1M  $HNO_3$

Crystal defects : 400°C vs. 800°C

Crystallite size : 800°C vs. 1200°C

- ❖ Crystallization state
- ❖ Crystallite size / grain size
- ❖ Densification rate / GB density
- ❖ Heterogeneity (incl. surface)
- ❖ ...

$$R_L = k_0 \times e^{-E_A/RT} \times a_{H^+}^n \times g(I) \times \prod a_i^{mi} \times f(\Delta_R G) \times f(\text{microstructure})$$



- ❖ **Discrimination of the impact of PGM's on the global dissolution process**
  - ↪ Individual role of Ru, Rh, Pd (solubilized redox species)
  - ↪ Impact of the presence of secondary phases (i.e. perovskite for Mo)
- ❖ **Precise impact of nitrogen based species coming from reduction of HNO<sub>3</sub>**
  - ↪ Combined effect (increase of production by PGM's)
- ❖ **Particular behavior of (U,Ce)O<sub>2</sub> solid solutions**
  - ↪ Impact of the "sample history" on the speciation of U and Ce
  - ↪ Consequence of redox reactions U(IV)/Ce(IV), U(V)/Ce(IV) @ the interface
- ❖ **Impact of structural parameters**
  - ❖ Effect of oriented MO<sub>2</sub> surface (single crystals) on the dissolution kinetics
  - ❖ Impact of dislocation loops at the interface
- ❖ **Impact of porosity (confined volumes) on the development of reactions**
- ❖ **Impact of irradiation and irradiation/dissolution couplings**

Thank you for listening...

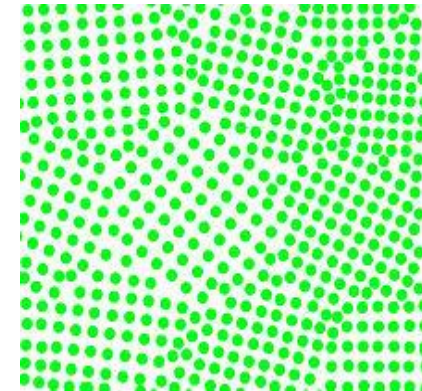
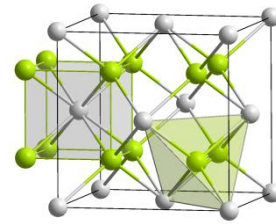
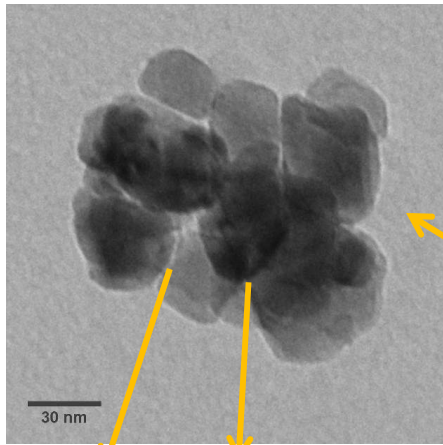




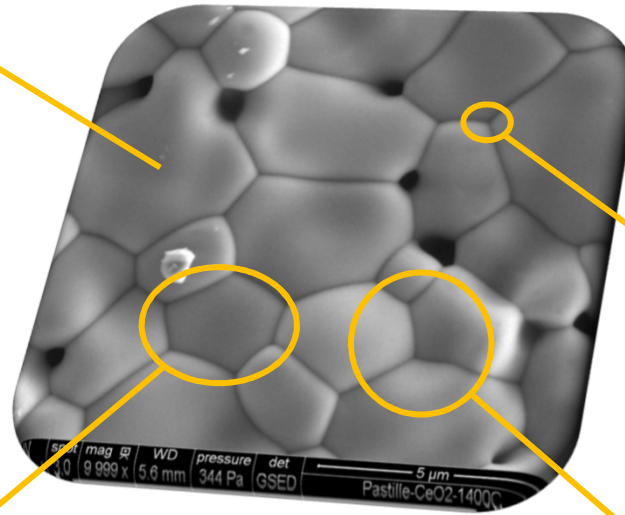
# Microstructural control : about the terminology ...



❖ **Cristallites**



❖ **Crystallite boundaries**



❖ **Triple junctions**

❖ **Grains**

❖ **Grain boundaries**