

# SCHOOL on Generation IV reactors fuel cycle

## Thermodynamic aspects of nuclear fuels (Modelling)

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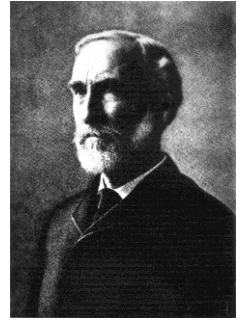
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13-17 May 2019, Delft, The Netherlands

# Outline

- 1 - The Calphad method
- 2 - Basic Gibbs energy models
- 3 - Modelling of the U-Pu-O system
  - 3.1 U-O
  - 3.2 Pu-O
  - 3.3 U-Pu-O
- 4 - Calculations on a irradiated MOX fuel
- 5 - Conclusion

# The Gibbs energy



Josiah Willard  
Gibbs  
(1839-1903)

- The Gibbs energy of a system is defined by:

$$G = H - TS = U + PV - TS$$

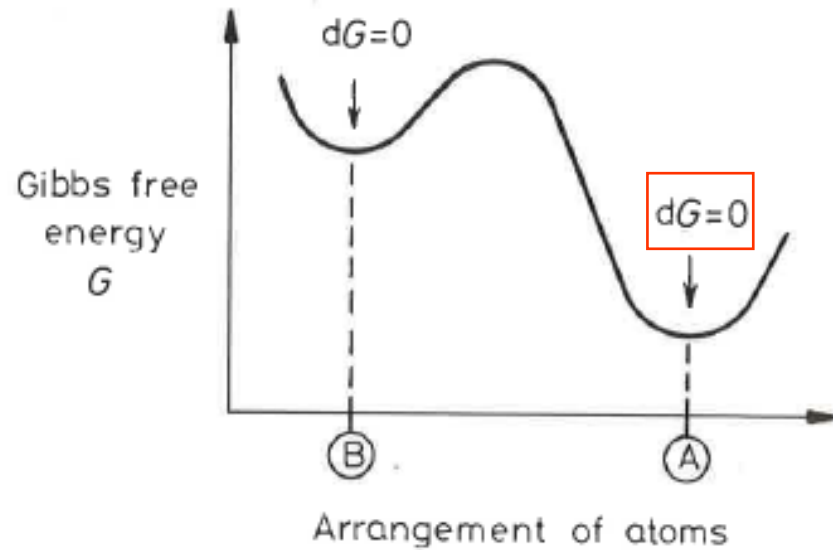
- $H$  is the **enthalpy**  $\Rightarrow$  heat content of the system
- $T$  is the temperature
- $S$  is the **entropy** of the system  $\Rightarrow$  randomness of the system
- $U$  is the internal energy of the system  $\Rightarrow$   $\underbrace{\text{kinetic}}_{\text{vibrations}}$  and  $\underbrace{\text{potential}}_{\text{bonds}}$  energies of atoms
- $P$  is the pressure
- $V$  is the volume
  
- $G$  is the **key function** in thermodynamics of materials
- At constant temperature and pressure, a closed system (fixed mass and composition) will be in stable **equilibrium** if it has the **lowest value of the Gibbs energy**:

$$dG = 0$$

# Thermodynamic equilibrium

- $G = H - TS$

⇒ Compromise between low enthalpy and high entropy



⇒ The A configuration is the lowest possible value of  $G$  ⇒ Equilibrium

⇒ The B configuration is a metastable equilibrium state (local equilibrium)

⇒ The intermediate configurations are unstable

⇒ The rate at which the system will reach the equilibrium is not provided by thermodynamics

# The Gibbs energy

⇒ Thermodynamic potential at given P, T, n

$$G = U + PV - TS = H - TS$$

- $H = U + PV$  ➔ Enthalpy ( $U$ : internal energy)
- $\left(\frac{\partial G}{\partial T}\right)_{P, N_i} = -S$  ➔ Entropy
- $\left(\frac{\partial G}{\partial N_i}\right)_{T, P, N_{j \neq i}} = \mu_i$  ➔ Chemical potential
- $C_P = -T \left(\frac{\partial^2 G}{\partial T^2}\right)_{P, N_i}$  ➔ Heat capacity

⇒ Key thermodynamic properties to describe the phases

# Gibbs energy minimization

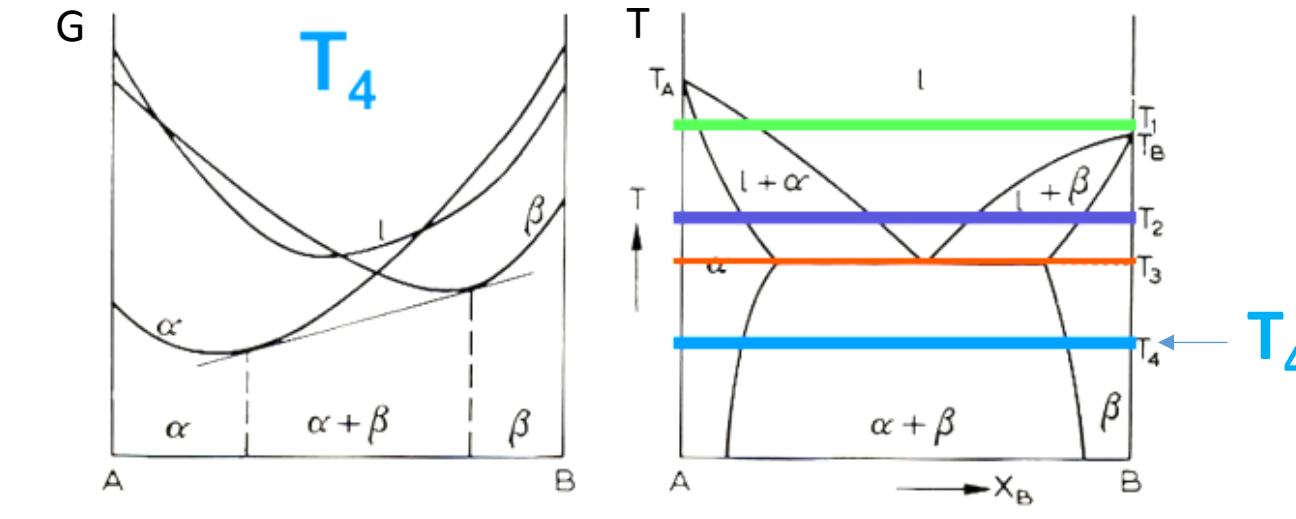
- At given  $T, P, n_i$  the **equilibrium** corresponds to the **minimum** of the Gibbs energy of the system:

$$dG = 0$$

- The Gibbs energy of the system  $G$  is a linear combination of the Gibbs energies of the phases,  $G_m^\varphi$  :

$$G = \sum_i m^\varphi G_m^\varphi$$

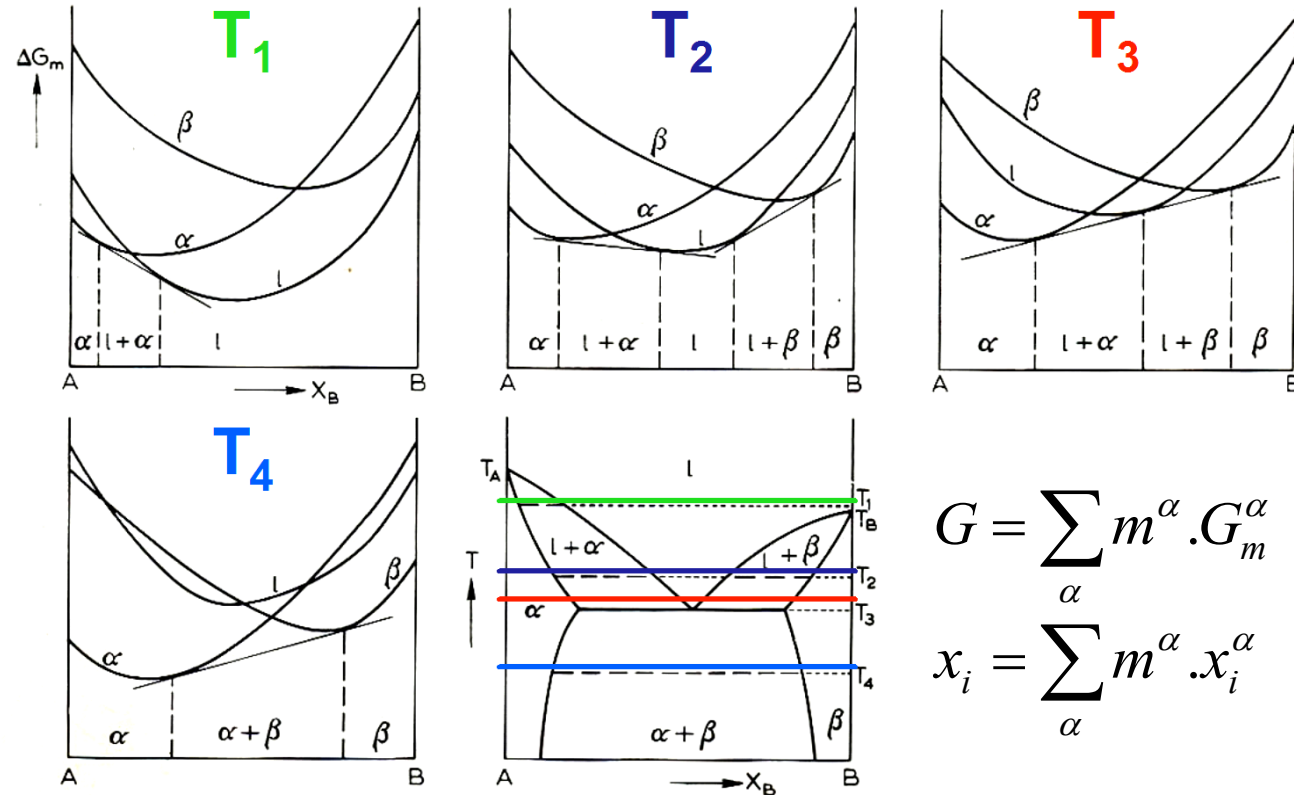
$m^\varphi$ : mole fraction of phase  $\varphi$



# CALPHAD (CALCulation of PHAse Diagram) method:

- At given  $T, P, n_i$  the **equilibrium** is calculated by **minimization of** the Gibbs energy of the system:  $dG = 0$

⇒ Coupling Gibbs energies and phase diagrams



$$G = \sum_{\alpha} m^{\alpha} \cdot G_m^{\alpha}$$

$$x_i = \sum_{\alpha} m^{\alpha} \cdot x_i^{\alpha}$$

➔  $\min(G) = \min \left( \sum_{\alpha} m^{\alpha} G_m^{\alpha} (T, p, x_i^{\alpha} \text{ or } y_k^{(l,\alpha)}) \right)$

The phase diagram can be calculated from the phases Gibbs energies

# Calphad modeling

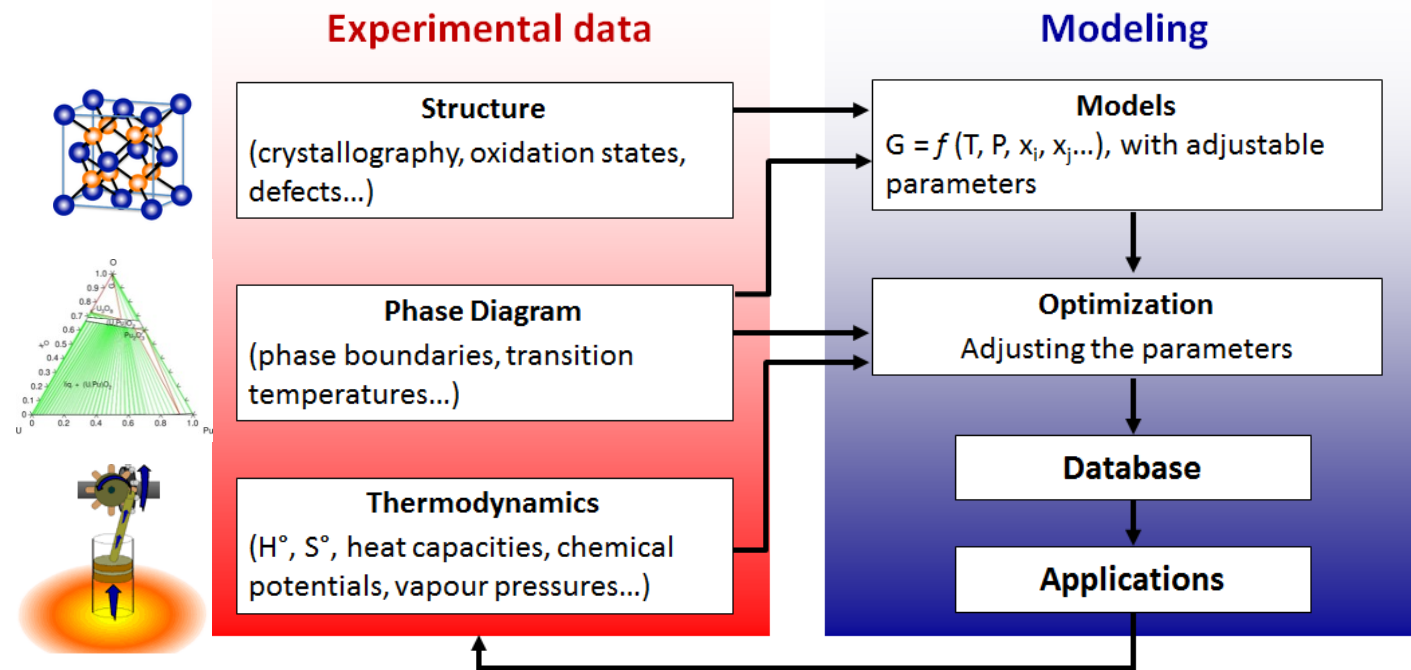
## ➔ Assessment procedure

- Mathematical functions are chosen to describe the Gibbs energy of the phases

$$G_m^\alpha(T, p, x_i^\alpha \text{ or } y_k^{(l, \alpha)})$$

- The variables are **assessed by a least-square minimizing method** to reproduce the available thermodynamic and phase diagram data
- For a multi-component system, the equilibrium is calculated by **extrapolation** from models for binary and ternary sub-systems

➔ **Good prediction of both phase diagram and phase thermodynamic data for multi-component systems**



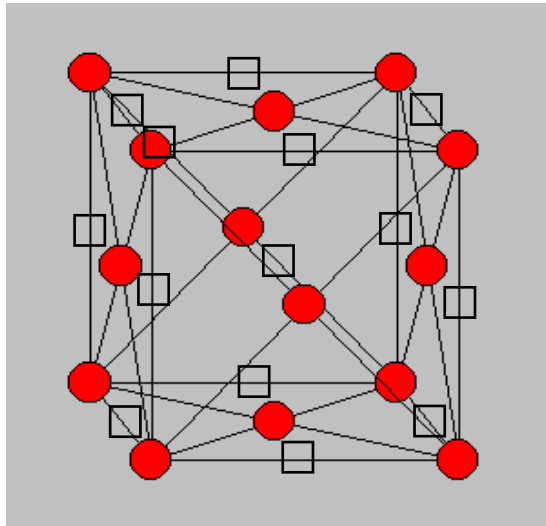
➔ SATA (School on Advanced Thermodynamic Assessment)



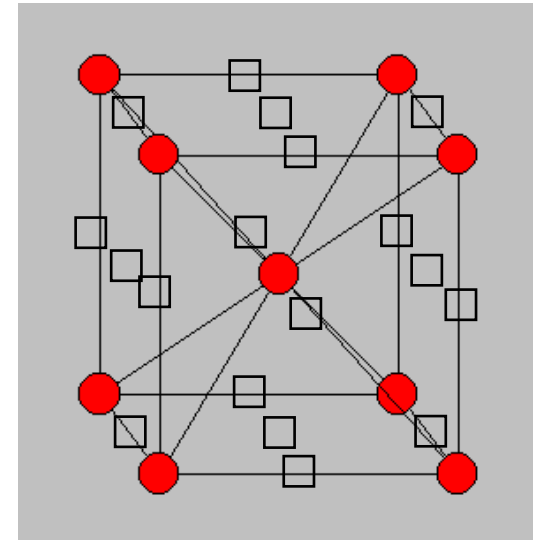
# ➔ Sublattice model to describe the phases

- Connection between thermodynamics and crystallography ➔ **Sublattice modeling**
  - **The sublattices correspond to equivalent positions** i.e. sites belonging to the same Wyckoff position
  - To simplify the model, several sets of equivalent positions may be combined and treated as a single sublattice
- ➔ **A single sublattice model is used for all the phases with the same crystalline structure**

FCC (Faced centered cubic)

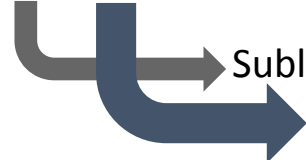


BCC (Body centered cubic)



● Atom A  
□ Vacant site (Va)

(A)1(Va)1



Sublattice 1: Substitutional site for metals A, B, C ....

Sublattice 2: Interstitial site for O, C, N ...

(A)1(Va)3



# Model for phases with a fixed composition

⇒ Pure elements, stoichiometric compounds

- $G_m^\alpha$  is the molar Gibbs energy of the phase  $\alpha$ , referred to the enthalpy of the pure elements in their stable state at 298.15 K and 1 bar (**SER: Stable Element Reference**).

$$\Rightarrow G_m^\alpha - \sum_i b_i H_i^{SER} = a_0 + a_1 T + a_2 T \ln T + a_3 T^2 + a_4 T^{-1} + a_5 T^3 \dots$$

$b_i$  is the stoichiometric coefficient of the element  $i$  in the phase  $\alpha$



$$H = G + T S = G - T \left( \frac{\partial G}{\partial T} \right)_{p, N_i}, \quad S = - \left( \frac{\partial G}{\partial T} \right)_{p, N_i}, \quad C_p = -T \left( \frac{\partial^2 G}{\partial T^2} \right)_{p, N_i}$$



$$H_m^\alpha - \sum_i b_i H_i^{SER} = a_0 - a_2 T - a_3 T^2 + 2a_4 T^{-1} - 3a_5 T^3 + \dots$$

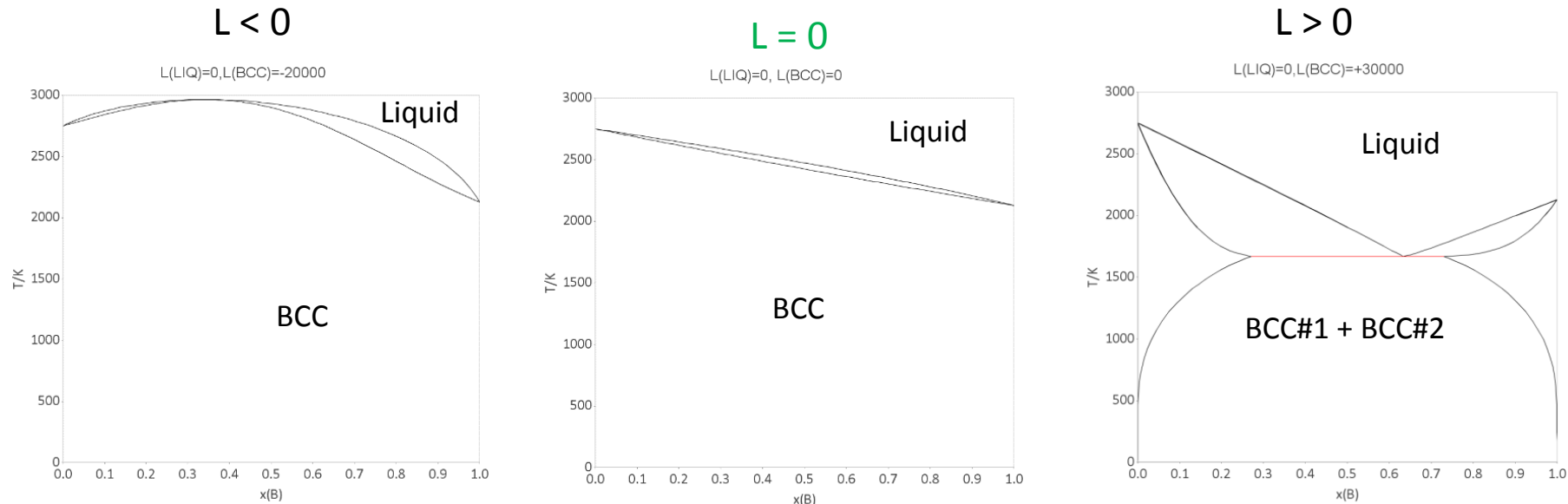
$$S_m^\alpha = -a_1 - a_2(1 + \ln T) - 2a_3 T + a_4 T^{-2} - 3a_5 T^2 + \dots$$

$$C_p^\alpha = -a_2 - 2a_3 T - 2a_4 T^{-2} - 6a_5 T^2 + \dots$$

# Model for a regular solution (A,B)

Influence of the interaction parameter  $L_{AB}$  on the phase diagram

$$G_m^\alpha = \underbrace{x_A \circ G_A + x_B \circ G_B}_{\text{G reference}} + \underbrace{RT(x_A \ln x_A + x_B \ln x_B)}_{\text{G ideal}} + \underbrace{x_A x_B L_{AB}}_{\text{G excess}}$$



**L(BCC) = -20000**  
Stabilization



**L(BCC) = 0**  
Ideal solution



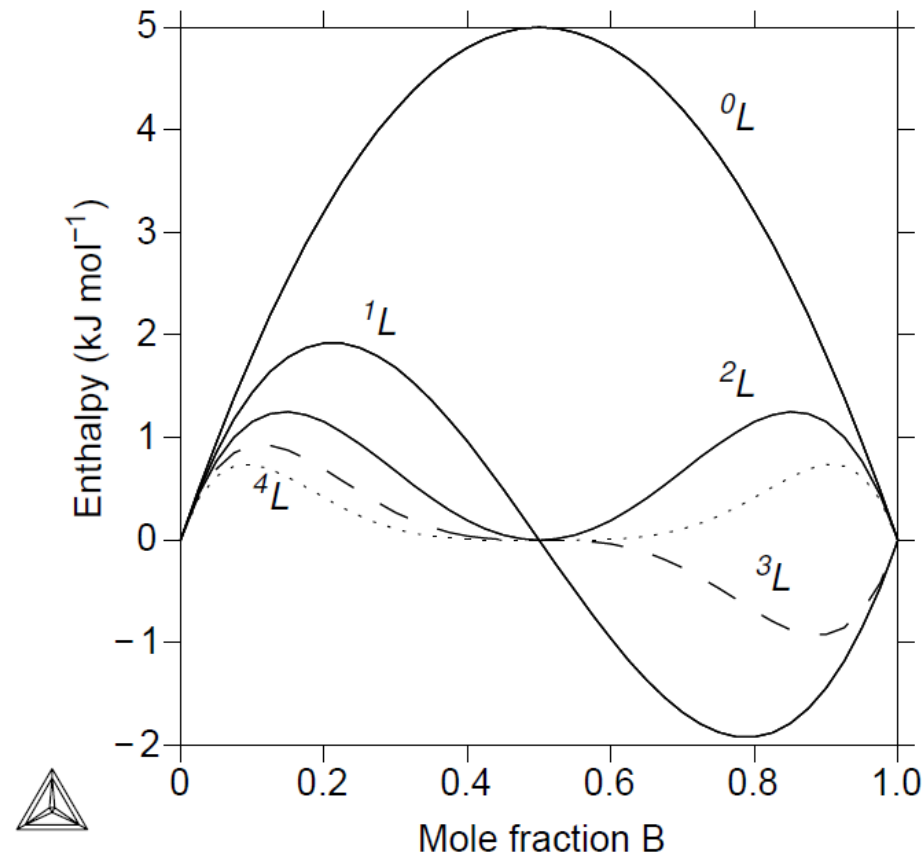
**L(BCC) = +30000**  
Phase separation  
(Miscibility gap)

# Model for a real solution (A,B)

Dependence in composition of the interaction parameter → **Redlich-Kister**

$$G_m^\alpha = x_A \text{ }^\circ G_A + x_B \text{ }^\circ G_B + RT(x_A \ln x_A + x_B \ln x_B) + x_A x_B L_{AB}$$

$$\rightarrow L_{AB} = \sum_{\nu=0} (x_A - x_B)^\nu \nu L_{AB} = {}^0L_{AB} + {}^1L_{AB} (x_A - x_B) + {}^2L_{AB} (x_A - x_B)^2 + \dots$$

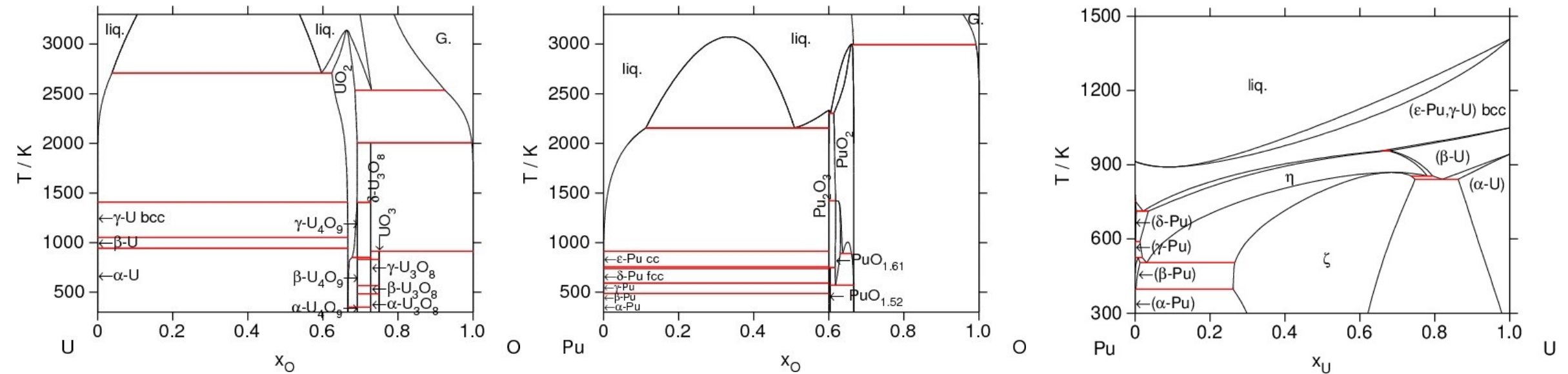


$$\nu L_{AB} = 20000$$

# How to model the U-Pu-O system ?

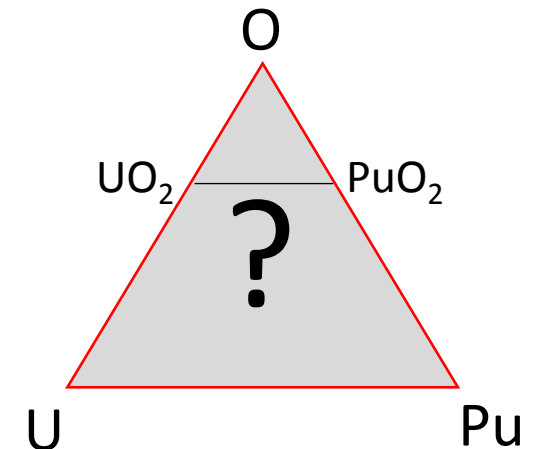
## 1<sup>st</sup> step: modeling of the U-O, Pu-O and U-Pu binary sub-systems

- Binary interaction parameters for solutions
- G functions for the binary compounds



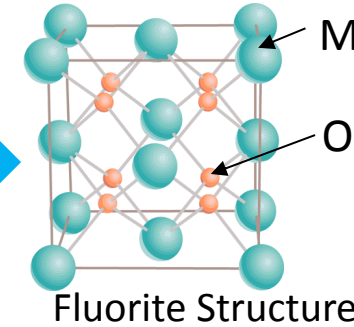
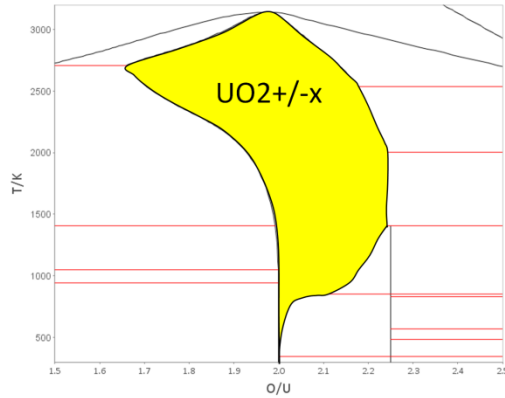
## 2<sup>nd</sup> step: modeling of the U-Pu-O ternary system

- Ternary interaction parameters for solutions
- G functions for the ternary compounds



# ➔ Sublattice model for non stoichiometric $\text{UO}_{2\pm x}$

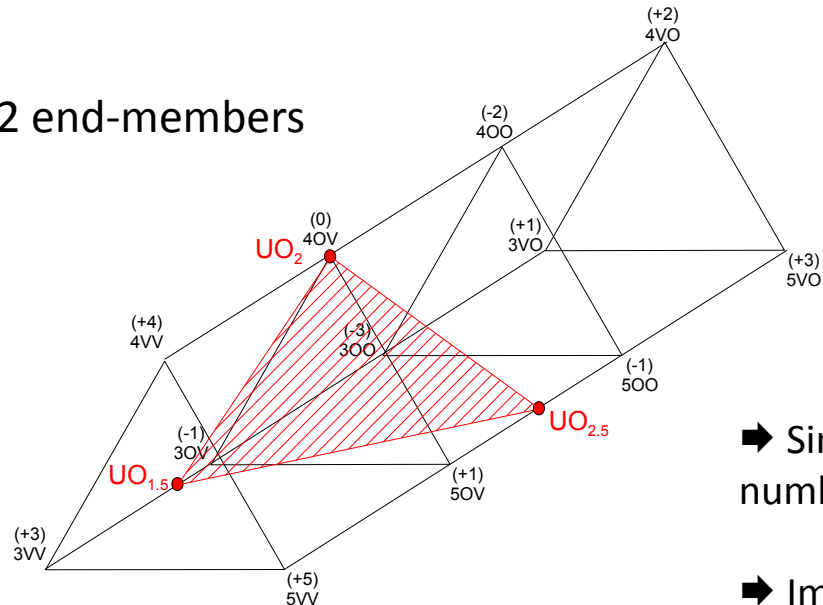
■ Uranium dioxide  $\text{UO}_{2\pm x}$  with fluorite structure has a large oxygen composition range



■ **Compound Energy Formalism + Three sublattice model ( $\text{U}^{+3}, \text{U}^{+4}, \text{U}^{+5}$ ) ( $\text{O}^{-2}, \text{Va}$ )<sub>2</sub> ( $\text{O}^{-2}, \text{Va}$ )**

➔ Formation of oxygen vacancies and interstitials compensated by reduction/oxidation of  $\text{U}^{+4}$  into  $\text{U}^{+3}/\text{U}^{+5}$

12 end-members



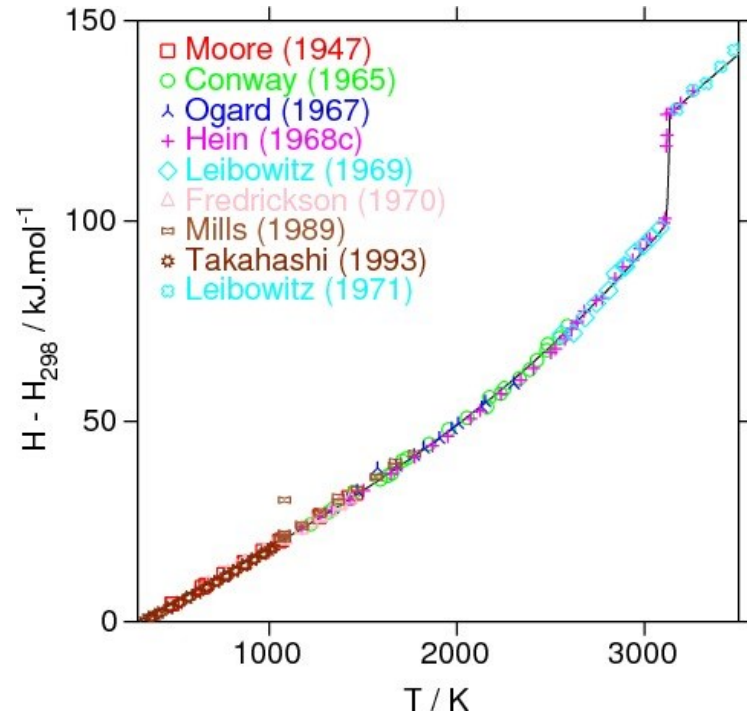
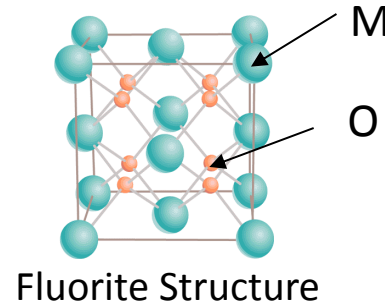
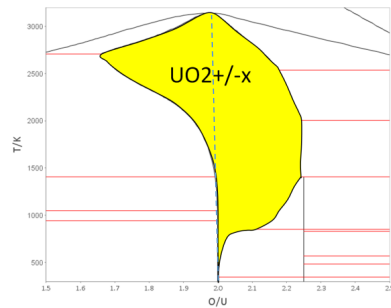
$$G_m^{\text{UO}_2} = y_3 y_O y'_V G_{3OV}^0 + y_3 y_V y'_V G_{3VV}^0 + y_3 y_O y'_O G_{3OO}^0 + y_3 y_V y'_O G_{3VO}^0 + y_4 y_O y'_V G_{4OV}^0 + y_4 y_V y'_V G_{4VV}^0 + y_4 y_O y'_O G_{4OO}^0 + y_4 y_V y'_O G_{4VO}^0 + y_5 y_O y'_V G_{5OV}^0 + y_5 y_V y'_V G_{5VV}^0 + y_5 y_O y'_O G_{5OO}^0 + y_5 y_V y'_O G_{5VO}^0 + RT(y_3 \ln y_3 + y_4 \ln y_4 + y_5 \ln y_5) + 2RT(y_O \ln y_O + y_V \ln y_V) + RT(y'_O \ln y'_O + y'_V \ln y'_V) + G_m^{\text{Excess}}$$

➔ Simple relationships between G parameters for the end-members are fixed to decrease the number of variables to be optimized

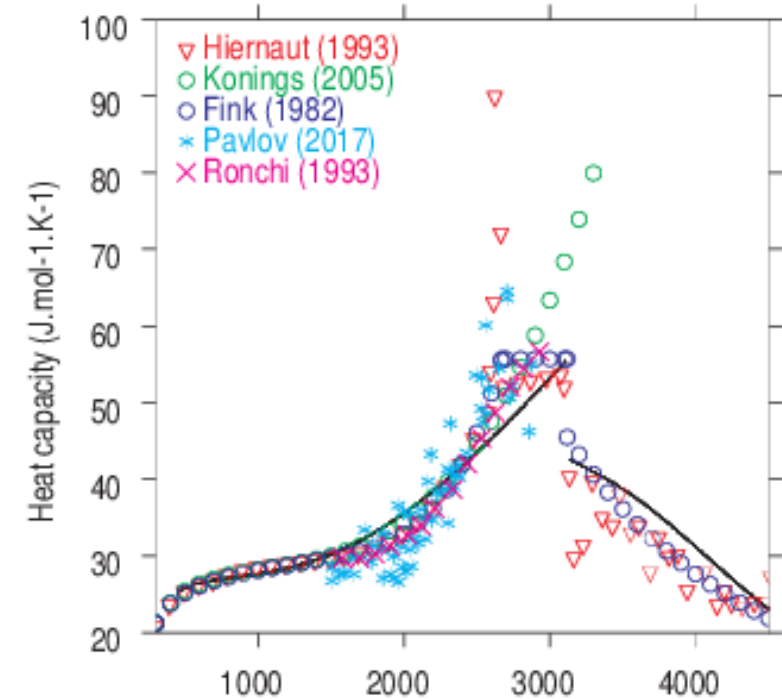
➔ Important parameters are:  $G(\text{UO}_{1.5})$ ,  $G(\text{UO}_2)$ ,  $G(\text{UO}_{2.5})$

# ➔ Thermodynamic properties for stoichiometric $\text{UO}_2$

- Even in stoichiometric  $\text{UO}_2$ , point defects (Oxygen Frenkel pairs, electronic defects) form at high temperature



$$C_P = \left( \frac{\partial H}{\partial T} \right)_{P, N_i}$$



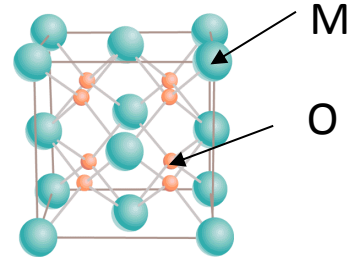
- ➔ The increase in the heat capacity for  $T > 1500$  K is due to the increase in point defect concentration

# ➔ Thermodynamic data on non stoichiometric $\text{UO}_{2\pm x}$

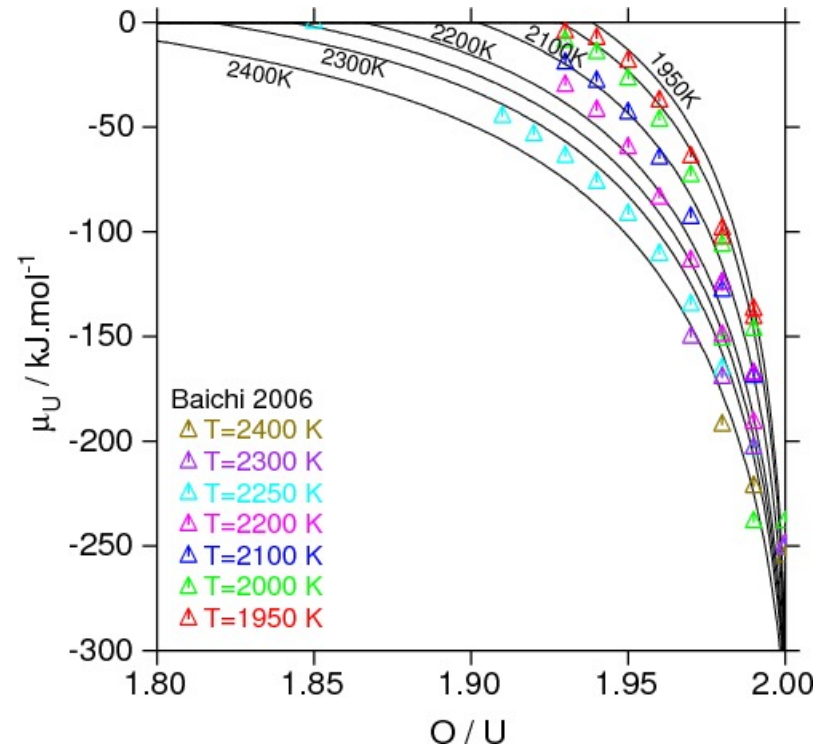
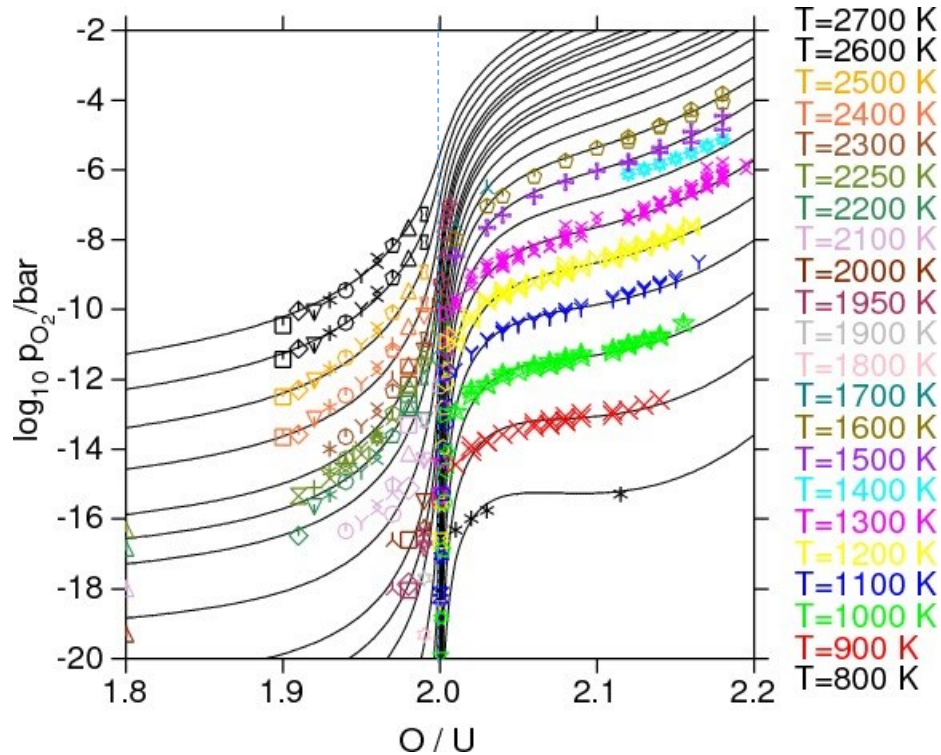
■ Experimental oxygen and uranium chemical potential data are available

$$\mu_{\text{O}_2} = \overline{\Delta G}(\text{O}_2) = R T \ln p_{\text{O}_2}$$

$$\mu_{\text{U}} = \overline{\Delta G}(U) = R T \ln a_{\text{U}}$$



Fluorite Structure



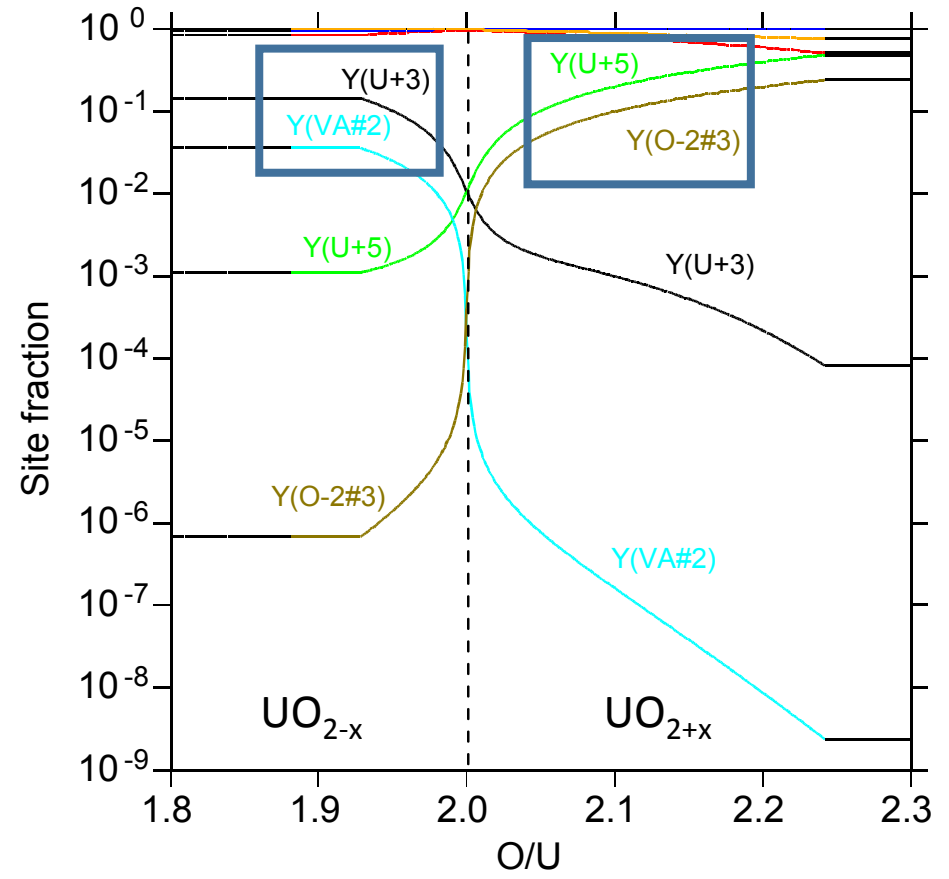
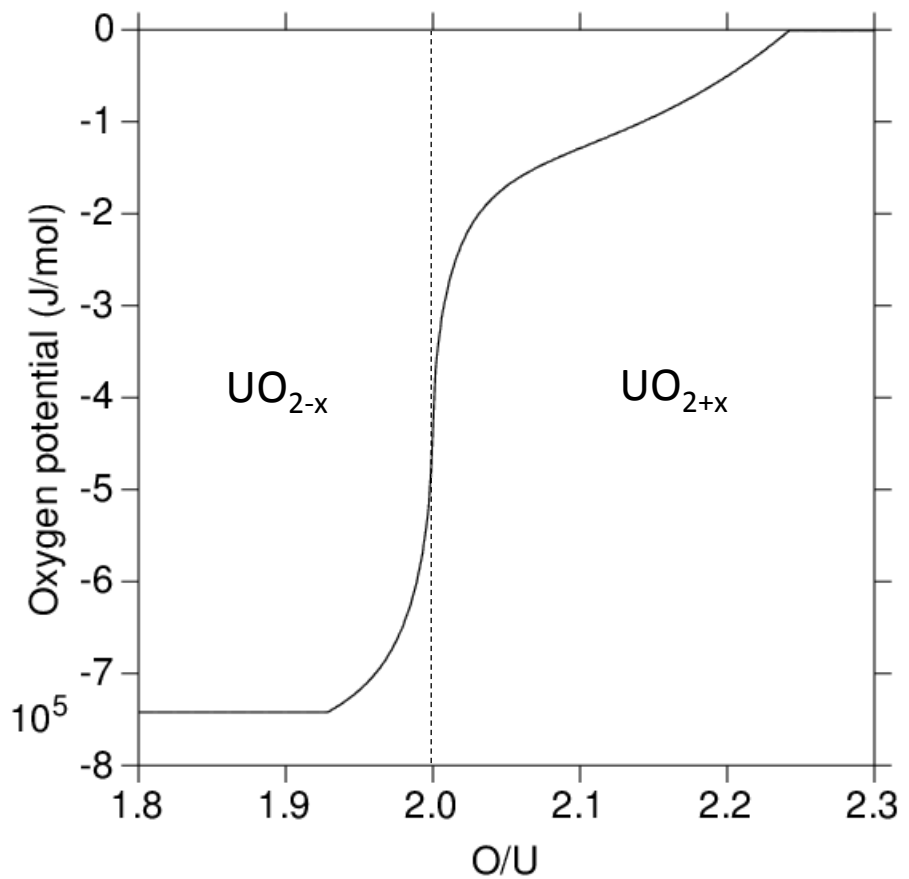
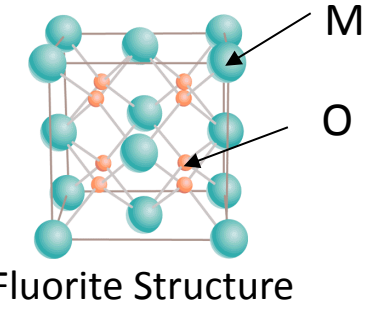
➔ The oxygen and uranium chemical potentials vary strongly with oxygen stoichiometry



# ➔ Thermodynamic data on non stoichiometric $\text{UO}_{2\pm x}$

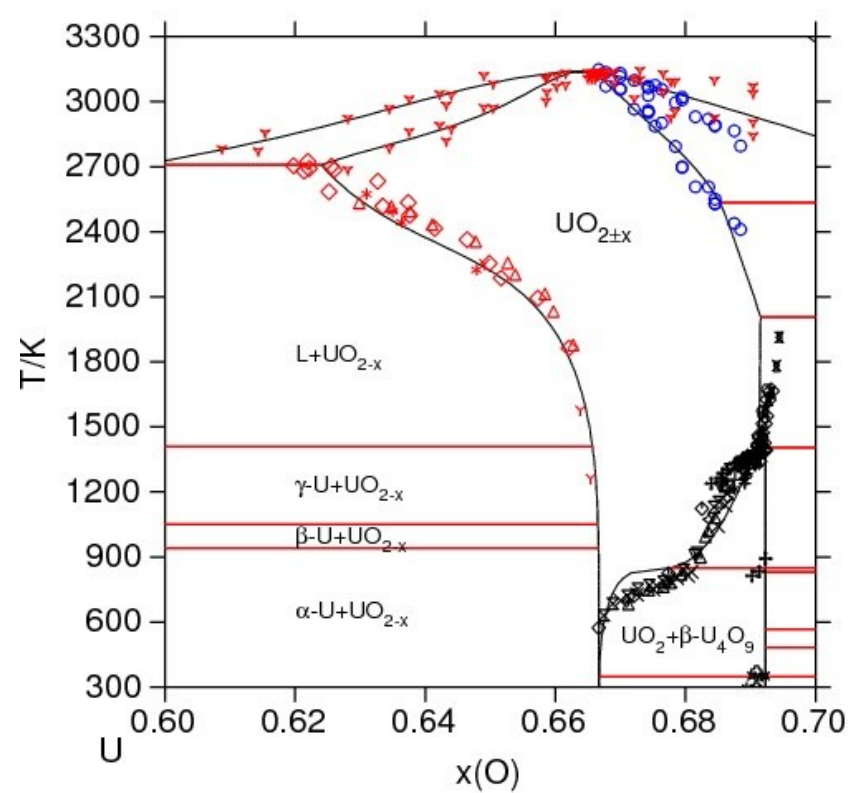
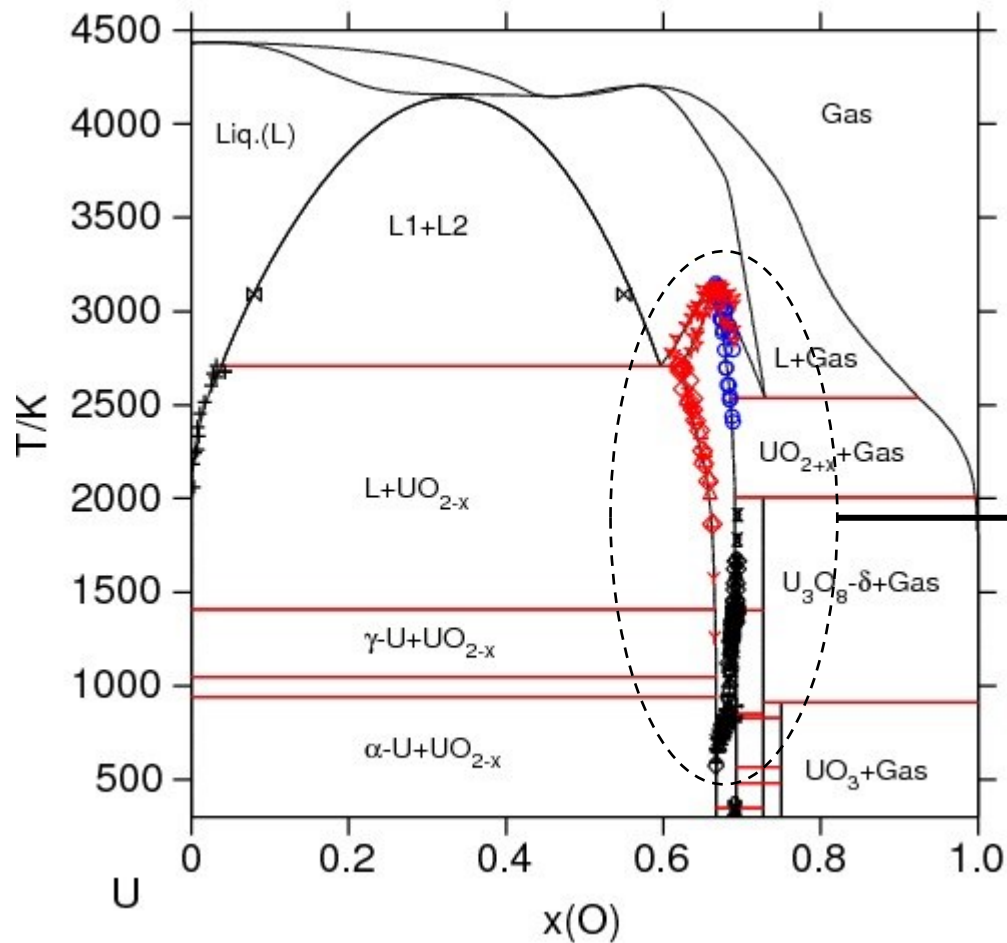
■ The oxygen potential variation is related to **point defect concentration**:

- $\text{O}/\text{M} < 2$ : ( $\text{U}^{+3}, \text{U}^{+4}$ ) ( $\text{O}^{-2}, \text{Va}$ )<sub>2</sub> ( $\text{Va}$ )  $\Rightarrow$  Oxygen vacancies and  $\text{U}^{+3}$
- $\text{O}/\text{M} > 2$ : ( $\text{U}^{+4}, \text{U}^{+5}$ ) ( $\text{O}^{-2}$ )<sub>2</sub> ( $\text{O}^{-2}, \text{Va}$ )  $\Rightarrow$  Oxygen interstitials and  $\text{U}^{+5}$



# Phase diagram data on the U-O system

## Phase diagram data



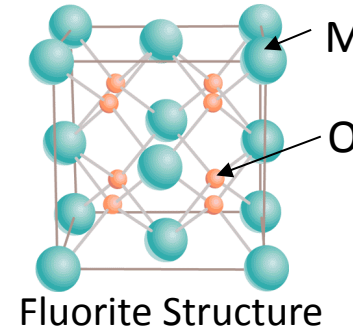
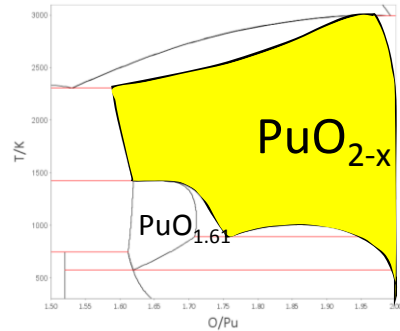
- \* SCHANER (1960)
- x INABA (1973)
- + NAITO (1973)
- + VAN LIERDE (1970)
- ACKERMAN (1973)
- ▼ PICARD (1981)
- + BLACKBURN (1958)
- ROBERTS (1961)
- x ANTHONY (1962)
- ▽ ARONSON (1961)
- Σ SCHANER (1960)
- ◇ GRONVOLD (1955)
- MARCHIDAN (1970.72.73.74.75)
- △ SAITO (1974)
- x MARKIN (1962)
- ◇ KIUKKOLA (1962)
- GERDANIAN (1981)
- ◇ ROBERTS (1961)
- + BLACKBURN (1958)
- PERRON (1968)
- ◇ KOTLAR (1968)
- HAGEMARK (1966)
- ◇ KOTLAR (1967)
- ◇ MARTIN (1965)
- ◇ GARG (1980)
- + EDWARDS (1966)
- \* GUINET (1966)
- △ ACKERMANN (1969)
- ▽ BANNISTER (1967)
- BATES (1966)
- FRYXELL (1968)
- ▽ LATTA (1970)
- ▽ PATTORET (1969)
- ◇ GUÉNEAU (1998)
- MANARA (2005)

○ D. Manara – Laser heating  
T solidus/liquidus for UO<sub>2+x</sub>

[ Manara et al, JNM 362 (2007) 14]

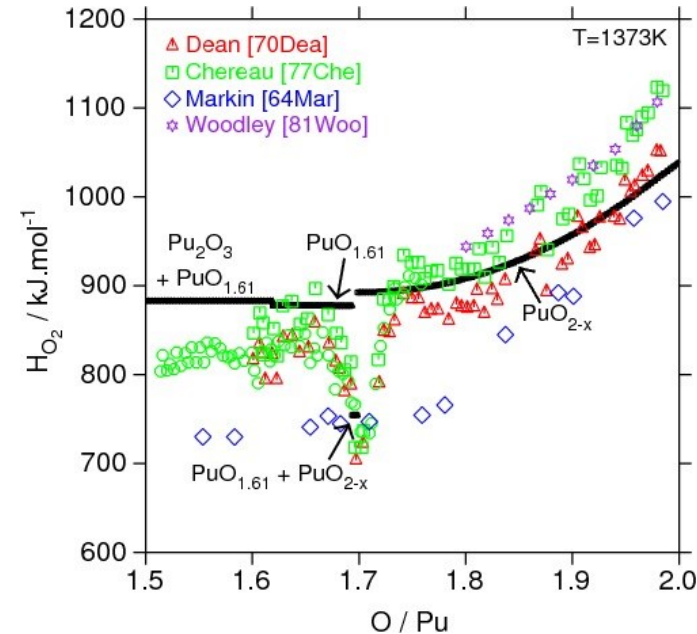
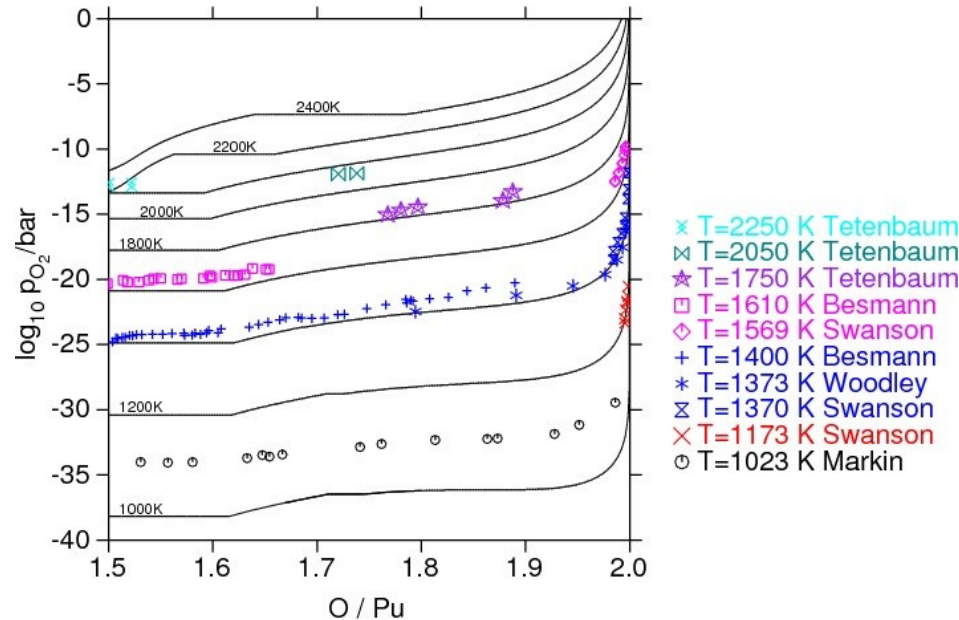
# ➔ Thermodynamic data on non stoichiometric $\text{PuO}_{2-x}$

■ Plutonium dioxide  $\text{PuO}_{2-x}$  has a large oxygen composition range with  $\text{O}/\text{Pu} < 2$



■ Three sublattice model  $(\text{Pu}^{+3}, \text{Pu}^{+4}) (\text{O}^{-2}, \text{Va})_2 (\text{Va})$

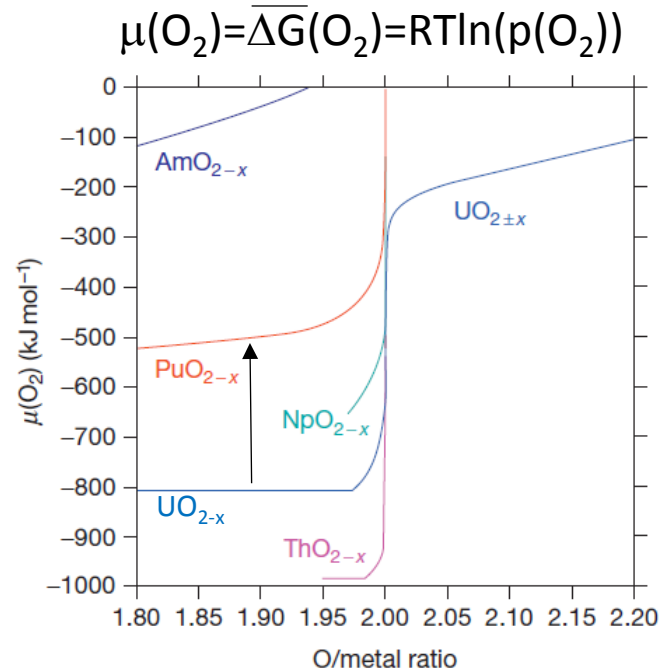
➔ Formation of oxygen vacancies (Va) compensated by reduction of  $\text{Pu}^{+4}$  into  $\text{Pu}^{+3}$



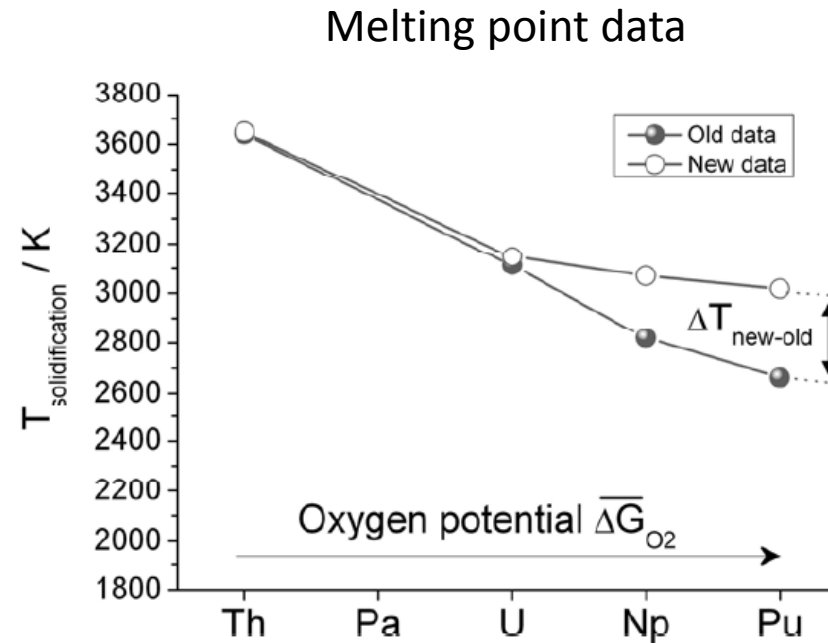


# ➡ Melting point data on actinide oxides

Why such large discrepancies between old and new measurements ?



[ Guéneau et al, Chap. 2.02, Comp. Nuc. Mater. (2012) ]



[ Manara et al, Procedia Chem. 7 (2012) 505 ]

The reactivity between actinide oxides ( $\text{ThO}_2$ ,  $\text{UO}_2$ ,  $\text{NpO}_2$ ,  $\text{PuO}_2$ ) and metallic crucibles (W...)   
 ↗ with the oxygen potential of the actinide oxides

$\mu(\text{O}_2)$  in  $\text{PuO}_2 \gg \mu(\text{O}_2)$  in  $\text{UO}_2$  ➡  $\text{PuO}_2$  loses oxygen at high temperature

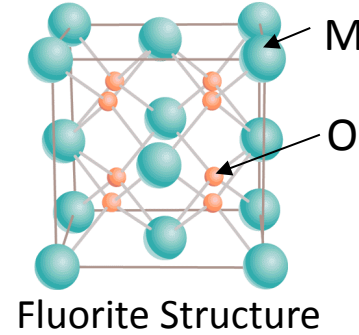
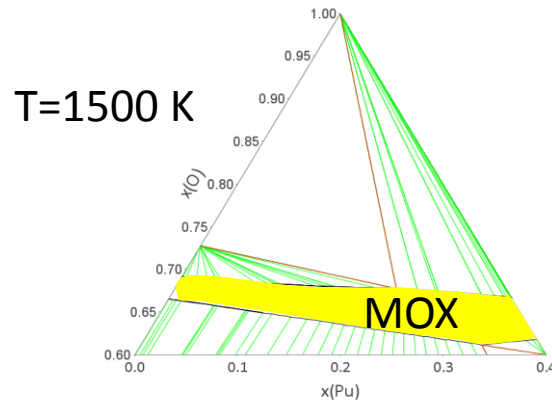
➡ The reactivity  $\text{PuO}_2/\text{W}$  is  $\gg$  than for  $\text{UO}_2/\text{W}$

➡ The melting point for  $\text{PuO}_2$  was underestimated due to a reaction with the crucible

➡ **Laser heating with self-crucible is a suitable method**

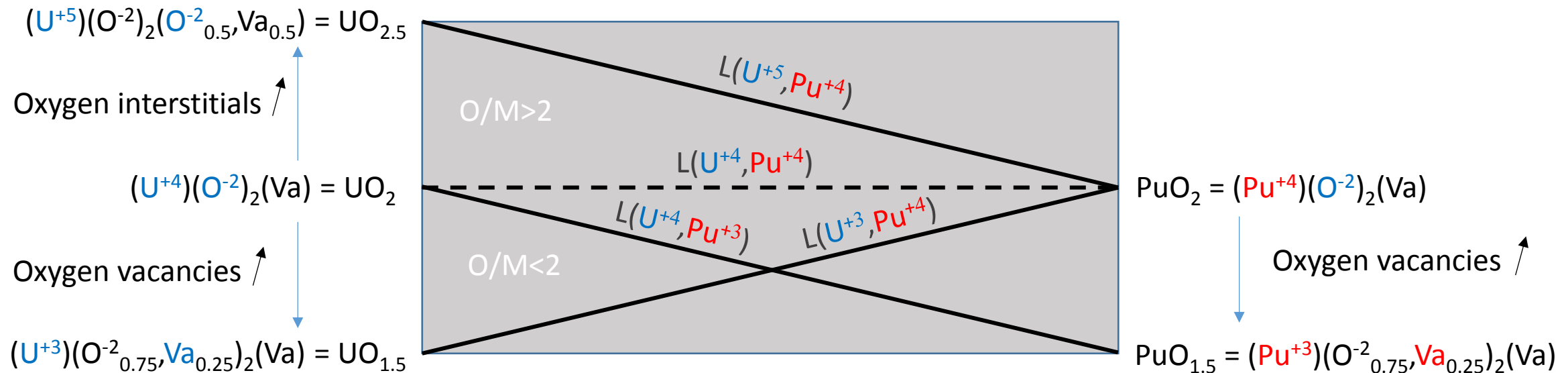
# ➔ Model for $(U,Pu)O_{2\pm x}$

■ Mixed uranium and plutonium dioxide  $(U,Pu)O_{2\pm x}$  has a large oxygen composition range

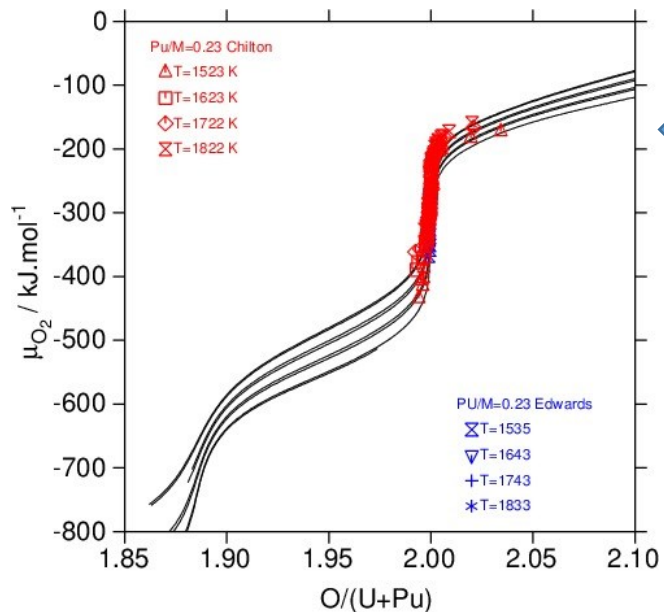
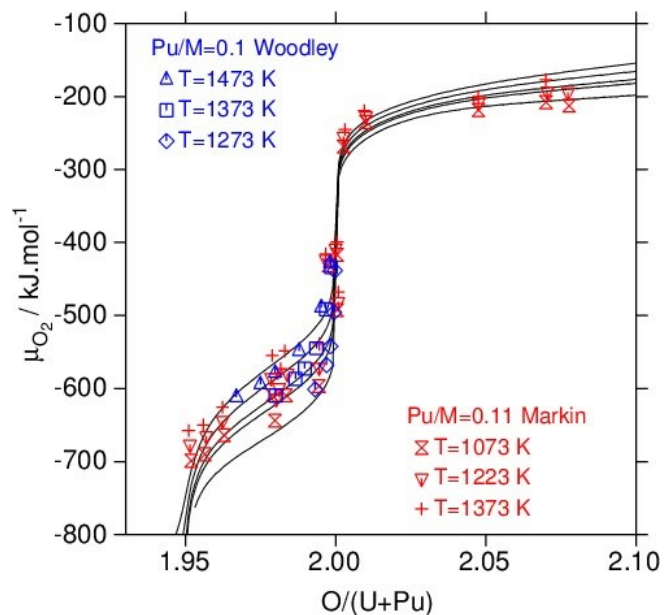


■ Three sublattice model  $(U^{+3}, U^{+4}, U^{+5}, Pu^{+3}, Pu^{+4}) (O^{-2}, Va)_2 (O^{-2}, Va)$

⇒ Ternary interaction parameters between cations have been adjusted to fit experimental data



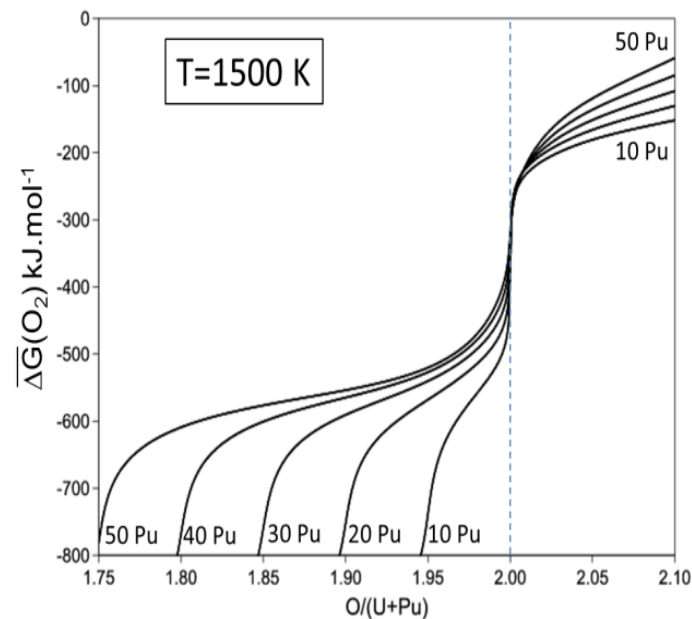
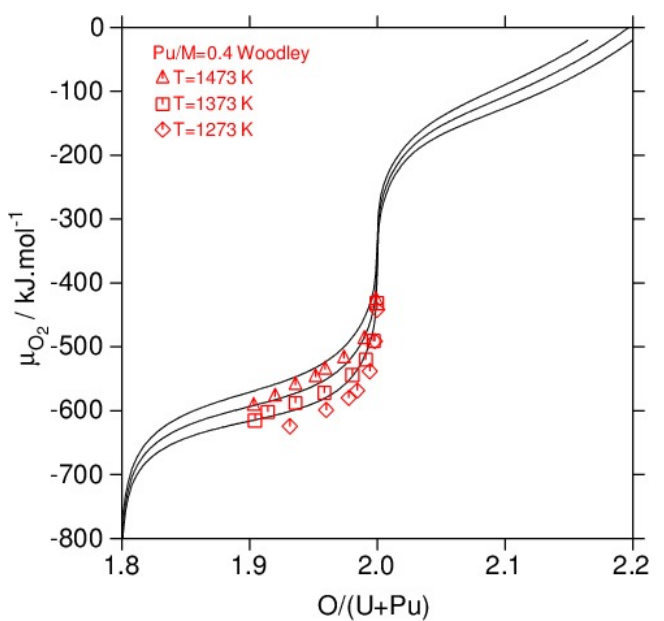
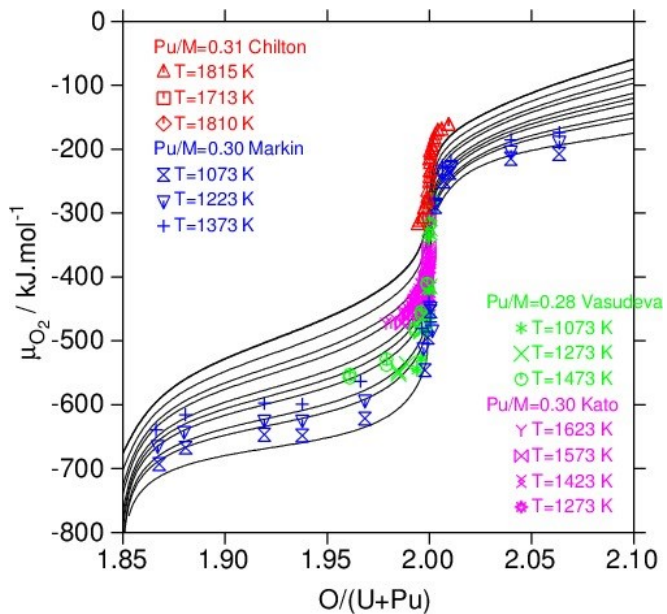
# Experimental thermodynamic data for (U,Pu)O<sub>2±x</sub>



- Oxygen chemical potential data are available for  $0.1 < \text{Pu}/(\text{U}+\text{Pu}) < 0.4$

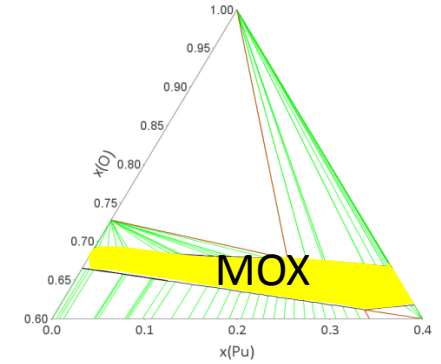
$$\mu_{\text{O}_2} = \Delta G(\text{O}_2) = R T \ln p_{\text{O}_2}$$

⇒ The oxygen potential increases with the Pu content



# Defect chemistry in $(U,Pu)O_{2\pm x}$

T=1500 K



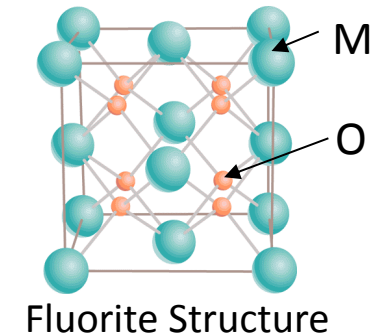
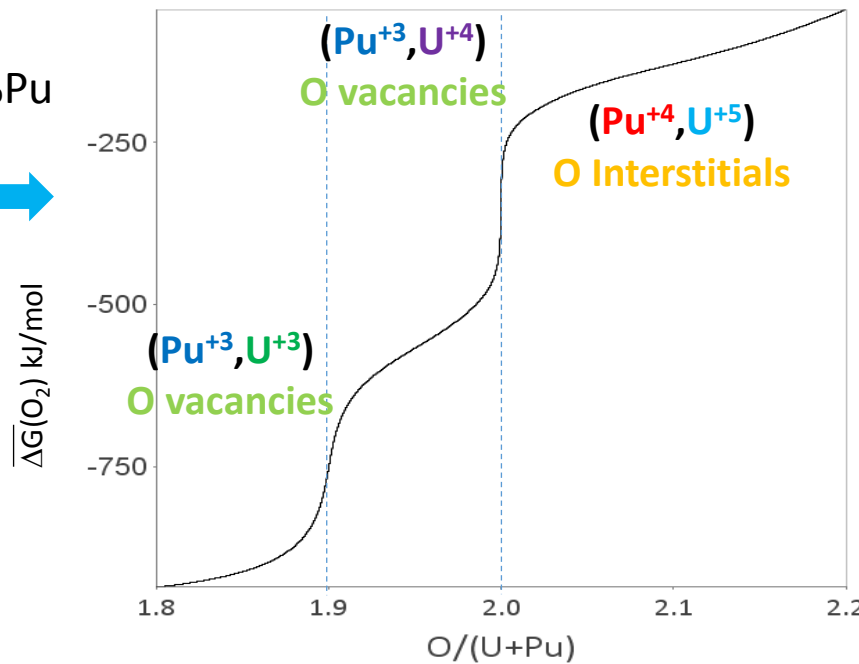
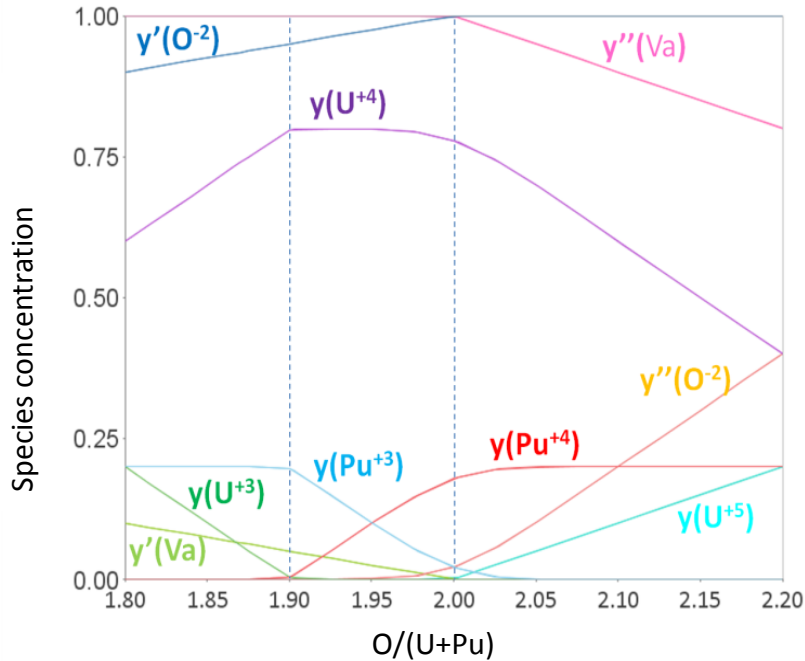
## Three sublattice model $(U^{+3},U^{+4},U^{+5},Pu^{+3},Pu^{+4}) (O^{-2},Va)_2 (O^{-2},Va)$

- For  $O/M < 1.9$ : Oxygen vacancies and  $U^{+4} \rightleftharpoons U^{+3}$ ,  $Pu^{+3}$
- For  $1.9 < O/M < 2$ : Oxygen vacancies and  $Pu^{+4} \rightleftharpoons Pu^{+3}$ ,  $U^{+4}$
- For  $O/M > 2$ : Oxygen interstitials and  $U^{+4} \rightleftharpoons U^{+5}$

- Reduction of  $U^{+4}$
- Reduction of  $Pu^{+4}$
- Oxidation of  $U^{+4}$

T=1500 K

MOX with 20%Pu

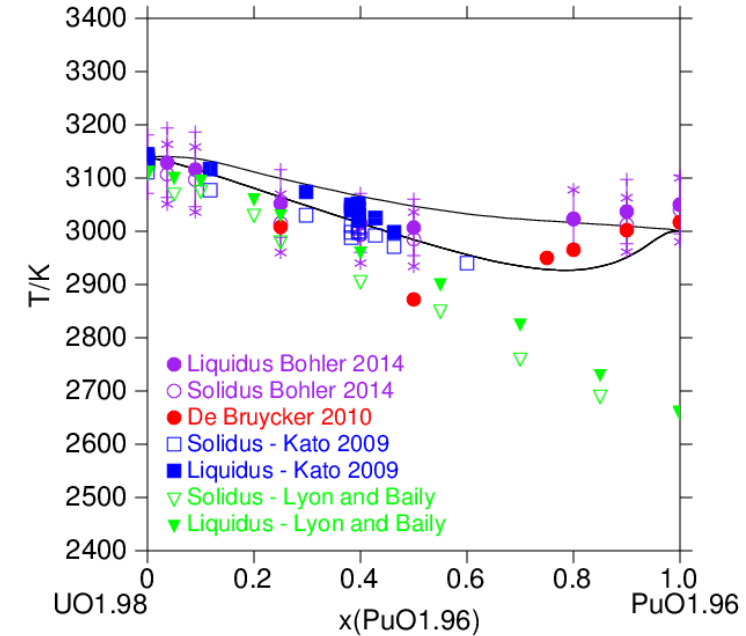
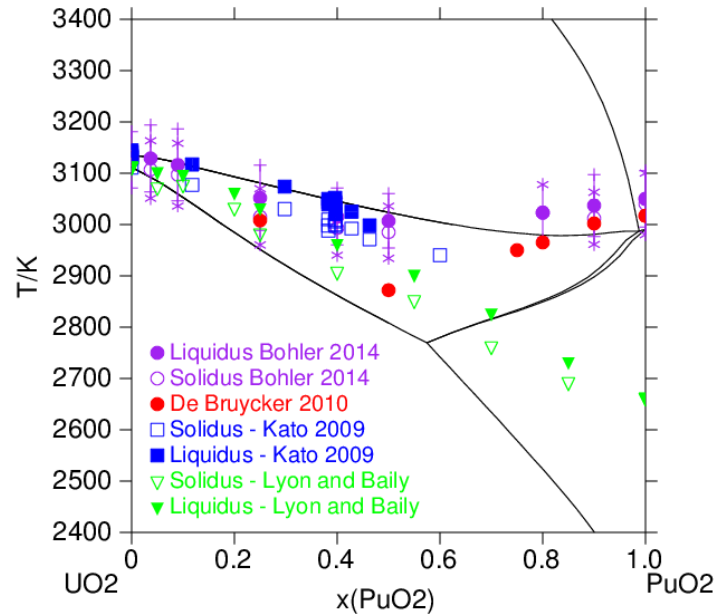




# ➔ UO<sub>2</sub>-PuO<sub>2</sub> system

## Phase diagram data

— Guéneau et al, JNM 2011



-Lyon and Bailey

➔ « **Reference** » data measured by thermal analysis in **W crucible**

- Kato et al

➔ Thermal analysis with **Re crucible** ➔ Higher solidus / liquidus T

- De Bruycker et al

➔ **Laser heating**

➔ **Consistent with the new melting point of PuO<sub>2</sub> (3017 K).**

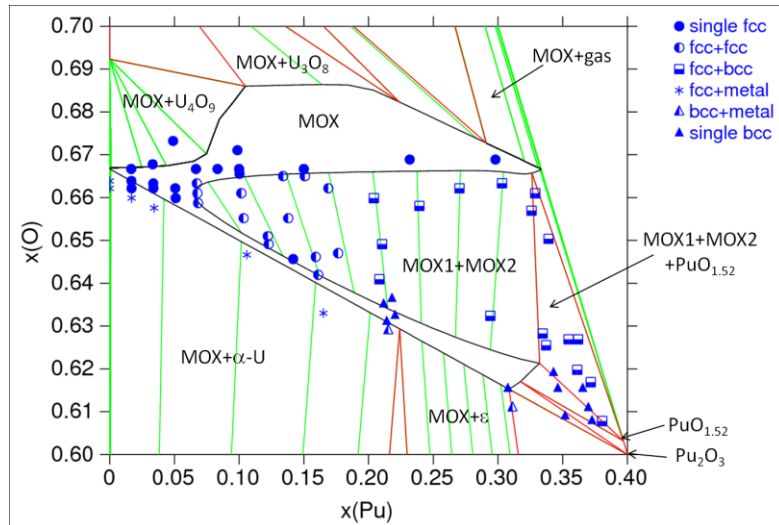
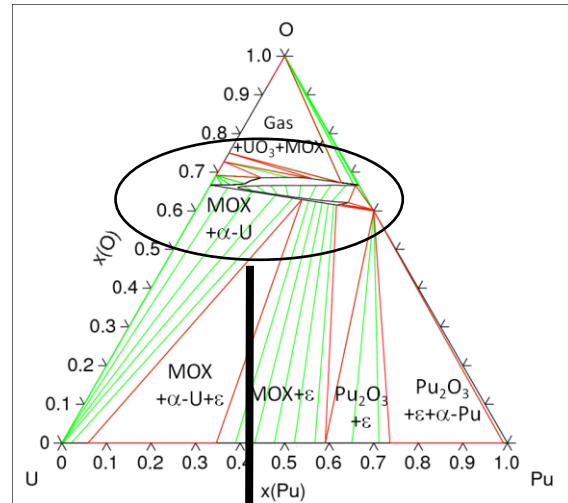
➔ **A minimum is found in the liquidus curve**

⇒ The data of Bohler (2014) have to be taken into account to improve the model for the liquid/solid transition

# ➔ Isothermal sections of the U-Pu-O system

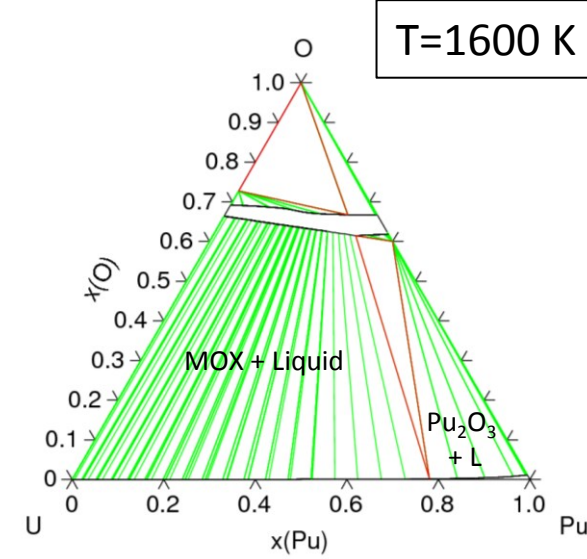
At low T: miscibility gap in  $(U,Pu)O_{2-x}$

T=473 K

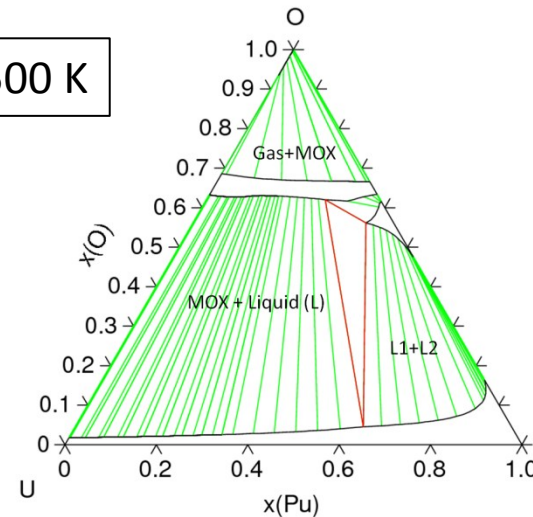


At high T: continuous solid solution  $(U,Pu)O_{2\pm x}$

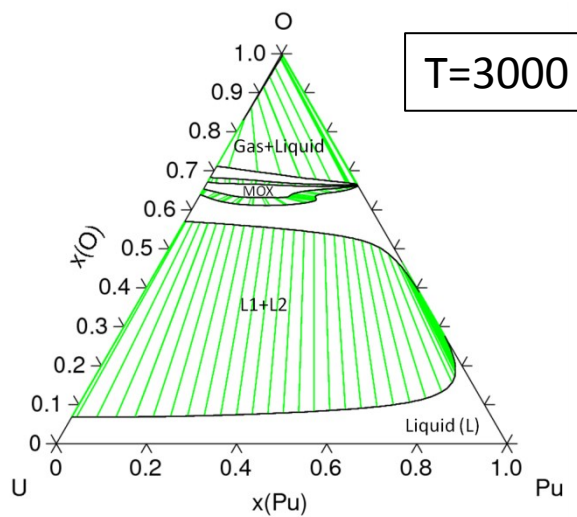
T=1600 K



T=2500 K



T=3000 K



# ➔ Thermodynamic parameters for (U,Pu)O<sub>2±x</sub>



Pu-O

MOX : (Pu <sup>+3</sup> ,Pu <sup>+4</sup> ,U <sup>+3</sup> ,U <sup>+4</sup> ,U <sup>+5</sup> )(O <sup>-2</sup> ,Va) <sub>2</sub> (O <sup>-2</sup> ,Va)
$G_{(U^{+3})(O^{-2})(Va)}^{MOX} = G_{UO_2}^{MOX} - G_{(U^{+4})(Va)(Va)}^{MOX} + G_{(U^{+3})(Va)(Va)}^{MOX}$
$G_{(U^{+4})(O^{-2})(Va)}^{MOX} - H_U^{SER} - 2H_O^{SER} = G_{UO_2}^{MOX} - H_U^{SER} - 2H_O^{SER}$ $= -1118940.2 + 554.00559T - 93.268T \ln T + 1.01704254 \cdot 10^{-2} T^2$ $- 2.03335671 \cdot 10^{-6} T^3 + 1091073.7 T^{-1}$
$G_{(U^{+5})(O^{-2})(Va)}^{MOX} = G_{UO_2}^{MOX} - 58351.62 + 39.67611T + 0.69315 RT$
$G_{(U^{+3})(Va)(Va)}^{MOX} = G_{UO_2}^{MOX} - 2G_O^{gas} + 747127 - 70.22618T + 1.12467 RT$
$G_{(U^{+4})(Va)(Va)}^{MOX} = G_{UO_2}^{MOX} - 2G_O^{gas} + 545210.5$
$G_{(U^{+5})(Va)(Va)}^{MOX} = G_{(U^{+5})(O^{-2})(Va)}^{MOX} - 2G_O^{gas} + 700000$
$G_{(U^{+3})(O^{-2})(O^{-2})}^{MOX} = G_{(U^{+3})(O^{-2})(Va)}^{MOX} + G_O^{gas}$
$G_{(U^{+4})(O^{-2})(O^{-2})}^{MOX} = G_{UO_2}^{MOX} + G_O^{gas}$
$G_{(U^{+5})(O^{-2})(O^{-2})}^{MOX} = G_{(U^{+5})(O^{-2})(Va)}^{MOX} + G_O^{gas}$
$G_{(U^{+3})(Va)(O^{-2})}^{MOX} - H_U^{SER} - H_O^{SER} = G_{(U^{+4})(Va)(O^{-2})}^{MOX} - H_U^{SER} - H_O^{SER}$ $= G_{(U^{+5})(Va)(O^{-2})}^{MOX} - H_U^{SER} - H_O^{SER} = +100000$
$L_{(U^{+4},U^{+5})(O^{-2})(O^{-2})}^{MOX} = -124936.9 - 21.6838T$
$L_{(U^{+3},U^{+4})(O^{-2})(Va)}^{MOX} = +40133.7 + 1076.4(y_{U^{+3}} - y_{U^{+4}})$

U-O

$G_{(Pu^{+4})(O^{-2})(Va)}^{MOX} - H_{Pu}^{SER} - 2H_O^{SER} = G_{PuO_2}^{MOX} - H_{Pu}^{SER} - 2H_O^{SER}$ $= -1099562.8 + 505.428856T - 83.31922T \ln T$ $- 0.00584178T^2 - 2.29241167 \cdot 10^{-11} T^3 + 913506T^{-1}$
$G_{(Pu^{+4})(Va)(Va)}^{MOX} = G_{PuO_2}^{MOX} - 2G_O^{gas}$
$G_{(Pu^{+4})(O^{-2})(O^{-2})}^{MOX} = G_{PuO_2}^{MOX} + G_O^{gas} + 80T$
$G_{(Pu^{+4})(Va)(O^{-2})}^{MOX} = G_{PuO_2}^{MOX} - G_O^{gas} + 80T$
$G_{(Pu^{+3})(O^{-2})(Va)}^{MOX} = G_{(Pu^{+3})(Va)(Va)}^{MOX} + 2G_O^{gas}$
$G_{(Pu^{+3})(Va)(Va)}^{MOX} = 0.5G^{Pu_2O_3} - 1.5G_O^{gas} + 3817.7 + 1.12467 RT$
$G_{(Pu^{+3})(O^{-2})(O^{-2})}^{MOX} = G_{(Pu^{+3})(Va)(Va)}^{MOX} + 3G_O^{gas} + 80T$
$G_{(Pu^{+3})(Va)(O^{-2})}^{MOX} = G_{(Pu^{+3})(Va)(Va)}^{MOX} + G_O^{gas} + 80T$
$L_{(Pu^{+3},Pu^{+4})(O^{-2})(Va)}^{MOX} = L_{(Pu^{+3},Pu^{+4})(Va)(Va)}^{MOX} = +9781.9 + 3.06205T$ $+ (y_{Pu^{+3}} - y_{Pu^{+4}})(-17507.47 + 5.46573T)$
$L_{(U^{+4},Pu^{+4})(O^{-2})(Va)}^{MOX} = -20000$
$L_{(U^{+4},Pu^{+3})(O^{-2})(Va)}^{MOX} = -150000$
$L_{(U^{+3},Pu^{+4})(O^{-2})(Va)}^{MOX} = +20000$
$L_{(U^{+4},Pu^{+3})(Va)(Va)}^{MOX} = -300000$
$L_{(Pu^{+4},U^{+5})(O^{-2})(*)}^{MOX} = -80000$

U-Pu-O

41 Elements

[www.oecd-nea.org/science/taf-id/](http://www.oecd-nea.org/science/taf-id/)

(Canada, France, Japan, The Netherlands, Korea, UK, USA)

206 Binaries

TAF-ID : Thermodynamics of Advanced Fuels - International Database

Home Introduction Models Phases Systems TDB

Elements

Assessed binary systems

Assessed ternary systems

Systems with **Ag, Al, Am, Ar, B, Ba, C, Ca, Ce, Cr, Cs, Fe, Gd, H, He, I, La, Mg, Mo, N, Nb, Nd, Ni, Np, O, Pd, Pu, Re, Rh, Ru, Si, Sr, Ta, Tc, Te, Th, Ti, U, V, W, Zr**

Periodic table

76 Ternaries

TAF-ID : Thermodynamics of Advanced Fuels - International Database

Home Introduction Models Phases Systems TDB

Elements

Assessed binary systems

Assessed ternary systems

Higher order systems

Systems with **Ag, Al, Am, Ar, B, Ba, C, Ca, Ce, Cr, Cs, Fe, Gd, H, He, I, La, Mg, Mo, N, Nb, Nd, Ni, Np, O, Pd, Pu, Re, Rh, Ru, Si, Sr, Ta, Tc, Te, Th, Ti, U, V, W, Zr**

Periodic table

**Binary systems described by the database**

The phase diagrams calculated at  $10^5$  Pa for the different assessed binary systems can be displayed thanks to the following list.

Ag-I\* Ag-O\* Ag-Ti\* Ag-Zr  
Al-Ca Al-Cr Al-Fe Al-Mg Al-O Al-Si Al-U\* Al-Zr\*  
Am-Fe Am-Np Am-O\* Am-Pu\* Am-U Am-Zr  
B-C B-Cr B-Fe B-H B-I B-Ni B-O\* B-Pu B-U B-Zr\*  
Ba-H Ba-I\* Ba-La\* Ba-Mo\* Ba-N Ba-O\* Ba-Pu\* Ba-Sr\* Ba-Ti\* Ba-U\* Ba-V\* Ba-Zr\*  
C-Cr C-Fe C-Mo C-N C-Nb C-Ni C-O C-Pu\* C-Re C-Si C-Ta C-Ti C-U\*  
C-V C-W C-Zr  
Ca-Fe Ca-Mg Ca-O Ca-Si Ca-U\* Ca-Zr\*  
Ce-Cr Ce-Fe Ce-Nd Ce-O\* Ce-U\*  
Cr-Cs\* Cr-Fe Cr-H Cr-I Cr-La\* Cr-Mo Cr-N Cr-Nd Cr-Ni Cr-O Cr-Pd Cr-Pu\* Cr-Si Cr-Ti\* Cr-U\* Cr-Zr\*  
Cs-I\* Cs-Mo\* Cs-Nb\* Cs-O Cs-Pu\* Cs-Ta\* Cs-Te\* Cs-Ti\* Cs-U\* Cs-V\* Cs-Zr\*  
Fe-Nd Fe-Ni Fe-Np Fe-O Fe-Pd\* Fe-Pu Fe-Si Fe-U Fe-Zr  
Gd-O\* Gd-U\*  
H-I H-O H-Sr  
I-Mo I-Sr\* I-Te  
La-Mo\* La-Nb\* La-O La-Pu\* La-Re\* La-Ta\* La-Te La-Ti\* La-U\* La-V\* La-W\*  
Mg-O Mg-U\* Mg-Zr\*  
Mo-N Mo-O Mo-Pd Mo-Pu\* Mo-Re Mo-Rh\* Mo-Ru Mo-Si Mo-Sr\* Mo-Te\* Mo-Ti Mo-U\* Mo-Zr  
N-O N-Pu\* N-Si N-Ti N-U\* N-Zr  
Nb-O Nb-Pu\* Nb-Si Nb-U Nb-Zr  
Nd-O\* Nd-Pd\* Nd-Pu\* Nd-U\* Nd-Zr\*  
Ni-O Ni-U Ni-Zr  
Np-O\* Np-Pu\* Np-U Np-Zr  
O-Pu\* O-Ru O-Si O-Sr O-Te O-Th\* O-Ti O-U O-Zr  
Pd-Rh Pd-Ru Pd-Tc Pd-Te Pd-U\* Pd-Zr\*  
Pu-Re\* Pu-Ru\* Pu-Si\* Pu-Sr\* Pu-Ti\* Pu-U\* Pu-W\* Pu-Zr  
Re-Si Re-U\* Re-W  
Rh-Ru\* Rh-Tc\* Rh-Te\*  
Ru-Te\* Ru-U\*  
Si-Ta Si-Ti Si-U\* Si-W Si-Zr  
Sr-Ti\* Sr-U\* Sr-V\* Sr-Zr\*  
Ta-U\*  
Ti-U\* Ti-Zr  
U-W\* U-Zr

Thus, over 820 binary systems, 206 are described by the present database, and 85\* assessed during the present work.

TAF-ID : Thermodynamics of Advanced Fuels - International Database

Home Introduction Models Phases Systems TDB

Elements

Assessed binary systems

Assessed ternary systems

Higher order systems

Systems with **Ag, Al, Am, Ar, B, Ba, C, Ca, Ce, Cr, Cs, Fe, Gd, H, He, I, La, Mg, Mo, N, Nb, Nd, Ni, Np, O, Pd, Pu, Re, Rh, Ru, Si, Sr, Ta, Tc, Te, Th, Ti, U, V, W, Zr**

Periodic table

**Ternary systems**

The assessed ternary systems defined by the database are listed hereunder by alphabetical order. At the current state of development of the database, only a few is assessed.

Al-Ca-O Al-Cr-O Al-Fe-O Al-Mg-O Al-O-Si Al-O-U Al-O-Zr  
Am-O-Pu  
B-C-Fe B-C-U B-C-Zr B-Fe-Zr B-H-O B-Pu-U  
Ba-Mo-O Ba-O-U Ba-O-Zr  
C-Mo-Re C-Mo-Si C-Mo-Ti C-Mo-U C-N-Ti C-N-U C-O-Pu C-O-U C-Pu-U C-Pu-W C-Re-U  
C-Re-W C-Si-Ti C-Si-U C-U-W C-U-Zr  
Ca-Fe-O Ca-Mg-O Ca-O-Si Ca-O-U Ca-O-Zr Ca-Si-U Ca-Si-Zr  
Ce-Fe-Nd Ce-O-U  
Cr-Fe-O Cr-Fe-Zr  
Cs-Mo-O Cs-O-U Cs-O-Zr  
Fe-O-Si Fe-O-U Fe-O-Zr Fe-U-Zr  
Gd-O-U  
La-O-U  
Mg-O-Si Mg-O-U Mg-O-Zr  
Mo-O-U Mo-Pd-Rh Mo-Pd-Ru Mo-Rh-Ru  
Nb-O-U  
Nd-O-U  
Ni-O-Si  
O-Pu-U O-Pu-Zr O-Si-U O-Si-Zr O-Sr-U O-Sr-Zr O-U-Zr  
Pd-Rh-Ru  
Pu-U-Zr

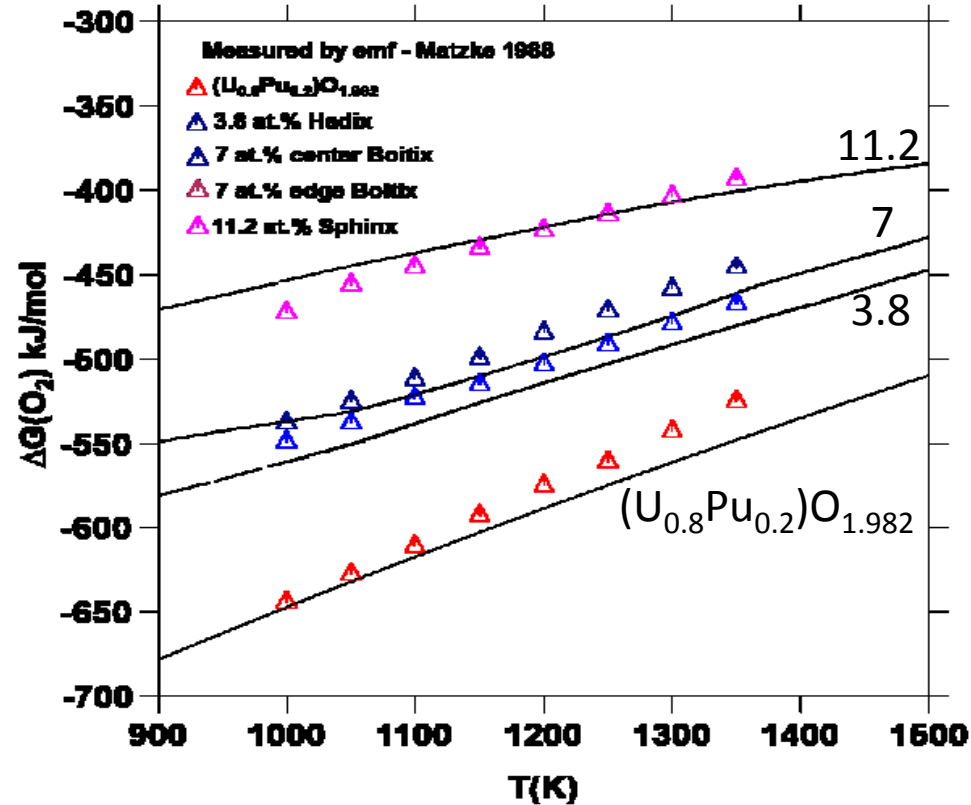
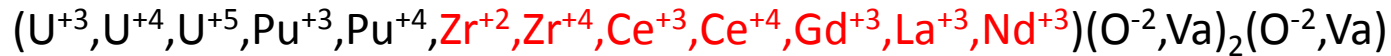
Thus over 10660 ternary systems, 72 systems are assessed in the current database.

⇒ Phase 2 : Dec. 2019 – Dec. 2022

# ➔ Calculations on irradiated MOX fuel

## PREDICTION OF OXYGEN POTENTIAL

Calculation for a MOX fuel with burnups of 3.8, 7 and 11.2 at .%  
 ⇒ 16 Fission Products (Nd,La,Gd,He,Ce,I,Zr,Cs,Sr,Ba,Te,Mo,Pd,Ru,Tc,Rh)



O/M of the oxide matrix at 1600 K

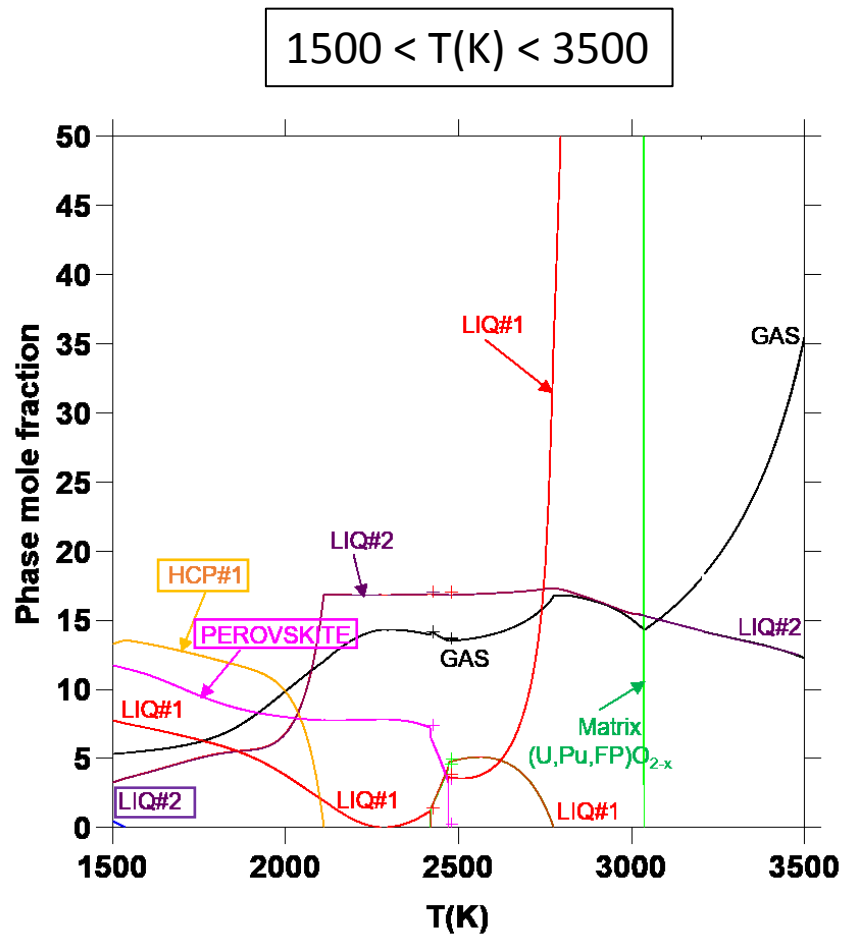
	1.997	↑ O/M ↗
Burnup ↗	1.996	
	1.995	

⇒ The oxygen potential of the fuel increases with burnup

⇒ Very good agreement between calc./exp. oxygen potential data

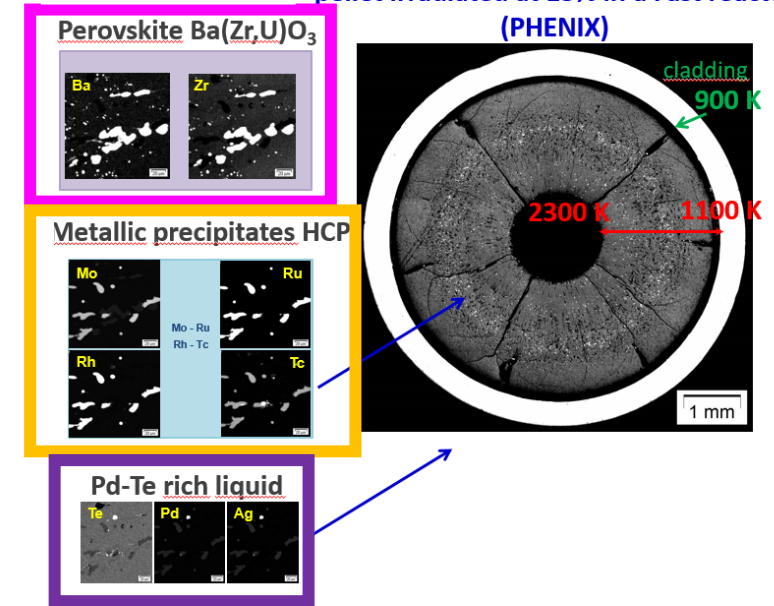
# Calculations on irradiated MOX fuel

## FORMATION OF SECONDARY FISSION PRODUCT PHASES FOR A 7 at. % BURNUP



Matrix (U,Pu,FPs)O<sub>2</sub> matrix  
 + Metallic precipitates (HCP)  
 + Perovskite precipitates  
 + Liquid phases  
 + Gas

Typical microstructure of a MOX fuel pellet irradiated at 13% in a Fast reactor (PHENIX)



Metallic precipitates (HCP)  
 Melting at T=2109 K

Perovskite (Ba,Sr)(Zr,U)O<sub>3</sub>  
 Melting at T=2469 K

Dissolution of the fuel matrix in the molten perovskite

Beginning of the oxide fuel melting

# ➔ Conclusion

- **Thermodynamic modelling** of nuclear fuels is required to provide **key input thermodynamic** and phase diagram data for **Fuel Performance Codes**
  - ⇒ Oxygen potential, fission product phases (JOG/ROG formation), solid/liquid transitions, heat capacity ....
- CALPHAD is a **suitable method** to model multi-component systems by **extrapolating** from binary and ternary sub-systems;
  - ⇒ It is time consuming ⇒ International collaborative projects are good frameworks to develop large databases
  - ⇒ Experimental thermodynamic measurements on fuels are challenging but needed to test the **validity** of the databases (Phase 2 of TAF-ID project)
  - ⇒ **First-principle calculations** are useful to calculate thermodynamic data that can be used in the models
- But thermodynamics (alone) cannot explain the fuel behaviour; it has to be **coupled with kinetic and mass transfer models**
  - ⇒ In the GERMINAL fuel performance code, there is a coupling using the open source code Open Calphad (developped by Bo Sundman) and the TAF-ID database
- Other Gibbs energy minimizer codes exist such as FACTSAGE, PANDAT, PyCALPHAD ...
  - ⇒ The format of the database can differ; in some cases a conversion of the database file is required (for instance from Thermo-Calc to FACTSAGE format);
  - ⇒ All the sublattice models are not implemented in all the codes

TAF-ID website: <https://www.oecd-nea.org/science/taf-id/>

A public version is available ⇒ contact person: [davide.costa@oecd.org](mailto:davide.costa@oecd.org)